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### **Agenda**

- A few words about Haldor Topsoe
- Handling sulfurous streams
  - ✓ the traditional way
  - ✓ the WSA way
- Introduction to WSA technology
- WSA process and lay-outs
- References
- Summary



### **Haldor Topsoe Company**

- Established in 1940 by Dr. Haldor Topsoe. Private 100% family owned company
- Global market leader in heterogeneous catalysis with a 75 year long track record
- ~2,700 employees in 11 countries across five continents.
- HQ in Lyngby, Denmark, HT Inc. located in Houston ~~250 employees





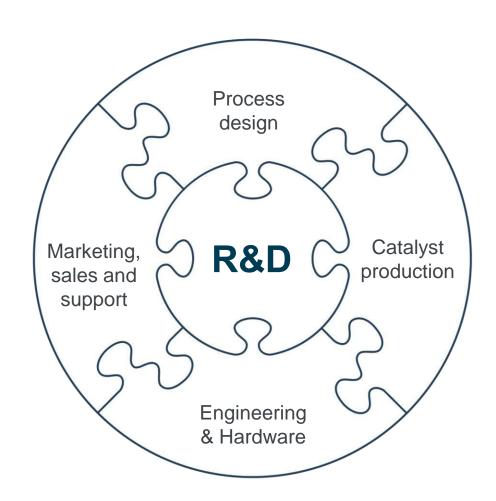
#### Services:

- Catalysts
- Technology/licensing
- Engineering
- Hardware
- Operation assistance



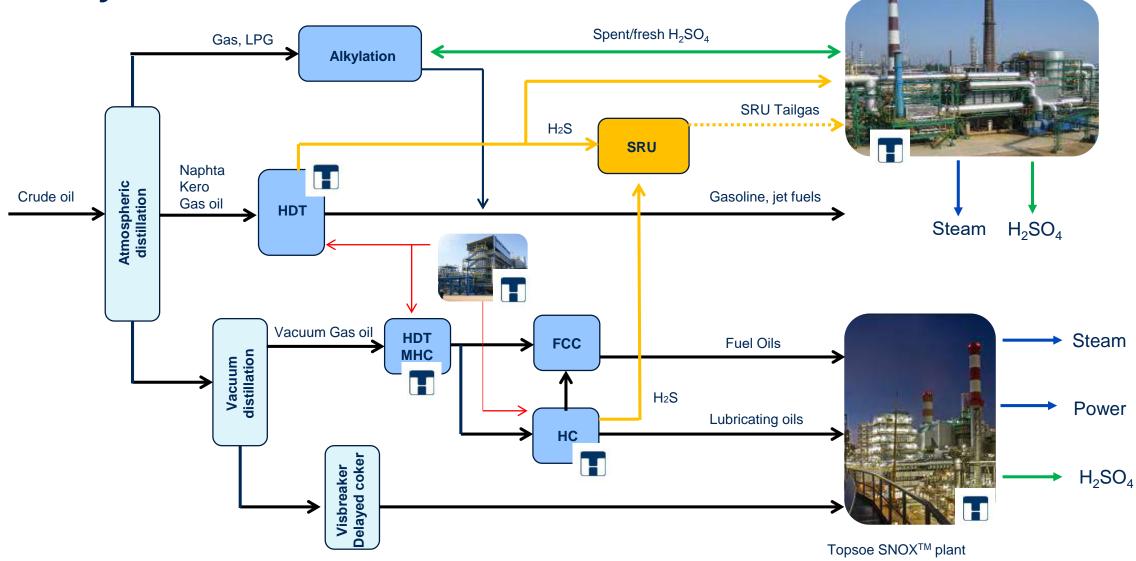
#### Synergies in the Topsoe business model

- Founded on the belief that applied fundamental research is key to build and retain a leading position in catalysis and technology supply
- Basic research and catalyst characterization done by 300+ world class scientists
- Approx. 10% of revenues annually applied to support R&D efforts
- Bringing science to the market
- Improving our products through costumer interaction



