Carbon Utilization and Petrochemical Integration: Capturing value via residue to chemicals projects

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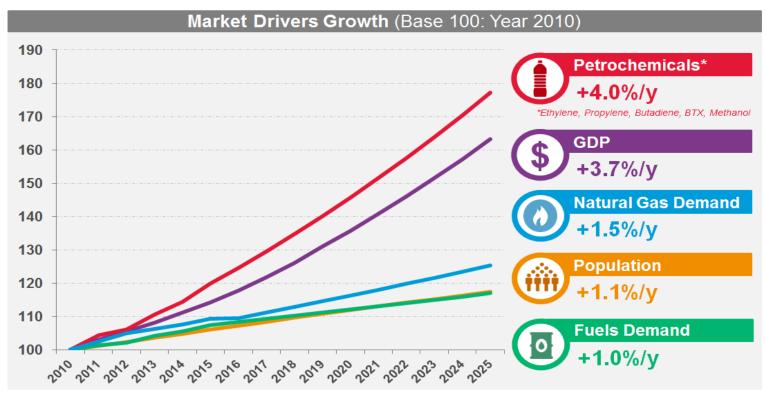


- Oil & Petrochemicals Market Dynamics and Challenges
- H-Oil Ebullated Bed Technology
- Crude to Chemicals Solutions
 - Aromatics Case Study : Grassroot Complex Towards Aromatics
 - Olefins Case Study : Integration with Steam Cracker Complex

Oil & Petrochemicals Market Dynamics and Challenges



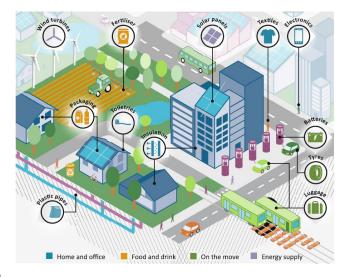
Strong Petrochemicals Demand Growth



Source: Bank, CEH, Axens



In 2035, How Much Oil will be Converted into Petrochemicals? (RTS Scenario, IEA 2018)



In 1990, 5.3 Mbpd were converted into petrochemicals

- 1) 10.2 Mbpd
- 2) 12.3 Mbpd
- 3) 15.6 Mbpd

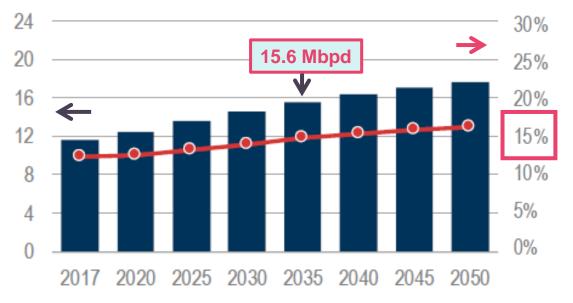




In 2035, How Much Oil will be Converted into Petrochemicals? (RTS Scenario, IEA 2018)

Feedstock Oil demand, Mbpd





Source : The Future of Petrochemicals, IEA, 2018



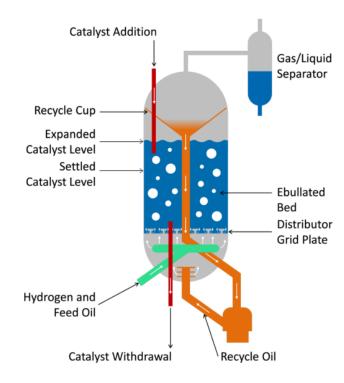
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H-Oil Technology

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Ebullated Bed Residue Hydrocracking H-Oil®



- Demonstrated high conversion levels
- No limitation on feed properties
- Mature & reliable technology more than 1.2 MBPSD licensed capacity
- High availability> 96% demonstrated on several units
- 2 new high conversion H-Oil[®] units starting-up in 2019
- **3** recent awards in 2019

