## Feed Entry Systems For The Modern Delayed Coking Unit

International Refcomm

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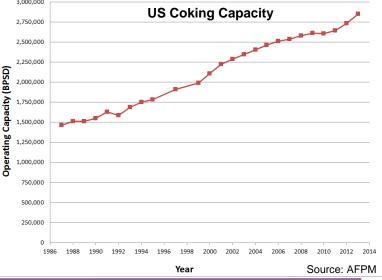




# **Delayed Coking**

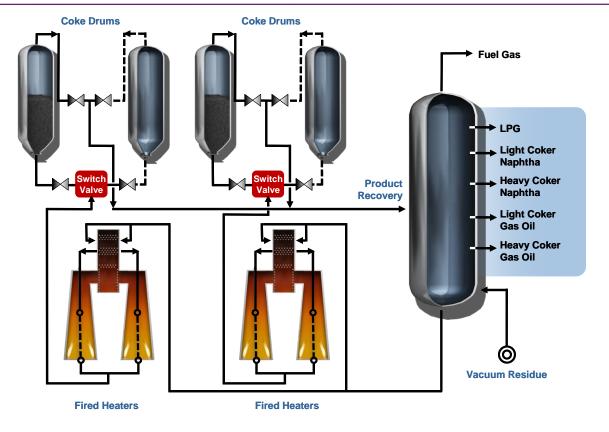
- Most commonly used residue upgrading process
  - Over 5,500,000 BPSD installed capacity
  - Amec Foster Wheeler is market leader
- Very attractive economics
- Complete residue conversion
  - Gas
  - Naphtha
  - Gas oils
  - Coke (disposal not an issue)
- Specialty coke production
- Maximized diesel yield with Hydrocracker integration
- Wide variety of feedstocks





## Delayed Coking Process Simplified Flowscheme





- Continuous batch process
- Typical cycle is 18 hour fill and 18 hour empty
- Extensive thermal and mechanical stresses on coke drums



## **Traditional Coke Drum Design**

- Utilized central, bottom feed entry
- "Uniform" upward flow in coke drum
- Bottom unheading was a difficult and dangerous task
  - Manpower intensive
  - Time consuming



Photograph courtesy of DeltaValve

## **Traditional Bottom Unheading**





Photographs courtesy of DeltaValve



# Semi-Automated Bottom Unheading Systems



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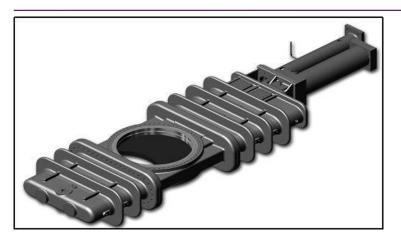
## **Problems with Bottom Unheading**



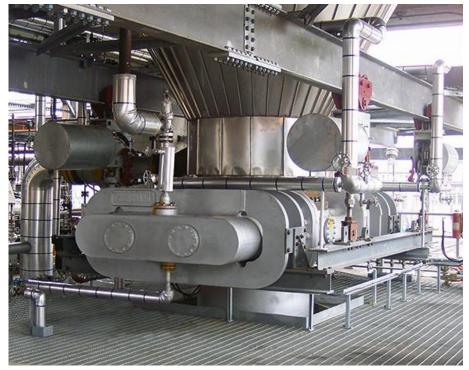
Photographs courtesy of DeltaValve



# Slide Valve Bottom Unheading Systems



- Developed by DeltaValve
- Revolutionized DCU operations
  - Fully automatic
  - Safe
  - Cleaner

