# **Duiker** Combustion Engineers

# +31 (0)174 282 700 www.duiker.com

#### **SRU Thermal Reactor Chemistry & Design**

Roelof ten Hooven Area Sales Manager





# **Company Profile**

- Engineering company specialized in process combustion equipment
- Founded in 1919
- ± 75 employees





# **Goals of the SRU**

- Recover elemental sulfur (S<sub>2-8</sub>) from all sulfur species in the feed gases (AAG and/or SWSAG).
- Destruct other harmful components of the feed gases.
- Limit the formation of new harmful substances.

Basically, comply with emissions regulations!



# **Typical Sulfur Recovery Unit**

![](_page_4_Figure_1.jpeg)

![](_page_4_Picture_2.jpeg)

# **Sulfur Recovery Unit Thermal Stage**

![](_page_5_Figure_1.jpeg)

![](_page_5_Picture_2.jpeg)

![](_page_6_Picture_0.jpeg)

![](_page_6_Picture_1.jpeg)

# **Thermal Stage Objectives**

- 65-70% Sulfur Recovery
- Ammonia Destruction
- Hydrocarbon Destruction
- By-product Conversion

![](_page_7_Picture_5.jpeg)

#### **Sulfur formation in the Reaction Furnace**

# **Claus reaction:** Acid gas 2H2S + SO2 1/2S2 + 2H2OHydrogenSulfurSulfurSulfur sulfide dioxide

![](_page_8_Picture_2.jpeg)

#### **Sulfur formation in the Reaction Furnace**

![](_page_9_Figure_1.jpeg)

![](_page_9_Picture_2.jpeg)

![](_page_10_Figure_0.jpeg)

#### **Ammonia destruction**

 $NH_3 + \frac{3}{4}O_2 \longrightarrow \frac{1}{2}N_2 + \frac{1}{2}H_2O$ 

![](_page_11_Picture_2.jpeg)

#### **Ammonia destruction**

$$NH_3 + \frac{3}{4}O_2 \longrightarrow \frac{1}{2}N_2 + \frac{1}{2}H_2O$$

![](_page_12_Figure_2.jpeg)

![](_page_12_Picture_3.jpeg)

# **Ammonia destruction**

Remaining NH<sub>3</sub> at MRF outlet:

- Expected < 20 ppm
- Guaranteed < 100 ppm

Provided:

- MRF operating temperature > 1300°C (2372°F)
- Residence time > 1 sec

![](_page_13_Picture_7.jpeg)

#### **Hydrocarbon destruction**

 $CH_4 + 2O_2 \longrightarrow CO_2 + 2H_2O$ 

![](_page_14_Picture_2.jpeg)

![](_page_15_Figure_0.jpeg)

![](_page_15_Picture_1.jpeg)

## **SRU Combustion Basics**

The degree of combustion depends on 3 factors, the three **T**'s of combustion:

- **T**emperature
- (Residence) Time
- Turbulence

![](_page_16_Picture_5.jpeg)

#### **SRU Temperature**

The overall temperature in the main reaction furnace depends on:

- Chemical reactions
  - Heat release and absorption
  - The stoichiometry
- Design conditions (set by process licensor)
  - Pre-heating of the combustion air / acid gas
  - Oxygen enrichment
  - Co-firing of fuel gas
  - Bypassing part of the amine acid gas

![](_page_17_Picture_10.jpeg)

#### **SRU Residence Time**

#### Minimum: determined by reaction kinetics

Longer: better destruction of impurities.

![](_page_18_Figure_3.jpeg)

![](_page_18_Picture_4.jpeg)

# **SRU Turbulence**

The flow pattern determines the shape of the flame, the degree of mixing as well as the flame stability. Mixing is achieved through:

- Burner geometry
  - E.g. physical restrictions, swirlers, constrictions, etc.
- Pressure drop
  - Higher pressure drop = more energy!
- Design principle
  - Pre-mixing vs. diffusion flame principle

![](_page_19_Picture_8.jpeg)

#### **Resulting Burner Requirements**

- Intense mixing of acid gas and oxygen
- Recirculation of flue gas

![](_page_20_Picture_3.jpeg)

#### **LMV Main Burner**

![](_page_21_Picture_1.jpeg)

![](_page_21_Picture_2.jpeg)

#### **LMV Main Burner**

![](_page_22_Picture_1.jpeg)

![](_page_22_Picture_2.jpeg)

![](_page_23_Picture_0.jpeg)

#### **LMV Burner Axial Velocity**

![](_page_24_Figure_1.jpeg)

Contours of Axial Velocity (m/s) Jun 17, 2011 ANSYS FLUENT 12.1 (axi, swirl, pbns, spe, RSM)

![](_page_24_Picture_3.jpeg)

#### **Turbulent combustion**

![](_page_25_Picture_1.jpeg)

![](_page_25_Picture_2.jpeg)

![](_page_26_Picture_0.jpeg)

![](_page_26_Picture_1.jpeg)