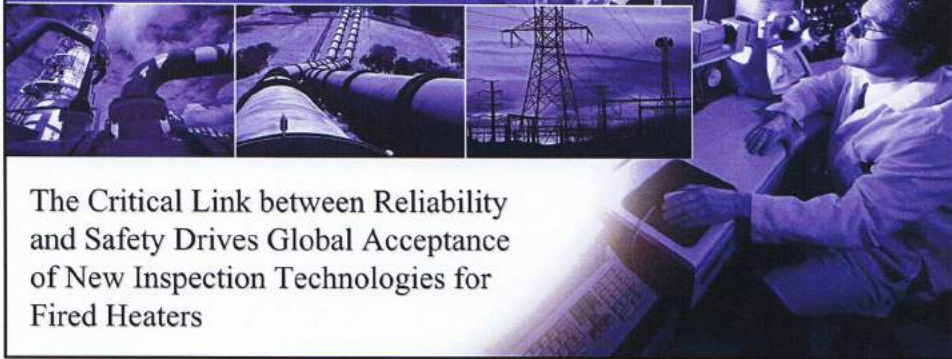


Refineries at Risk



The Critical Link between Reliability and Safety Drives Global Acceptance of New Inspection Technologies for Fired Heaters

State of Refining

- ▶ Refinery infrastructure is aging
- ▶ Refineries operating at as high as 99.4%
- ▶ Overuse increases the potential for failure
- ▶ Recent failures are understandable given the aging infrastructure and overuse

*Paraphrased from - Larry Chorn, PhD, Chief Economist, Platts Analytics
(Dec. 2006)*

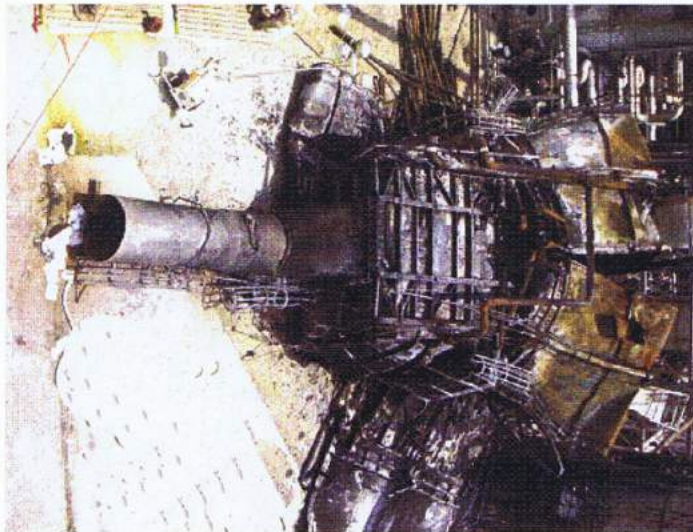
Catastrophic Heater Failures



QUESTTruTEC

QUEST
RELIABILITY

Catastrophic Heater Failures



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Catastrophic Heater Failures



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Rapid/Global Change

- ▶ Refiners around the world have been re-defining entire heater reliability programs around ongoing monitoring programs and “New Inspection Technologies” for fired heater – FTIS™ & LOTIS®. These programs coupled with engineering assessment (RLA and FFS) allow refiners to manage risk of operations. Nowhere in the refinery is this more important than in the Coker Unit.



Ongoing Heater Monitoring Program

1. Identify Key Reliability/Safety Parameters
2. Reliability Measurement Tools
3. Routine Monitoring Program
4. Detect Potential Failures

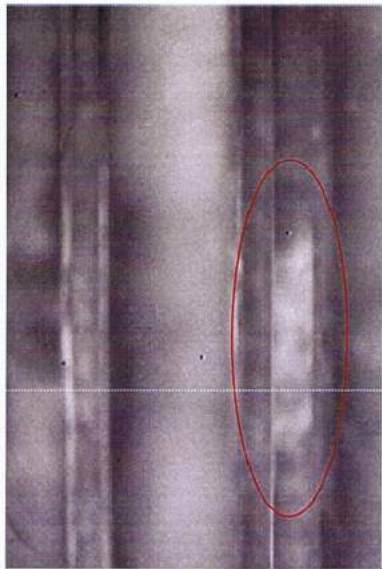


Key Reliability Parameters

1. Tube Metal Temperature
2. Process Fluid Temperature
3. Heat Flux Rate
4. Excess Oxygen
5. Fuel Gas Pressure
6. Process Feed Characteristics
7. Process Charge Rate
8. Flue Gas Temperature
9. Draft
10. Environmental Emissions
11. Process Fluid Pressure
12. Structural Component Temperature



Why is Temperature Important?