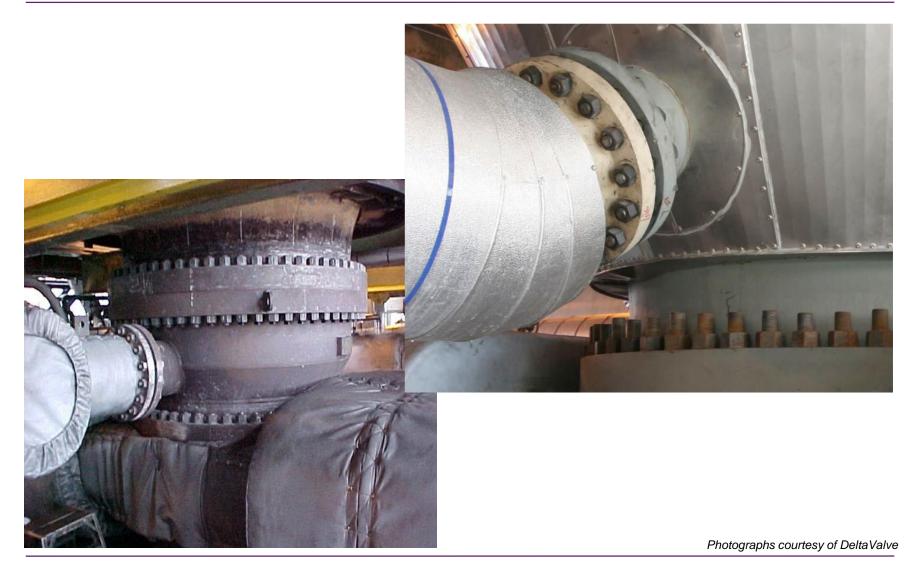


- However introduced a new problem
  - How to introduce feed into the coke drum

Photographs courtesy of DeltaValve

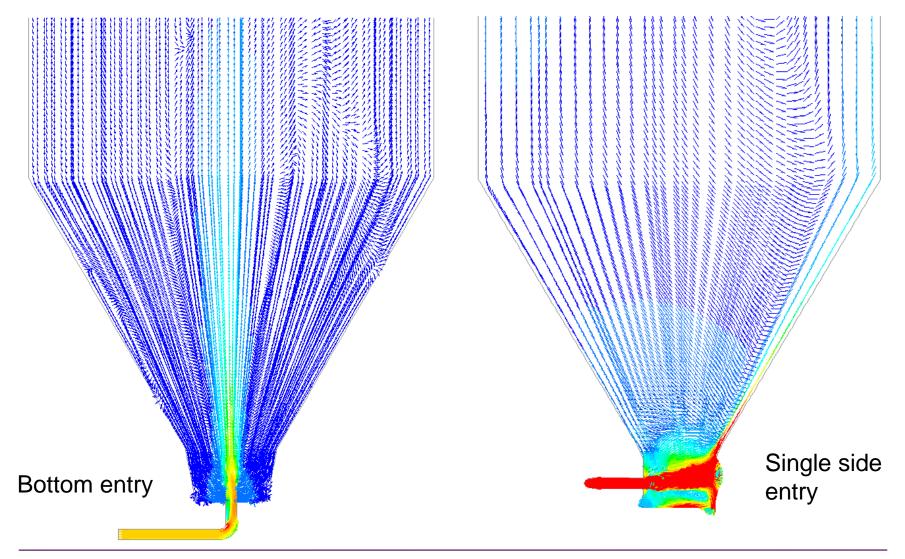


## Single Side Feed Entry



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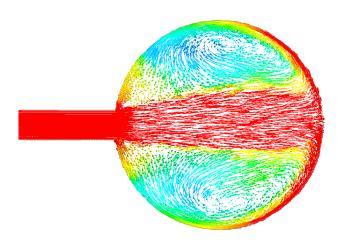


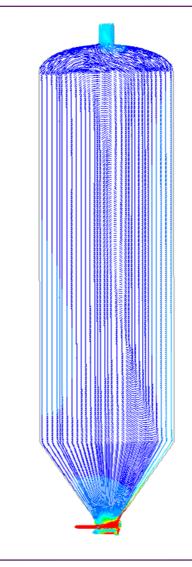




# Issues With Single Side Entry Feed Systems

- Non-uniform flow in the coke drum
- Non-uniform temperature profiles
  - Enhanced banana movement
  - Enhanced thermal fatigue
- Hot spots
- Blow-outs
- Vibration

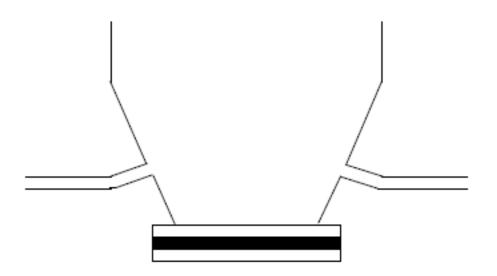






#### **Dual Feed System**

Claims more uniform flow than in single side entry systems





## **Dual Feed System**

- Claims more uniform flow than in single side entry systems
  - Not necessarily the case due to interactions of streams
- Issues
  - More complicated piping runs around coke drums
  - Equalization of flow
  - Deformation of BUD attachment flange leading to leaks

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#### Introducing the DeltaValve Center Feed Device