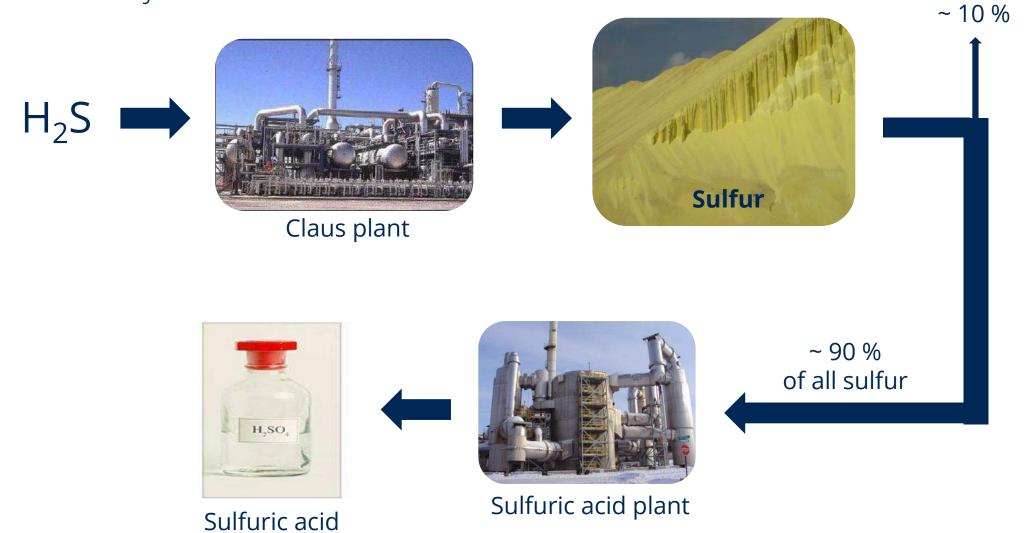
# **Refinery Overview**

#### Topsoe WSA plant



# What to do with H<sub>2</sub>S?

The traditional way



Other uses

of sulfur

# What to do with H<sub>2</sub>S?

The direct way

H<sub>2</sub>S



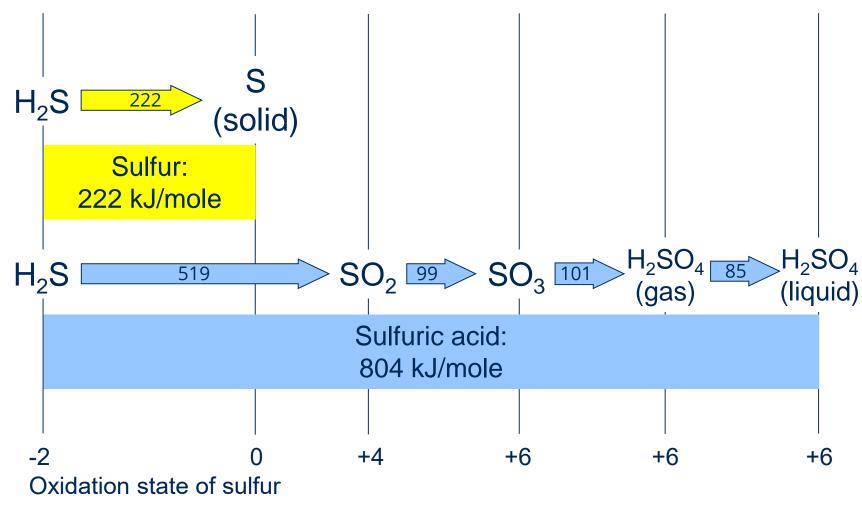
Sulfuric acid



Sulfuric acid plant (WSA)

#### Four times more energy

when producing sulfuric acid instead of sulfur



### Limitations when producing sulfur in a Claus plant

- Minimum H<sub>2</sub>S content in feed gas of 20 vol.-%
- Other combustibles than H<sub>2</sub>S (like NH<sub>3</sub> and hydrocarbons) make air control more complex



- Ammonia requires very high furnace temperature
- Hydrocarbons give risk of carbon formation and catalyst deactivation
- COS and CS<sub>2</sub> require special design
- Sulfur solidifies below 120°C and gets viscous above 160°C.