- ▶ Controls availability
- ▶ Determines reliability
- ▶ Allows an assessment of risk



Measuring Tube Metal Temperatures

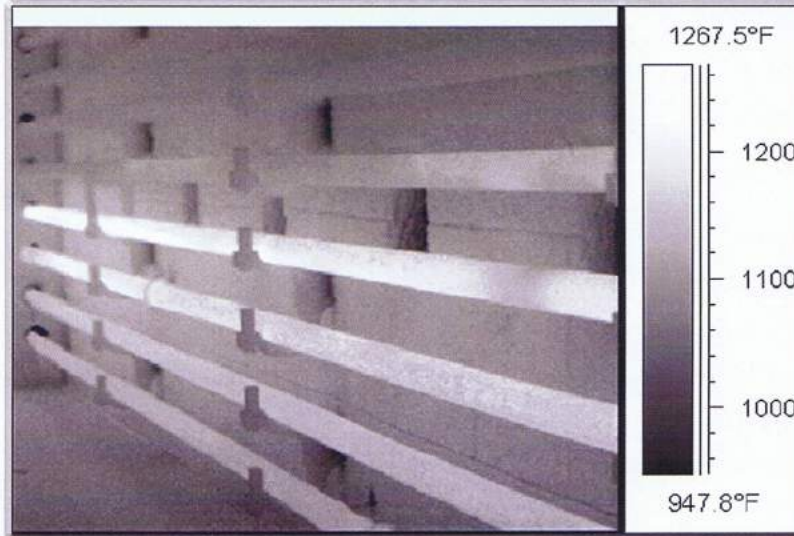


Flir Systems ThermaCam SC1000

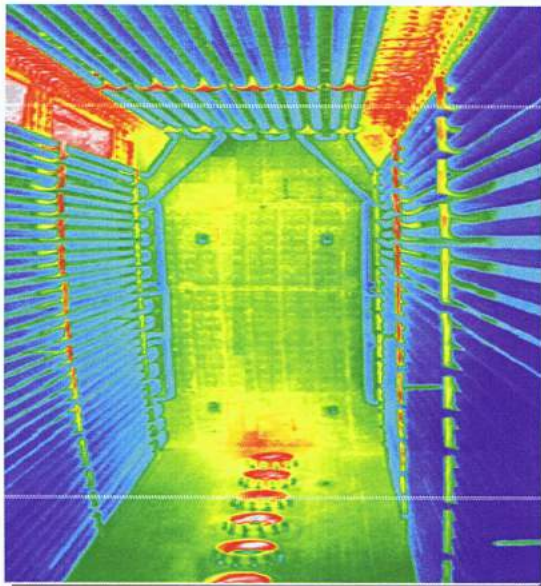
- Handheld portable radiometer camera
- Electrically cooled FPA imager
- Temperature range: 14 to 2732 deg F
- Color LCD Display
- Digital Video Output
- ThermaCam Reporter Software



Coker Charge Heater During Steam-Air Decoke



Observe Heat Distribution Pattern



Crude Charge Heater

- heat distribution
- tube temperatures
- burner signature



Flue Gas Analyzer

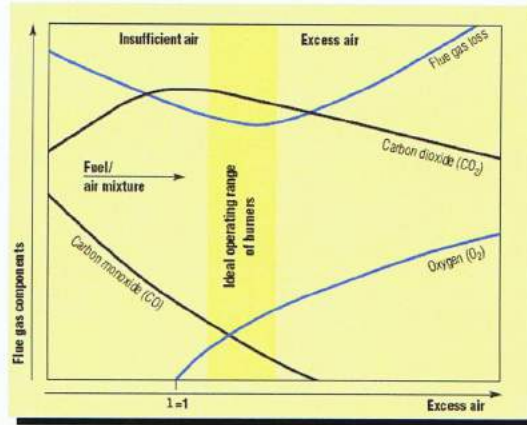


Testo 300 M Analyzer

- ▶ Handheld portable flue gas analyzer
- ▶ Measures O₂, CO, NO_x and SO_x emissions, draft and flue gas temperature



