Octane Boost and Capacity Increase for Hydrotreated Naphtha

ExoS[™] - Extraction Desulfurization Technology

REFCOMM Galveston 2019

Brant Aggus Refining Technologist INVISTA Performance Technologies



KIKOCH-GLITSCH.

ExoS[™] - Sulfur Extraction Technology for Mid-Cut Naphtha

- A great investment for meeting 10 ppm sulfur limits in the blending pool
- Generates an olefin rich C6-C7 raffinate with less than 10 ppm Sulfur that bypasses the FCC naphtha hydrotreater for direct blending
- Value Drivers:
 - Can reduce full range FCC Naphtha RON loss to <1
 - *Reduces hydrotreater feed flow by up to 40% and H2 consumption by up to 50%*
 - Reduces or eliminates light FCC naphtha treatment and heavy naphtha posttreatment
 - ExoS[™] can treat C5 naphtha
 - Olefin bypass of the hydrotreater reduces mercaptan revision
 - For units already taking a mid-cut FCC napththa split pre-hydrotreater, ExoS[™] eliminates the need to over-treat heavy cut to blend down total sulfur
- Commercially proven success 8 units in operation and 7 in design
 - Can be installed with a new hydrotreater to reduce the size, CAPEX and OPEX of the hydrotreater
 - Can be installed as a revamp to save Octane and free up hydrotreater capacity



TOPICS

DEVELOPMENT AND BASIS

EXOS TECHNOLOGY OVERVIEW

BENEFITS OVERVIEW AND EXAMPLE

COMMERCIAL EXAMPLES AND SUMMARY

INVISTA / KOCH-GLITSCH PARTNERSHIP

ExoS™ DEVELOPMENT AND TECHNOLOGY BASIS



How Best to Desulfurize FCC Gasoline?

Desulfurization vs. Olefin Recovery

Lose olefins to hydrogenation? Or..... Find a way to recover them. Oil product optimization
Fuel upgrading to <10 ppm S





Traditional FCC Naphtha Sulfur Treating.....





(Fundamental research findings)

BASIS

Typical FCC Gasoline Analysis

| С | nP | iP | 0 | Ν | Α | Total | wt% | Olefin wt% |
|-------|-----|------|------|-----|------|-------|------|---|
| 4 | 0.1 | / | 0.6 | / | / | 0.7 | 87.5 | 1.6 |
| 5 | 1.2 | 7.8 | 18.0 | / | / | 26.9 | 66.8 | 44.2 |
| 6 | 1.1 | 5.9 | 11.9 | 2.0 | 0.8 | 21.6 | 55.0 | 29.3 |
| 7 | 0.9 | 2.2 | 4.3 | 3.2 | 3.7 | 14.3 | 30.3 | 10.7 |
| 8 | 0.4 | 2.7 | 3.6 | 1.8 | 6.4 | 14.9 | 24.2 | 8.9 |
| 9 | 0.3 | 1.6 | 1.4 | 1.3 | 7.8 | 12.3 | 11.2 | 3.4 |
| 10 | 0.2 | 0.7 | 0.7 | 0.2 | 4.0 | 5.7 | 11.7 | 1.5 |
| 11 | 0.3 | 1.5 | 0.1 | / | 1.0 | 3.0 | 5.4 | 0.4 |
| Total | 4.4 | 22.2 | 40.6 | 8.6 | 23.6 | 99.4 | / | 100.0 |
| | | | | | | | | si di seconda di second |

Mercaptans are Treated with Existing Technology - • C5 Olefins : 40~50 wt%

VISTA[™]

But what about these? • C6-C7 Olefins: ~40 wt%

(Fundamental research findings)

BASIS

Typical Sulfides Distribution in FCC gasoline

| Component | BP, °F | ppmw |
|-----------------|---------|------|
| cos | -58 | 0.9 |
| C2SH | 95 | 5 |
| DMDS | 99 | 2.5 |
| CS ₂ | 117 | 1.4 |
| C3Thiol | 133-154 | 9.2 |
| C2H6S | 149 | 0.3 |
| C4SH | 149-208 | 2.2 |
| Thiophene | 183 | 113 |
| C2H6S2 | 230 | 0.8 |
| IC5SH | 243 | 0.4 |
| Methylthiophene | 237 | 241 |

| Component | BP, °F | ppmw |
|-------------------|--------|------|
| Tetrahydrothiphn. | 246 | 25.4 |
| Ethylthiophene | 271 | 40.5 |
| Dimethylthiophene | 273 | 205 |
| Hexathiol | 304 | 19.6 |
| C Hexasulfide | 295 | 19.8 |
| Trithiophene | 316 | 180 |
| Octathiol | 390 | 11.2 |
| C Octasulfide | 365 | 4.4 |
| Tetrathiophene | 358 | 108 |
| | | |
| Total | | 1000 |