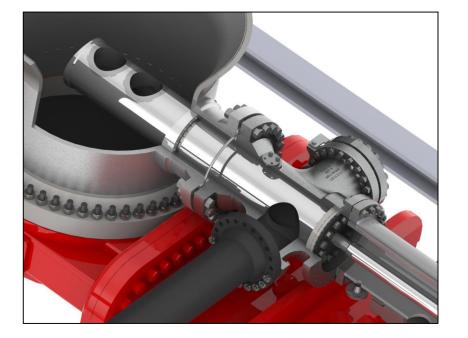
- Simulates traditional bottom feed entry
- Based on slide valve unheading technology

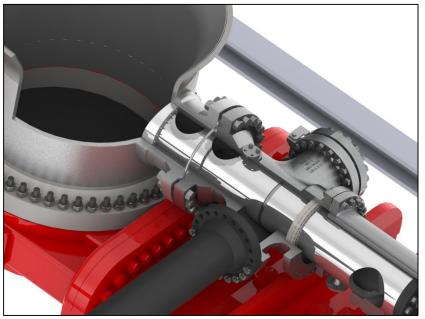


Photograph courtesy of DeltaValve

#### **Center Feed Device**







Photographs courtesy of DeltaValve



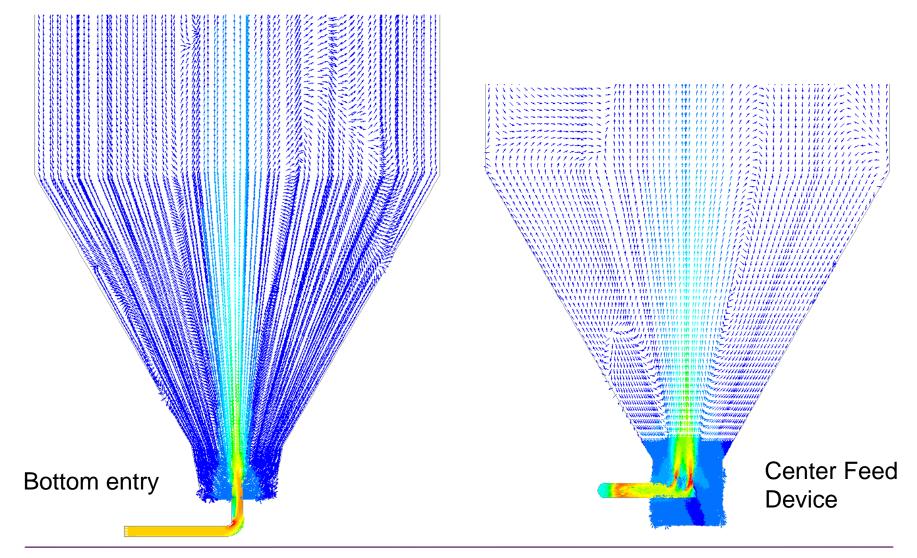
#### **Center Feed Device**

- Commercially operating (over 5 years successful operation) in 3 locations
- Benefits observed
  - Minimum to zero banana effect
  - Drastic reduction in frequency of hot spots and blowouts
  - Low differential thermal gradients observed during coking and quenching