Flue Gas Analysis



- ▶ Burner performance (flame quality, emissions)
- ▶ Heater efficiency monitoring

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Routine IR/Heater Monitoring Program

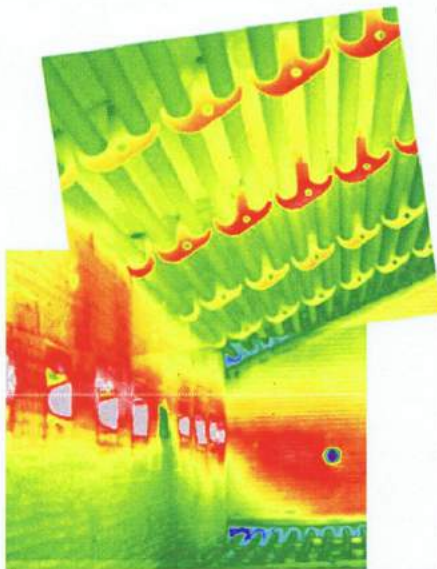
- ▶ Determine who will perform monitoring (Internal Resources/External Resources/Shared)
- ▶ Establish heater baseline performance
- ▶ Determine monitoring frequency per heater:
 - weekly, monthly, quarterly, as needed
- ▶ Data collection and analysis
- ▶ Determine action plan forward

QUESTTruTEC QUEST RELIABILITY

Step 4: Detect Potential Failures

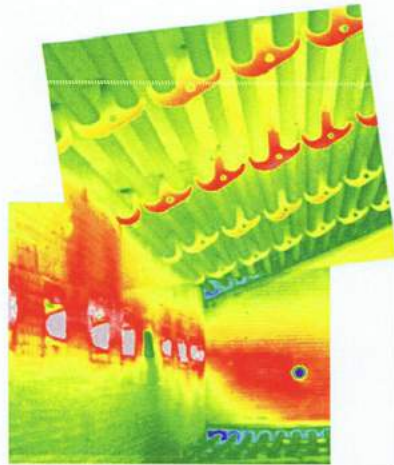


Can you identify the performance problems?



QUESTTruTEC QUEST RELIABILITY

Which heater would you choose?



Before



After

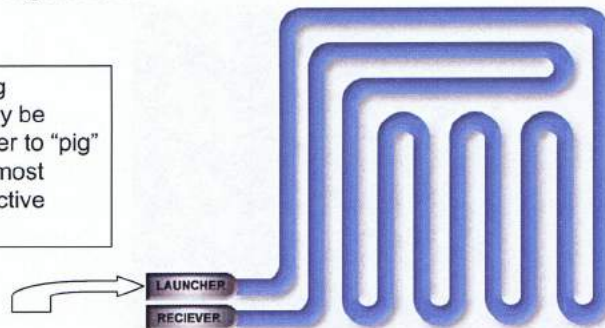
QUESTTruTEC QUEST RELIABILITY

Inspection Technologies Defined

► FTIS™ - (Furnace Tube Inspection System)

- Untethered intelligent pig utilizing Ultrasonics (UT) to rapidly inspect both the radiant & convection section as well as other piping configurations.

Inlet/Outlet piping modifications may be necessary in order to "pig" a furnace in the most efficient and effective manner.



QUESTTruTEC QUEST RELIABILITY

Inspection Technologies Defined

► FTIS™ - (Furnace Tube Inspection System)

- Untethered intelligent pig utilizing Ultrasonics (UT) to rapidly inspect both the radiant & convection section as well as other piping configurations.

► LOTIS® - (Laser Optic Tube Inspection System)

- Laser based system designed to internally inspect tubes of many services (Boilers, Steam Reformers, Heaters, etc.)