- Thiophenic Sulfur: 91%
- Distributed in: 175~275 °F Range



(Fundamental research findings)

BASIS





Solubility Advantage

With molecular properties of PONAS, mid cut naphtha feed is separated into PNO rich and AS rich oil, with S rich oil sent to Hydrotreating. Most of olefin is not sent to HDS unit, so that olefin is *not saturated*.

| НС | Benzene | Toluene | Cyclohexane | Every other HC |
|-----------------|-----------|----------------------|-------------|-------------------|
| Rel. Solubility | 8.0 | 4.8 | 2.0 | <1.0 |
| Sulfide | Thiophene | Methyl- Thiophene | Thioether | Mercaptan |
| Rel. Solubility | 10.5 | 5.2 | 5.0 | 4.7 |



ExoS[™] Technology Overview





4-3-2 of ExoS Technology





- 1. Light olefin
- 2. Process water
- 3. Solvent





Olefin separation
Solvent circulation



Simplified Flow Scheme for ExoS Process



Benefits Overview and Example



Hoekstra multi-client group has done field tests on 11 different posttreaters





Hoekstra model estimates ExoS[™] will save 3-4 RON on these units





| Commercial Example | | | | | | | nP | iP | 0 | N | A | sum | | |
|--------------------|--|-------------|---------|----------|---------|-------|-------|------|------|------|-------------|-------|------|-------|
| | | | | | | | 5 | 1.4 | 1.6 | 7.2 | 0.5 | 0 | 10.7 | |
| Kannale | | | | | 6 | 5.8 | 14.0 | 33.7 | 7.5 | 0 | 61.0 | | | |
| MCN Feed | | | | | | 7 | 3.4 | 9.9 | 7.6 | 6.8 | 0 | 27.7 | | |
| | (• | | 01 1012 | in ree r | aprici | ia) | | 8 | 0 | 0.3 | 0.1 | 0.2 | 0 | 0.6 |
| | and the second | | | | Extract | | 10.6 | 25.8 | 48.6 | 15.0 | 0 | 100.0 | | |
| | | | | S | | | 8.0 p | pmw | | · | | | | |
| | nP | iP | 0 | N | A | sum | | | | | | | | |
| 5 | 1.2 | 1.3 | 6.1 | 0.4 | 0.0 | 9.0 | | nP | iP | 0 | Ν | J | Α | sum |
| 6 | 4.9 | 11.7 | 29.5 | 6.5 | 6.7 | 59.2 | 5 | 0 | 0 | 0.8 | 3 (|) | 0 | 0.8 |
| 7 | 3.1 | 8.4 | 7.3 | 6.3 | 2.5 | 27.6 | 6 | 0.2 | 0.1 | 8.8 | 3 1. | 6 3 | 39.7 | 50.4 |
| 8 | 0.1 | 0.5 | 0.5 | 0.5 | 0.5 | 2.0 | 7 | 1.4 | 1.2 | 6.1 | L 3. | 6 1 | 4.7 | 27.0 |
| 9 | 0.1 | 0.2 | 0.3 | 0.1 | 0.6 | 1.3 | 8 | 0.7 | 1.3 | 2.3 | 3 1. | 8 | 3.0 | 9.1 |
| 10 | 0.1 | 0.1 | 0.2 | 0.1 | 0.4 | 0.8 | 9 | 0.6 | 1.0 | 1.8 | 3 0. | 8 | 3.7 | 7.9 |
| | 94 | 22.2 | 43 9 | 13 9 | 10 7 | 100.0 | 10 | 0.5 | 0.8 | 0.9 | 0. | 4 | 2.2 | 4.8 |
| C | 5.7 | <i>LL.L</i> | 200 0 | 10.0 | 10.7 | 100.0 | | 3.4 | 4.4 | 20. | 7 8. | 2 6 | 3.3 | 100.0 |
| 3 | | | 380.0 | hhum | | | S | | | 221 | 2.4 pp | mw | | |
| | | | | | | | | | | | | | | |

(All values are wt%)

INVISTA[®]