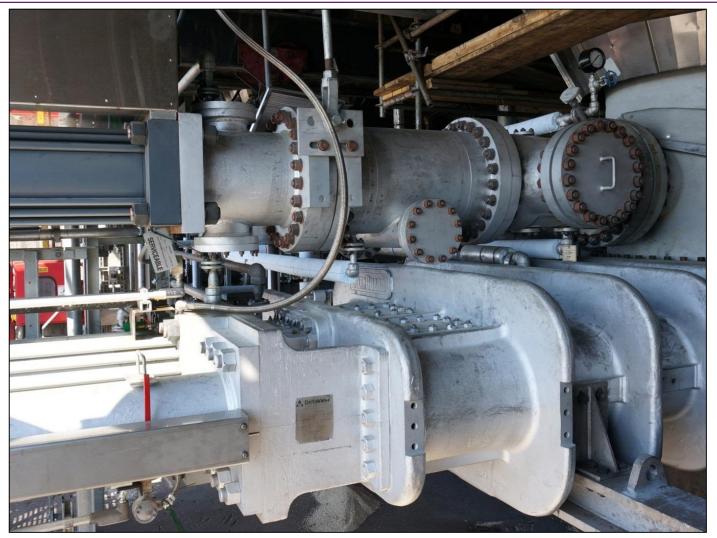
Photograph courtesy of DeltaValve





## **Center Feed Device Installation**

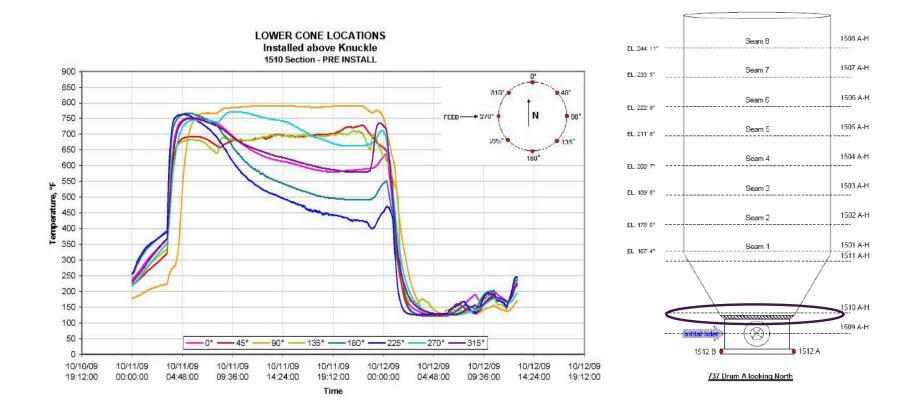




Photograph courtesy of DeltaValve

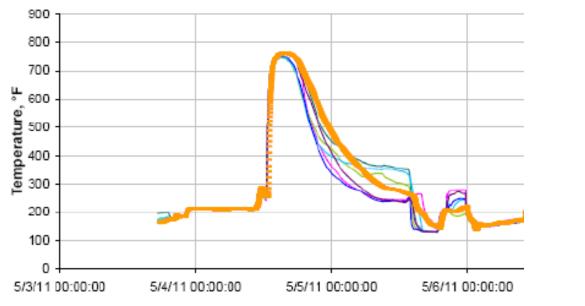
## Coke Drum Temperature Profiles Side Entry

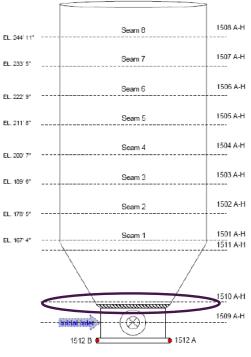




## Coke Drum Temperature Profiles Center Feed Device



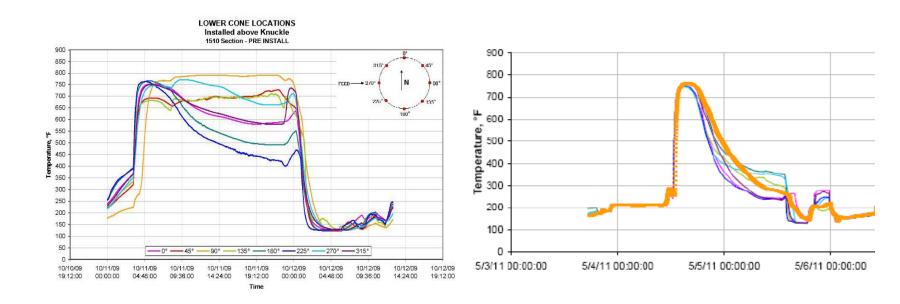




737 Drum A looking North

## Temperature Profile Improvement With Center Feed Device



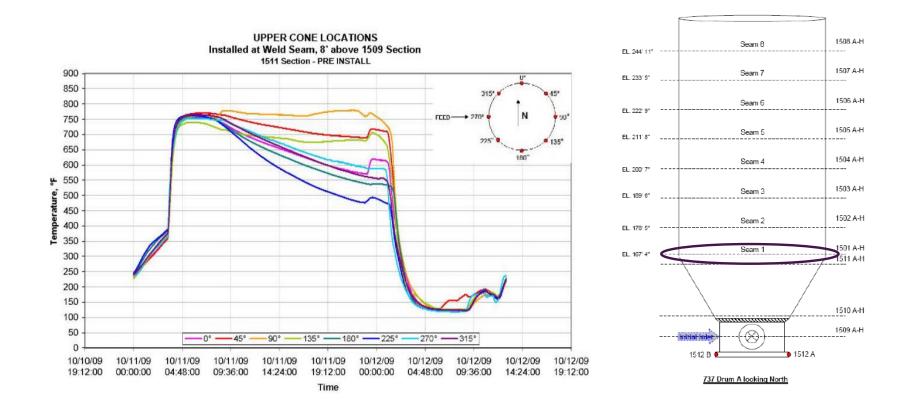


- Large circumferential temperature gradients
- Non-uniform flow in the drum

- Uniform temperature gradients
- Uniform flow
- Coke insulation layer
- Lower wall cooling rates during quench