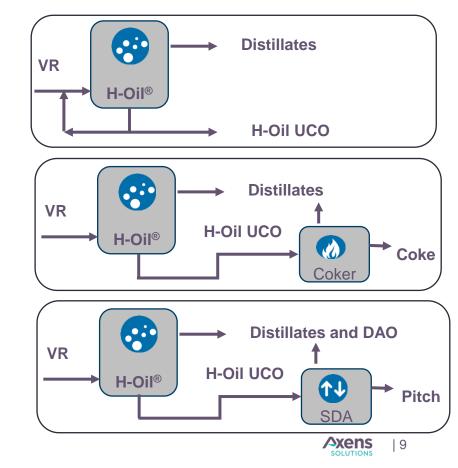


VR High Conversion: Main technology routes

- Vacuum Bottoms Recycle
- Residence Time Path:
 - Low Space Velocity Design
- Coker Integration:
 - Concentration of the CCR in the Coke

SDA Integration:

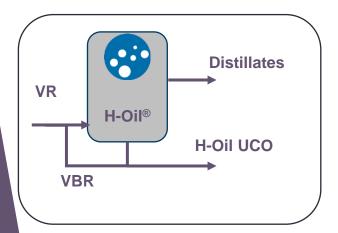
Concentration of Asphaltenes in pitch



H-Oil Reactor Design : Paths for High Conversion



- Recycle of the Vacuum Bottom VBR
 - VBR reduces the severity per pass, low conversion per pass and reduced formation of sediment levels
 - Demonstrated Commercially : H-Oil unit started-up in the 80's had operated at high conversion of VR with VBR, this mode was part of the design.



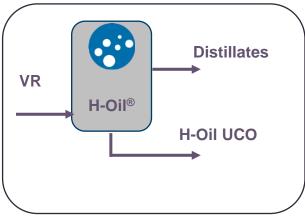
Operating Mode	LSFO	High Conversion	Maximum Capacity
VR Feed Capacity	Base	Base Plus VBR	Base + 25%
1000 °F+ Conversion,	Base	Above 85%	Base

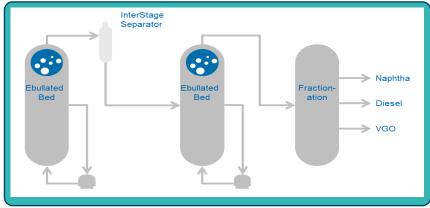


H-Oil Reactor Design : Paths for High Conversion



- Low LHSV Design Long residence time
 - Maximize catalytic performance for both conversion and hydrorefining
 - Control the sediment with reactor temperature
 - High quality Effluents due to High HDS and High CCR Removal
 - Demonstrated in commercial unit :
 - H-Oil under start-up in 2019 at low LHSV is design for more than 85% of conversion.







H-Oil[®] Suite : Low LHSV Commercial Follow-up

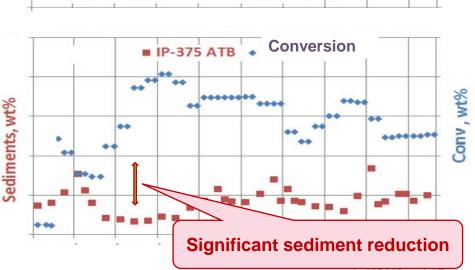
wt%

ion,

Conver

40% VR availability reduction

- Lower capacity operation industrial demonstration
 - Higher conversion
 - Less sediment production
 - Enhanced refining performance
- LHSV / WABT prove powerful to break conversion ceiling



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Conversion, wt%

44



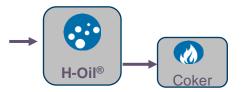
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Up to 15% of conversion