# **Comparison WSA vs. Claus**

Operating expenses (OPEX)

3 x more steam	
and better quality	/

Item	Unit price	Topsoe's WSA technology		Claus technology	
	USD	Production/day	USD/year	Production/day	USD/year
Sulfur, MT	80			100	2,640,000
Sulfuric acid, MT	40	306	4,040,000		
HP steam, MT	20	710	4,690,000		
MP steam, MT	12			225	891,000
Production revenues, USD/year			8,730,000		3,530,000
		Consumption/day	USD/year	Consumption/day	USD/year
Fuel gas, Nm³	0.28			6,100	563,000
Cooling water, m³	0.01	2,800	9,000		
Electric power, KWh	80.0	37,000	976,800	6,400	169,000
Waste water, MT	10			57	188,000
Production cost, USD/year			985,800		920,000
Net income, USD/year			7,740,000		2,600,000

#### **Comparison WSA vs. Claus**

#### Summary

- WSA offers larger revenues and less CAPEX
- WSA produces 3 times as much steam; this means saving in fuel consumption and CO<sub>2</sub> emissions
- WSA produces HP steam; Claus produces mostly MP steam
- WSA handles NH<sub>3</sub>, COS and hydrocarbons
- DeNOx is conveniently included in the WSA process, when required
- Smaller plot area for WSA than for Claus
- Less equipment is required
- WSA is simple and easy to operate.





#### What is WSA - Wet gas Sulfuric Acid

A process for cleaning sulfur containing streams under production of concentrated sulfuric acid

Lean H<sub>2</sub>S gas Rich H<sub>2</sub>S gas SRU tail gas SWS gas  $SO_2$ SO<sub>3</sub> Elemental sulfur CS<sub>2</sub> / COS Spent H<sub>2</sub>SO<sub>4</sub>



- ...No need to dry the gas
- ...No water consumption
- ...No need to use chemicals or other additives
- ...No generation of waste products
- ...With high energy efficiency.

#### **WSA process lay-out**

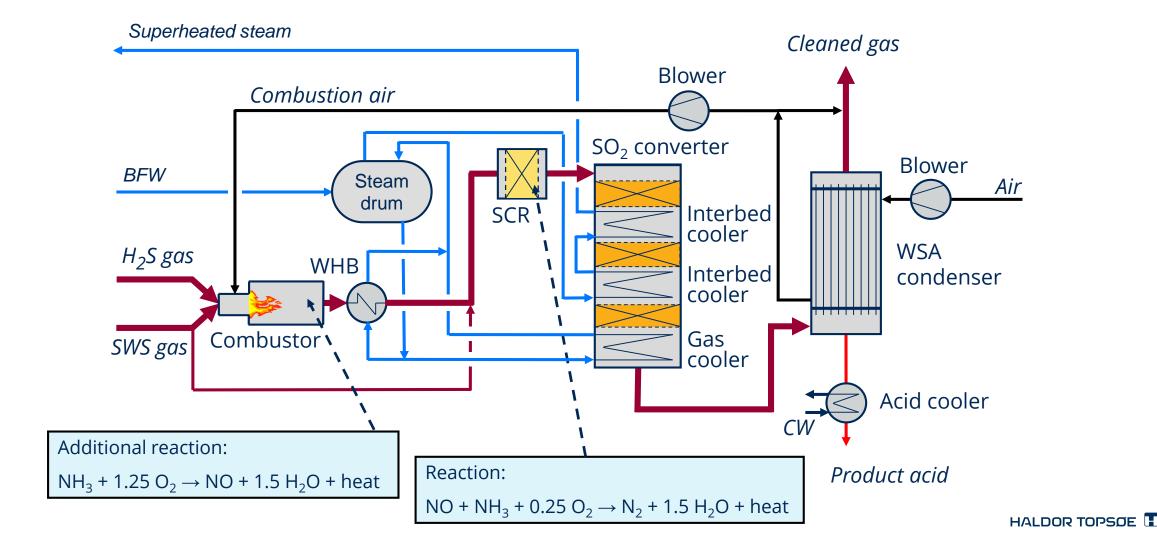
H<sub>2</sub>S gas Reaction:  $H_2SO_4(g) \rightarrow H_2SO_4(liq) + heat$ Superheated steam Cleaned gas Blower Combustion air SO<sub>2</sub> converter Blower **BFW** Steam Air drum Interbed cooler **WSA WHB** Interbed condenser  $H_2S$  gas cooler Combustor \ Gas cooler 11/ Reaction: Acid cooler  $H_2S + 1\frac{1}{2}O_2 \rightarrow SO_2 + H_2O + heat$ Reaction: Reaction: **Product** acid