## Coke Drum Temperature Profiles Side Entry





## Coke Drum Temperature Profiles Center Feed Device



1508 A-H

1507 A-H

1506 A-H

1505 A-H

1504 A-H

1503 A-H

1502 A-H

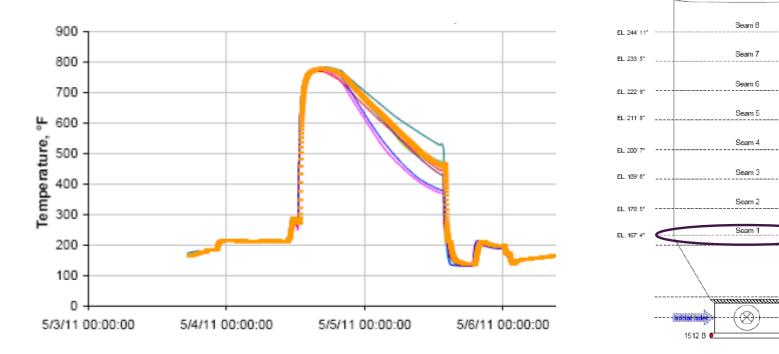
501 A-H

1511 A-H

1510 A-H

1509 A-H

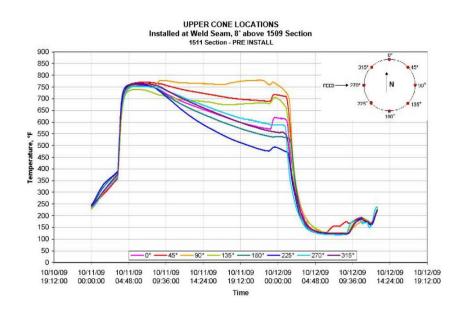
1512 A



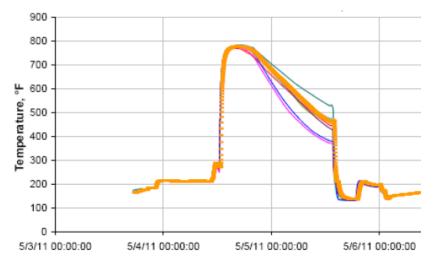
737 Drum A looking North

## Temperature Profile Improvement With Center Feed Device





- Large circumferential temperature gradients
- Non-uniform flow in the drum



- Uniform temperature gradients
- Uniform flow
- Coke insulation layer
- Lower wall cooling rates during quench



## **Coke Drum Movement**

- Circumferential temperature gradients result in "Banana Movement" of the drum
- The Banana Movement can be calculated

 $BM = 1.2 X (R + 0.5D) X (1 - \cos \alpha)$ 

where 
$$\alpha = \frac{57.2956 X \gamma X L X (T_h - Tc) X (1 + \gamma X Tc)) X \pi}{(180 X D)}$$
  
and  $R = \frac{D}{(\gamma X (Th - Tc))}$ 

- D = coke drum diameter
- L = coke drum length
- $T_h$  = hot side temperature
- $T_c = cold side temperature$
- $\gamma$  = coefficient of thermal expansion



#### **Banana Movement**

Condition	Calculated Banana Movement (in)	Observed Banana Movement (in)
Side entry	6.7	~ 6
Center Feed Device	3.1	~ 3

The Center Feed Device results in a significant reduction in the Banana Movement of the coke drum



- In March 2016 DeltaValve and Amec Foster Wheeler entered into an alliance to promote, sell and install the Center Feed Device
  - Amec Foster Wheeler fully endorses the Center Feed Device
  - The Center Feed Device is now Amec Foster Wheeler's standard feed entry system for all new DCUs
  - Both DeltaValve and Amec Foster Wheeler can sell the Center Feed Device into existing units
  - Amec Foster Wheeler can provide the necessary engineering to support a Center Feed Device retrofit
  - Amec Foster Wheeler can provide installation services for retrofits

## Summary



- Traditional and current coke drum feed entry systems have issues
  - Safety
  - Environmental
  - Coke drum life
- The Center Feed Device improves coke drum operation
  - More uniform temperature gradients
  - Reduced thermal and mechanical stress on the drums
  - Reduced Banana Movement of the coke drums
  - Reduced maintenance and operational costs
  - Demonstrated performance
- DeltaValve and Amec Foster Wheeler have formed an alliance to promote the Center Feed Device



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