



**Coking.com**

Galveston, TX May 2-6, 2011



## Stop Throwing Money Away in the Coker Unit!

Thomas Willingham, PE  
Controls Southeast, Inc.

[willingham@csiheat.com](mailto:willingham@csiheat.com)

---

---

---

---

---

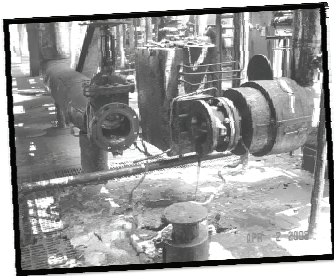
---

---

---

## Feedback from coker units

Chevron • CNRL • ConocoPhillips • Hovensa • Lyondell • Marathon • PetroCanada •  
Shell • Suncor • Total



Flushing oil  
Missed coker cycles  
Ceramic heat blankets  
600 psig steam

2



---

---

---

---

---

---

---

---

## Problems emerge over time



Plant start-ups focus on conversion rates, chemistry, and  
coke morphology... not on stress testing the thermal  
maintenance system

3



---

---

---

---

---

---

---

---

## Agenda



1. What are the problems?
2. Why are there problems?
3. How much do the problems cost?
4. Is there a better way?

4



---

---

---

---

---

---

---

---

1

## What are the problems?



5



---

---

---

---

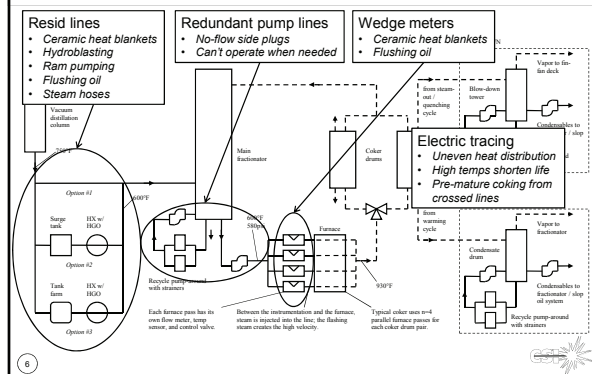
---

---

---

---

## Reported plugging areas



6



---

---

---

---

---

---

---

---

2

Why are there problems?



7



---

---

---

---

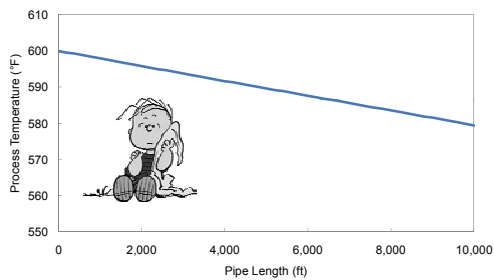
---

---

---

No heat needed if flowing

Coker Feed Flowing Through 8" Line Without Heating



8



---

---

---

---

---

---

---

No flow/ melt out = design condition **#1**

- No-flow condition is common...
  - Bypass lines (NNF)
  - Turnarounds
  - Upsets



→ **Need melt-out capability!**

9



---

---

---

---

---

---

---

## Inadequate specifications #2

- Typical P&ID:
  - “Heat Trace”, “Heavy Tracing”
- Problem?
  - Does not specify what outcome is required!
  - A single tube trace could be used and meet spec
  - Need to define more specific requirement:

Steam tracing design basis: (1) Maintain process at 325F during no flow and (2) raise process temperature from ambient to 325F within 12 hr after loss of utilities. Vendor is required to supply calculations to show compliance.