Commercial Example, 6.8 MBPD Mid-Cut Naphtha

| | Feed | Raffinate | Extract |
|--------------------------|-------|-----------|---------|
| Flow rate, Mlb/hr | 70.6 | 58.7 | 11.9 |
| Percentage, wt% | 100.0 | 83.1 | 16.9 |
| Olefin content, wt% | 43.9 | 48.6 | 20.7 |
| Olefin flow rate, Mlb/hr | 30.9 | 28.5 | 2.4 |
| Olefin split, % | 100.0 | 92.1 | 7.9 |
| Sulfur content, ppmw | 380.0 | 8.0 | 2212.4 |
| Elemental S split, % | 100.0 | 1.8 | 98.2 |

- Olefin Recovery: 92.0%
- Sulfur Recovery: 98.2%



Utility Consumption

| | | Consumption (/ton feed) | | | |
|---|----------------|----------------------------|------|--|--|
| | | unit | Cons | | |
| 1 | Cooling water | ton | 14.7 | | |
| 2 | Power | Kw∙h | 10.5 | | |
| 3 | 300 psig steam | ton | 0.3 | | |
| 4 | Condensate | ton | -0.3 | | |
| 5 | N2 | scf | 64.0 | | |
| 6 | Instrument air | scf | 64.0 | | |
| | | | | | |

Low energy consumption, low cost



Key Advantages , ExoS[™] vs Hydrotreating Alone

| | ExoS | HDS Alone |
|-------------------------------|----------------------------------|-------------------------------|
| Product S | <10 ppmw | <10 ppmw |
| Ron Loss (A) | 0.5-1.5 (worth \$31 USD/t) | 2.0-4.0 (\$0 benefit-base) |
| H2 Consumption | 1/3-1/2 | 1 (base) |
| Selective Hydrogenation Ratio | 45 wt% | 80% |
| Product Loss | 0.2-0.4 wt% (worth \$6 USD/t) | 0.8 wt% (\$0 benefit-base) |
| Capex (B) | 45MM USD | 45 MM USD |
| Орех | \$17 USD/t | \$19 USD/t |
| \$ Benefit | \$39 USD/t | \$0 - base |

- (A) Based on gasoline spec w/ <10 ppm S requirement.
- (B) Based on 1000 kTPA plant capacity, built in China.



Environmental Benefits

No wastes

Solvent consumption: 1lb/100Mlb gasoline





Can be coupled with existing hydrotreating tech



 \sim 50% FCC gasoline to be hydrotreated with ExoS vs \sim 80% FCC gasoline to be hydrotreated without

Process can drop into an existing plant

Can revamp aromatics extraction units



Commercial Examples and Summary



Client: A Chinese refinery

Capacity: 600 kta (FCC Gasoline Upgrading ExoS Project)

Start up: Jan. 2015

RON loss: < 1.0 (vs original 4.0) Sulfur content: < 5 ppm





Client: A PetroChina Refinery

Capacity: 350 kta

Start up: Oct. 2016

RON loss saving: ~4 Sulfur content: < 10 ppm





Client: A ChemChina Refinery

Capacity: 1,100 kta

Start up: Nov. 2016

RON loss: < 1.5 Sulfur content: < 5 ppm





INVISTA / Koch-Glitsch Partnership





| Commodity Trading | Minerals | | | |
|---|--|--|--|--|
| Electronic Components | Polymers and Fibers (IPT) | | | |
| Energy | Ranching | | | |
| Fertilizers | Refining, Chemicals and Biofuels (FHR) | | | |
| Forest and Consumer Products | Glass | | | |
| Process and Pollution Control Equipment and Technologies (KG-JZ) | | | | |

KOCH-GLITSCH.

**Koch revenues fluctuate with the price of commodities. They have been estimated by Forbes as high as \$115 billion.

Georgia Pacific

INVISTA"

molex

GUARDIAN

IPT – KG Partnership

IPT is INVISTA's technology transfer business with more than 40 years in continuous licensing

Licensed more than 100 license projects for PTA, Polyester, BDO, PTMEG and Nylon 66 since joining KII in 2004

Supporting technology development, commercialization and licensing within KII since 2013

Entry into the refining space spawned by collaborations with KII Affiliates ... Flint Hills Resources and Koch-Glitsch

IPT-KG Partnership to Offer Exos[™], DTL[™], IsoA[™] and other Refining Technologies to the Market









Summary

- ➤ Exos[™] is an advantaged option for meeting 10 ppmw Tier 3 Sulfur Limits
 - Generates an olefin rich C6-C7 raffinate with less than 10 ppm Sulfur
 - Reduces Octane loss to <1</p>
 - Reduces hydrotreater feed flow by up to 40%, and
 - Reduces hydrotreater H2 consumption by up to 50%
- We'd appreciate the opportunity to provide a detailed proposal to meet your specific needs
- > Questions?



THANK YOU

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