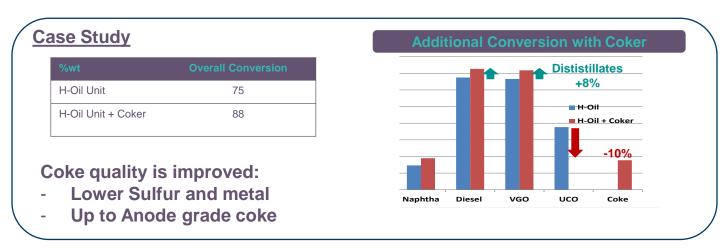
-Unit Capacity

Unit Capacity, t/h

Coker Integration



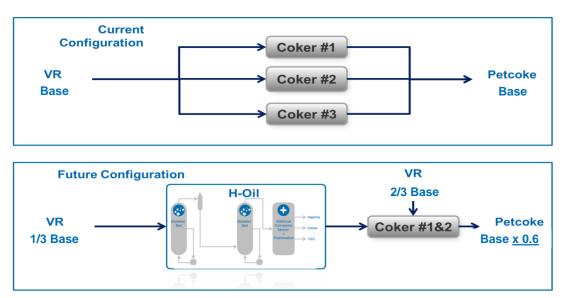
- Unlock sediment constraints for H-Oil® UCO
- Create value not only with high conversion but also with better coke quality
- Maximize the use of existing assets



UCO to Coker Unit

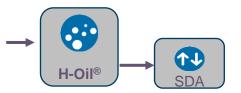
Commercial Reference: Asia Location, under commissionning
 Maximize the use of existing assets:

Combination H-Oil + Coker reaches 94% of VR conversion









Unlock sediment constraints for H-Oil[®] UCO and concentration of Asphaltens in the pitch

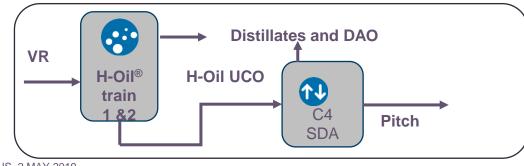
Reduced CAPEX in comparison with Coker Unit

High Incremental Conversion for refinery with pitch disposal

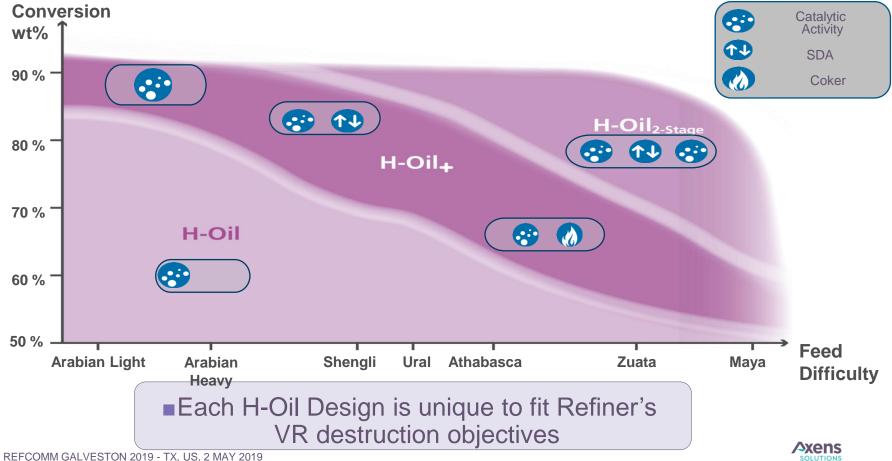
Pitch is better than Coke for hydrogen production in Gasification

Commercial References:

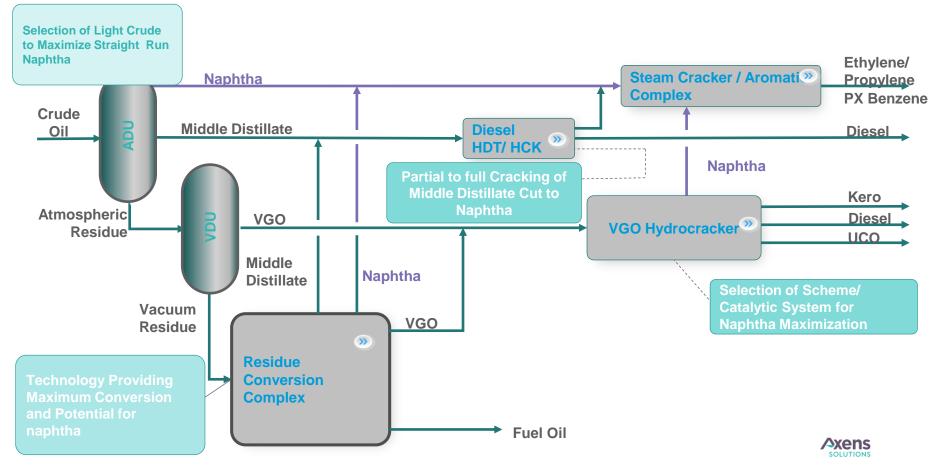
- Hengli Crude to Paraxylene Complex. H-Oil unit has started-up