10




---

---

---

---

---

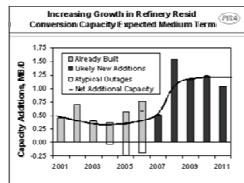
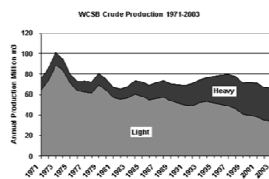
---

---

---

## Heavier resid makes it worse #3

**HEAVIER CRUDE SOURCES** + **MORE EFFICIENT PROCESSING** = **HEAVIER RESID TO COKER**



11




---

---

---

---

---

---

---

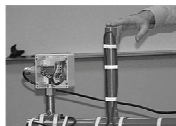
---

## Historical heating methods ineffective #4

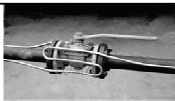
Tube Tracing



Electric Tracing



Both give the illusion of “working” when lines are flowing!



$$q = U \times A \times \Delta T$$

$$q = \text{Constant} = q_{\text{ambient\_loss}} + q_{\text{process}}$$

12




---

---

---

---

---

---

---

---



## Low expectations of heating system

- Common Coping Mechanisms:
  - Flushing oil procedures to clear lines
  - Ceramic heat blankets
  - Hydro-blasting or other mechanical removal
  - Steam hoses
  - Ram pumping

**Workarounds Common – Why Tolerated?**

13



---

---

---

---

---

---

---

---



## How much do the problems cost?



14



---

---

---

---

---

---

---

---

## Operational cost impact

Operational Cost	\$ Impact
<b>Flushing oil</b> <i>(prevent plugging prior to pending known downtime)</i>	
<b>Missed coker cycles</b> <i>(dependent on drum size, coke margin)</i>	
<b>Plugging removal</b> <i>(insulation removal/replacement; ceramic blankets)</i>	

15



---

---

---

---

---

---

---

---

4

Is there a better way?



16



---

---

---

---

---

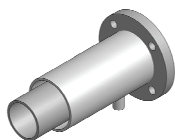
---

---

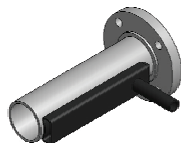
---

### Different heating approaches

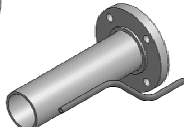
Jacketed Pipe



ControTrace™



Tube/Electrical  
Tracing



$$q = U \times A \times \Delta T$$

17



---

---

---

---

---

---

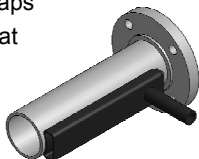
---

---

### ControTrace

- 2"x1" rectangular tubing is banded onto piping
- Designed with ASME Section VIII
- Contoured to fit pipe OD
- Heating medium flows through tracing
- HTC used to remove air gaps
- Add elements for more heat

$$q = U \times A \times \Delta T$$



18



---

---

---

---

---

---

---

---

## ControTrace on piping



19



---

---

---

---

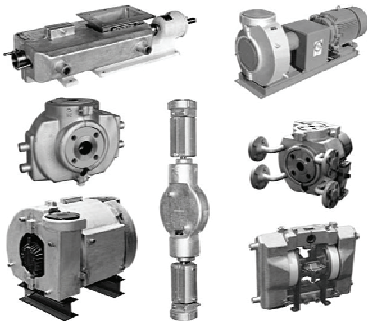
---

---

---

---

## ControHeat for components



20



---

---

---

---

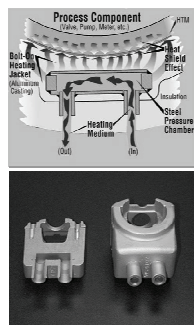
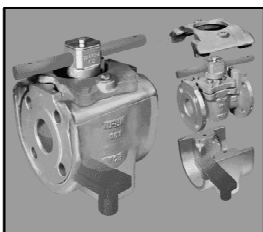
---

---

---

---

## How ControHeat works



21



---

---

---

---

---

---

---

---

### Higher U and A with CT

$$q = U \times A \times \Delta T$$

TT	U = 1
CT	U = 40

Diagram illustrating a circular vessel with a Temperature Transmitter (TT) on the left and a Control Transmitter (CT) on the right.