Refiners Applying FTIS™ & LOTIS® Today

ConocoPhillips



ExxonMobil



Marathon
Oil Corporation



VALERO ENERGY
CORPORATION



SK Corporation



Synocrude
Securing Canada's Energy Future

ChevronTexaco



SUNCOR
ENERGY

el paso

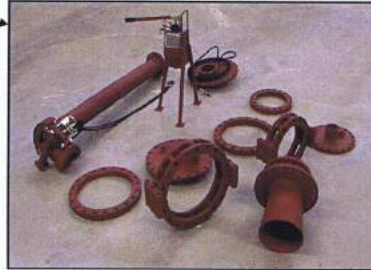


FLINT HILLS
RESOURCES



Applications

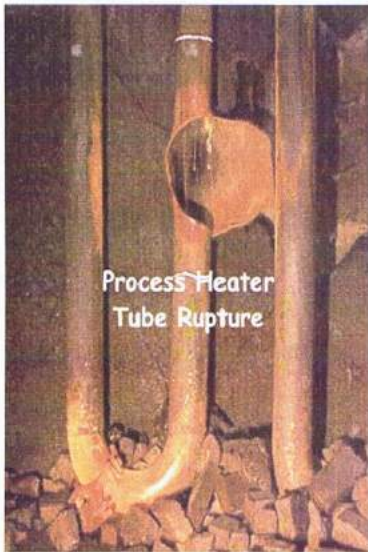
- **Furnaces Piping / Tubing**
 - Numerous Furnace Types (*Coker, Vacuum, Crude, UOP Platforming Heaters (CCR), Can, Cabin, etc.*)
 - Various Coil Configurations (*Vertical, Horizontal, U-Shape, etc.*)
 - Changing Diameter Coils (*4" ϕ 5" ϕ 6" ϕ 8"*)
 - Non-piggable furnaces in some cases (*i.e. Common Headers*) (*Common Header Delivery Systems**)
- **Pipelines**
 - Underground / Buried / Road Crossings
 - Insulated (*i.e. Asbestos*)
 - Overhead (*i.e. Congested Pipe Racks*)
 - In Plant / Between Plants / Wharf Lines



*Common Header Delivery System only available in Europe at this time



FTIS™ Detectable Failure Mechanisms

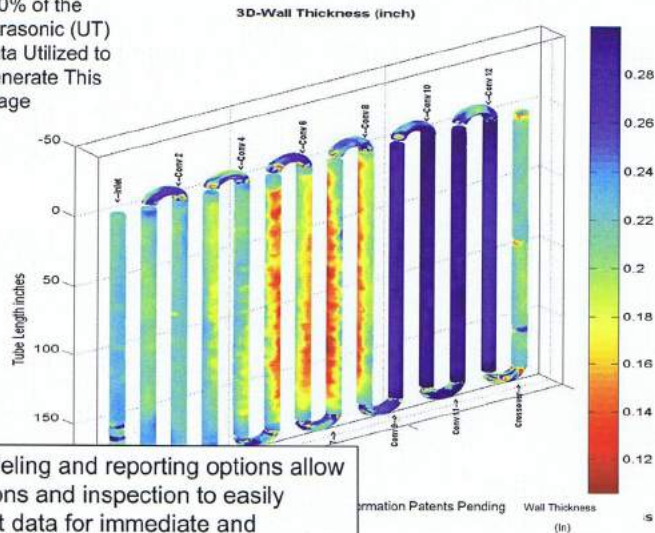


- **Pipe/Tube Wall Loss**
 - Corrosion (*Int. or Ext.*)
 - Erosion (*Int. or Ext.*)
 - Pitting (*Int. or Ext.*)
 - Mechanical Damage (*Int. or Ext.*)
- **Deformation**
 - Bulging (*i.e. Flame Impingement*)
 - Swelling (*i.e. Creep Strain*)
 - Denting
 - Ovality



3D Modeling of FULL Serpentine Coil

100% of the
Ultrasonic (UT)
Data Utilized to
Generate This
Image

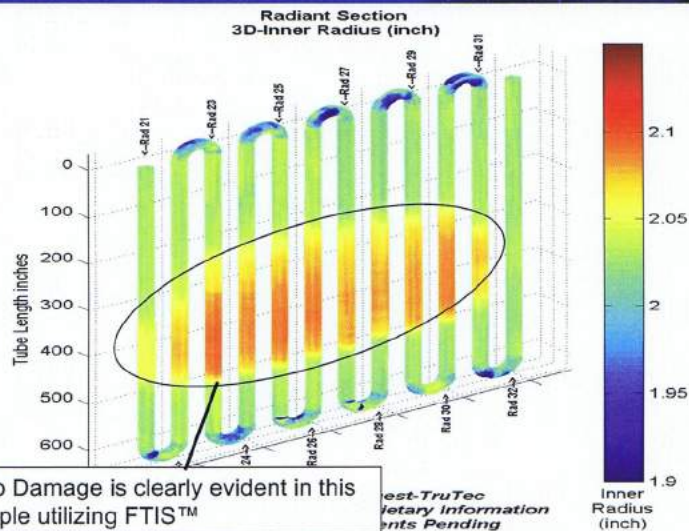


3D modeling and reporting options allow operations and inspection to easily interpret data for immediate and accurate corrective actions