H-Oil[®] Suite



Refining & Petrochemicals Integration How to Increase Naphtha Production?



Crude to Chemical Options

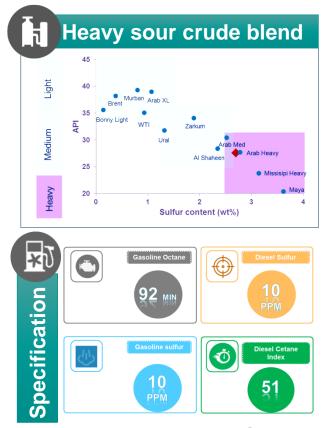
Aromatics Production



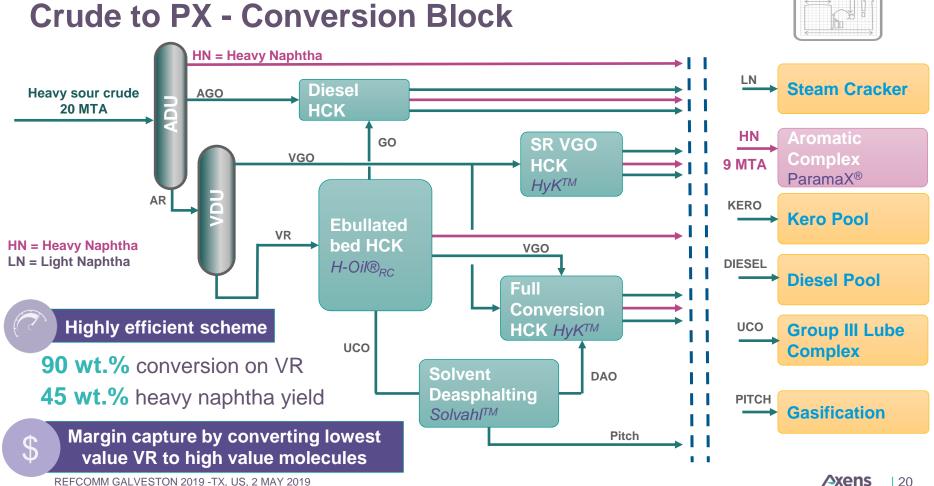
Crude to PX Project - Feed and Products

Feed 400,000 BPSD of crude oil

- 60% Arabian Heavy •
- 30% Arabian medium •
- 10% Marlim •
- Product Requirement
 - 211,000BPSD of Heavy Naphtha • for PX production
 - Co-Production of high quality gasoline, • diesel & jet fuel
 - Production of Group III Lube Base Oil •
 - Minimization of residue production •



Axens



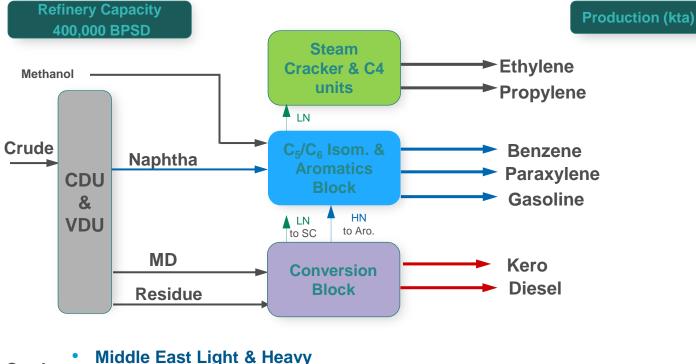
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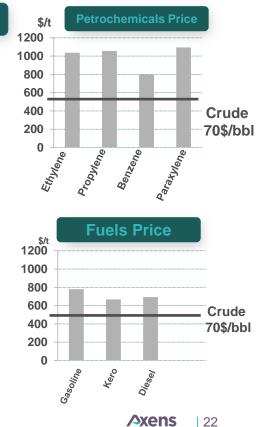
Crude to Chemical Options