---

---

---

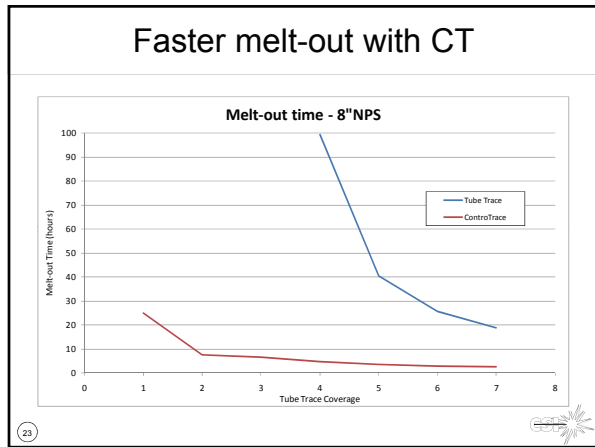
---

---

---

---

---




---

---

---

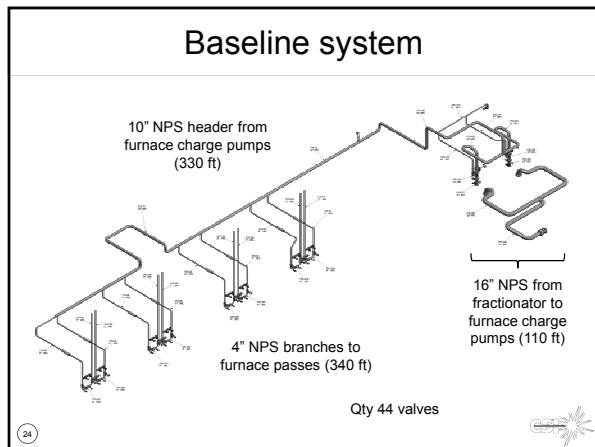
---

---

---

---

---




---

---

---

---

---

---

---

---

## Consider all the costs!



Heating system cost

### Ongoing Costs:

1. Flushing oil
2. Missed Coker cycles
3. Ceramic heat blankets
4. HP (600psig) steam

25



---

---

---

---

---

---

---

---

## Summary & recommendations

- Specify required thermal duty for the system
- Require vendors to perform engineering to:
  - Meet thermal duty
- When evaluating a heating system, consider:
  - Will it be able to melt out?
  - Will it keep the process from plugging in no flow?
  - Capital cost of an engineered solution versus the ongoing costs of plugging

26



---

---

---

---

---

---

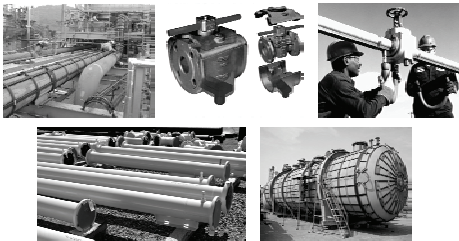
---

---

## CSI general overview

### 1. Heated piping systems

- ControTrace™ & ControHeat™ bolt-on jacketing systems
- Jacketed piping
- Flexible metal hoses (jump-overs and jacketed)



27



---

---

---

---

---

---

---

---

## CSI general overview

1. Heated piping systems
- 2. Process piping**
  - Up to 200 spools/week



28



---

---

---

---

---

---

---

---

## CSI general overview

1. Heated piping systems
2. Process piping
- 3. Specialty fabrication**
  - Code pressure vessels
  - Precision manifolds
  - Skids/modules



29



---

---

---

---

---

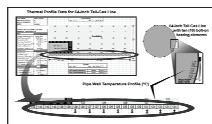
---

---

---

## CSI general overview

1. Heated piping systems
2. Process piping
3. Specialty fabrication
- 4. Engineering services**
  - Manifold-to-manifold responsibility
  - Thermal and fluid modeling
  - Piping and pressure vessel design
  - Project integration



30



---

---

---

---

---

---

---

---