Information Patents Pending
Data Pending

QUEST
RELIABILITY

3D Modeling of FULL Serpentine Coil

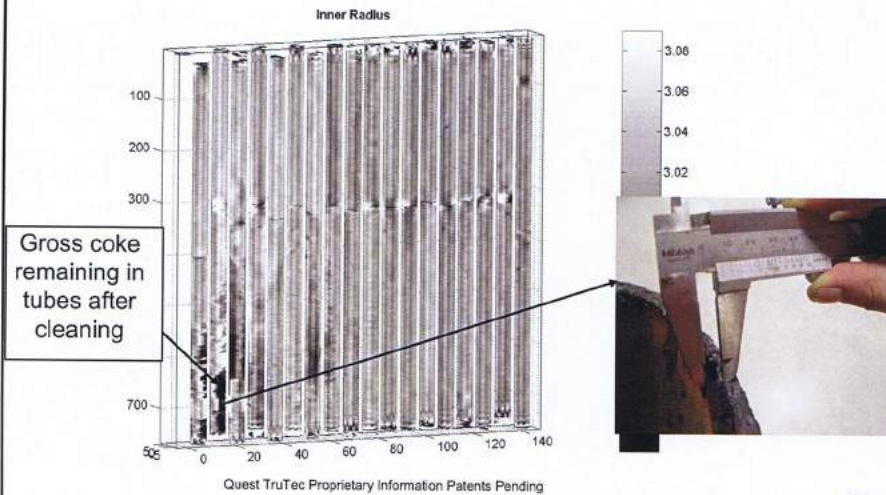


Creep Damage is clearly evident in this example utilizing FTIS™

Quest-TruTec
Industry Information
Patents Pending

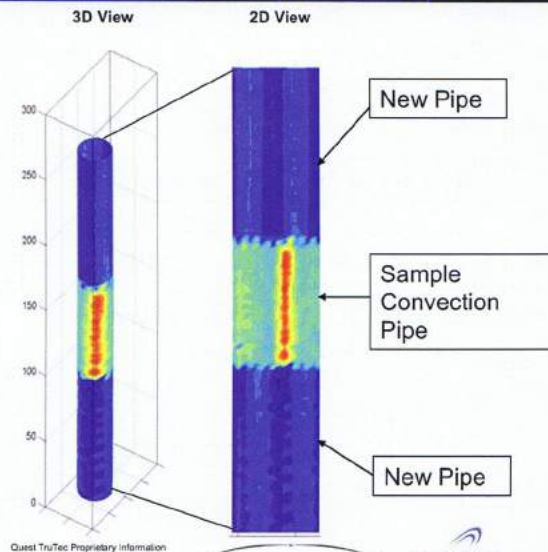
QUESTTRUtec QUEST
RELIABILITY

"Gray Scale" Decoking Assurance



QUEST TruTec QUEST RELIABILITY

External Studded or Finned Surfaces



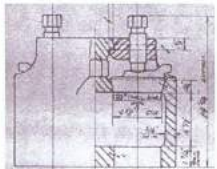
QUEST TruTec QUEST RELIABILITY

FTIS™ Current Limitations

- ▶ Current Design can handle minimum ID of 3.862" (6th Generation will reduce this minimum)
- ▶ Requires use of couplet (water) to push FTIS™ through piping coil and couple ultrasonic transducers.
- ▶ For Mule Ear (Plugged) Headers, the use of LOTIS® technology is recommended.