 $SO_3 + H_2O \rightarrow H_2SO_4(g) + heat$ 

 $SO_2 + \frac{1}{2}O_2 \rightarrow SO_3 + heat$ 

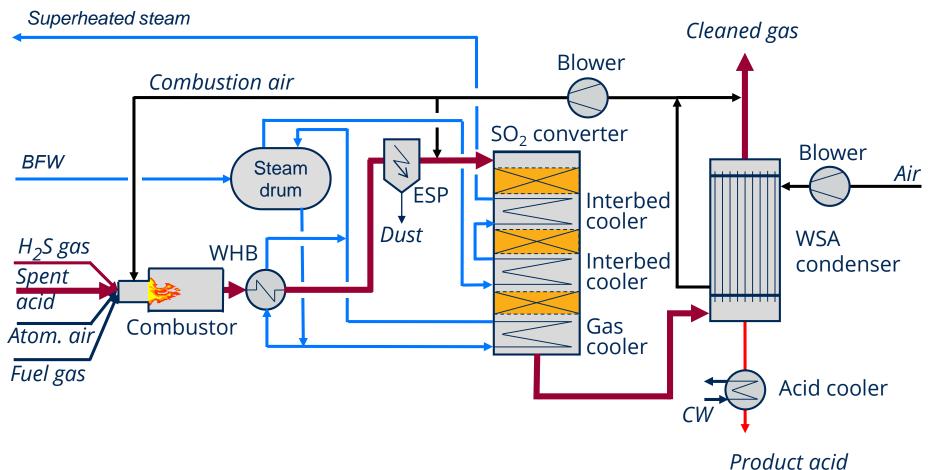
#### **WSA** process lay-out

H<sub>2</sub>S gas + SWS gas



# **WSA process lay-out**

# Spent acid regeneration



# SO<sub>2</sub> conversion catalyst series VK-W

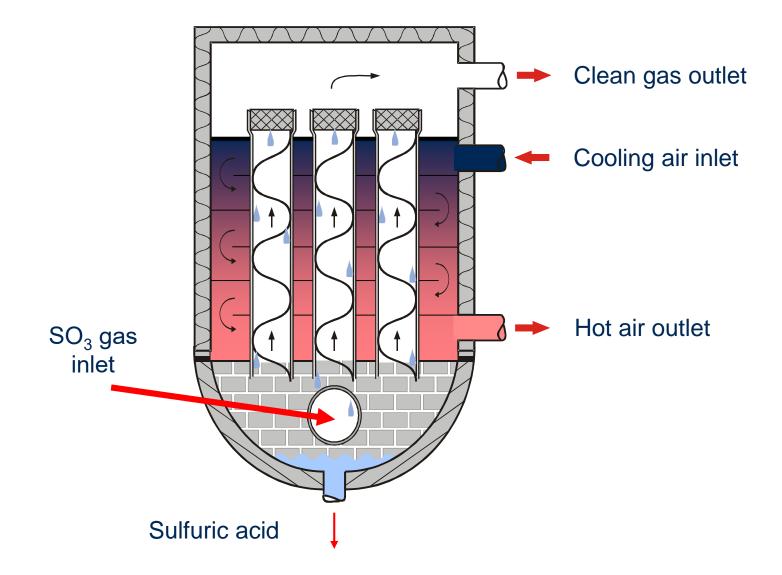


VK-WSX / VK-WL 9 mm Daisy

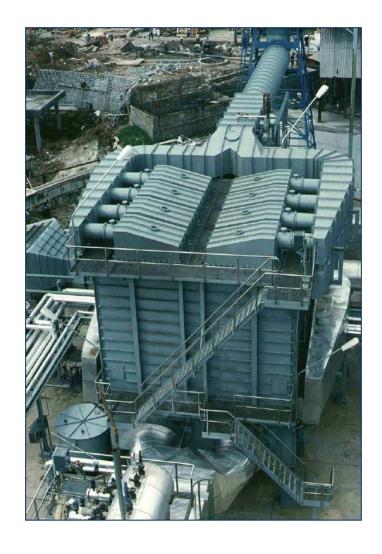
VK-WSA 25 mm Daisy

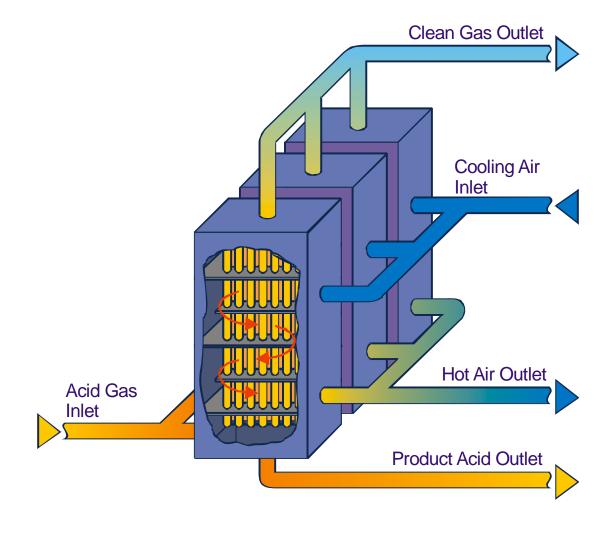
VK-WSA / VK-WH 12 mm Daisy

# **WSA** condenser



# WSA condenser - modular construction



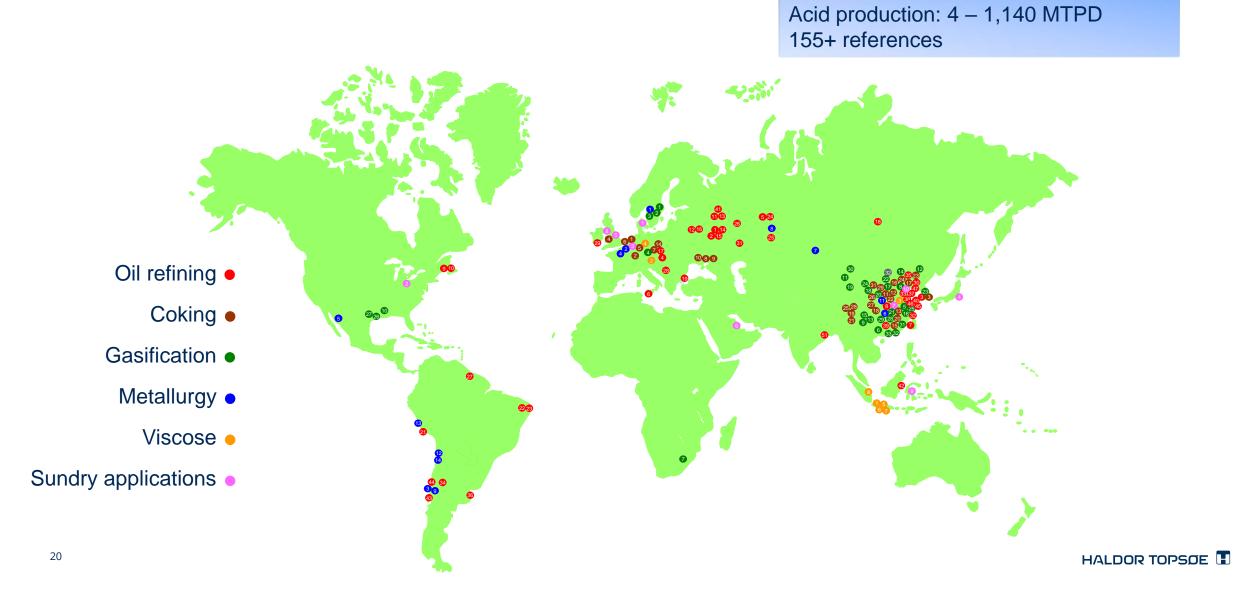


# WSA condenser design



#### **WSA/SNOX**<sup>TM</sup> references

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# **Refinery WSA plants**



Irving Oil Limited, NB, Canada

Claus plant tail gas treatment 40 t/d sulfuric acid



#### OSC Slavneft (YaNOS) Yaroslavl, Russia

Spent acid regeneration 260 t/d sulfuric acid

#### Too good to be true??

#### Conclusions



- Attractive OPEX and CAPEX
- Simple process and easy to operate
- Proven and reliable technology (155+ references)
- Low emissions and no waste materials
- No issues with NH<sub>3</sub> and hydrocarbons.