Olefins Production



World-class Integrated Project – Asia Location Petrochemicals & Fuels Production





SOLUTIONS

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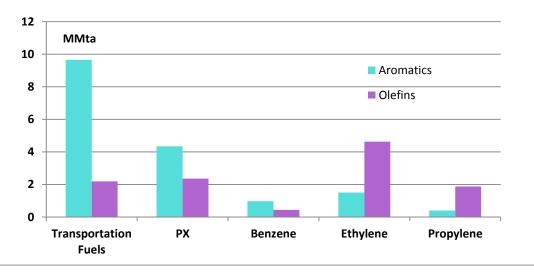
Arabian Medium

Brazil Frade

Crude

Products Distribution for the two cases studies

Comparison Aromatics and Olefins Production



Flexibility in the design is Key to maximize products value

Same VR Conversion

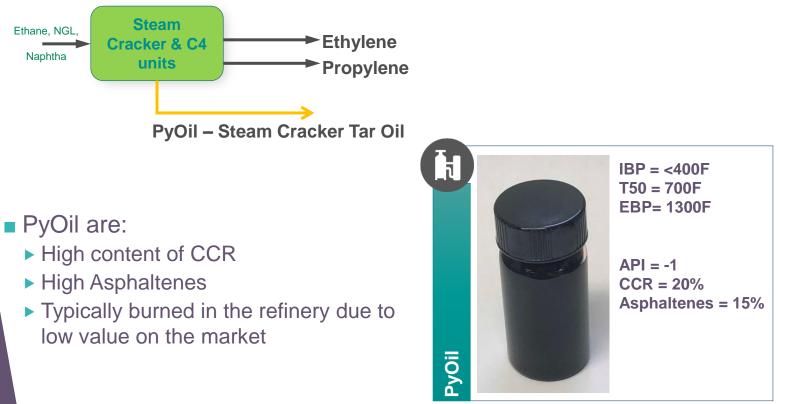
Case Study 1
High transportation fuel and
Paraxylene Products

• Case Study 2 Less transportation fuel but high Paraxylene and Olefins production

Chemical Complex design has a large panel of technologies to cover from Maxi PX to Maxi Olefins.

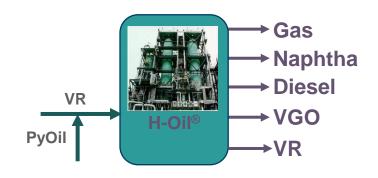


Olefins Market : Steam Cracker Complex



Pyoil Co-processed in H-Oil Unit

Two Recent Awards : Crude to Chemical complex with pyOil in the H-Oil feed



Hydrogen = 2.8 \$/MMBtu H-Oil Feed & Products Value, \$/bbl 140 120 +54\$/b 100 Brent at 70\$/b 80 60 40 20 Fuel VR VGO Diesel Naphtha Pyoil After H-Oil

Initial Case: PyOil to Fuel Design Case: PyOil is sent to the H-Oil Unit PyOil is hydrogenated and converted PyOil Value is more than double

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H-Oil : Capturing Value from the Heavy Ends



- Petrochemicals demand growth higher than that of fuels
- Crude Oil-to-Chemical complexes offer many advantages:
 Expanding into higher growth markets
 - Mitigating risks related to raw material and product price variations
 Improving asset profitability
- Crude Oil-to-Chemical projects implementing advanced technologies is a way to catch these opportunities
- Ebullated Bed Residue Hydrocracking H-Oil® has commercially proven High Conversion Operation