LOTIS® Detectable Failure Mechanisms



- ▶ Internal Pipe/Tube Wall Loss
 - Corrosion
 - Erosion
 - Pitting
 - Mechanical Damage
- ▶ Deformation
 - Bulging (i.e. Flame Impingement)
 - Swelling (i.e. Creep Strain)
 - Denting
 - Ovality



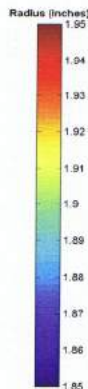
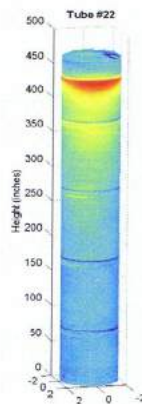
Internal LOTIS™ System, Model - 400M



0.460" to 5.64" (11mm to 143mm) ID
Accuracy of plus/minus 0.002" (0.05mm)

QUESTTruTEC QUEST RELIABILITY

Tube by Tube Analysis



Please enter the warning radius (in):

Please enter the probe tip radius (in):

Please enter the probe body radius (in):

Please enter the probe body diameter (in):

Please enter the probe body length (in):

Please enter a value for endstop:

Please enter a maximum radius for the radius:

Please enter a minimum radius for the radius:

Please enter a value for the radius:

☒ Sample Data ☐ ☐

☐ Indicators ☐ ☐

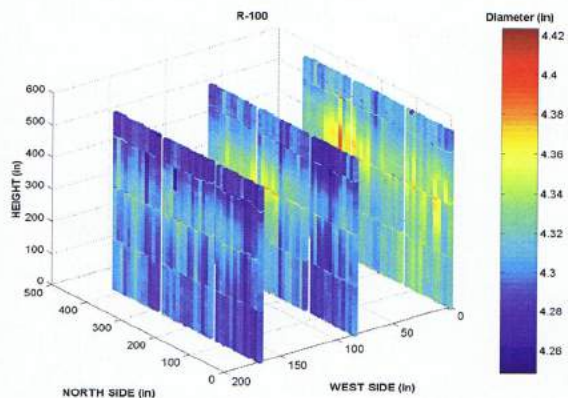
Save Data

Instrument Parameters for Tube Analysis
Tube # 22200

Change the value of the radius of the tube
Percentage Radius Growth = 434

QUESTTruTEC QUEST RELIABILITY

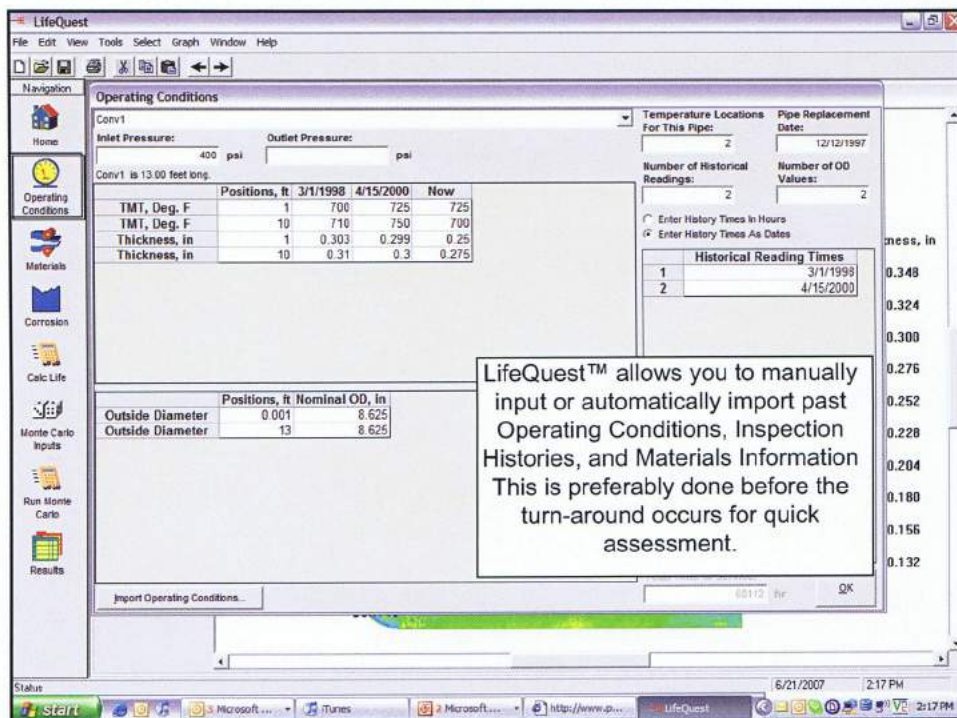
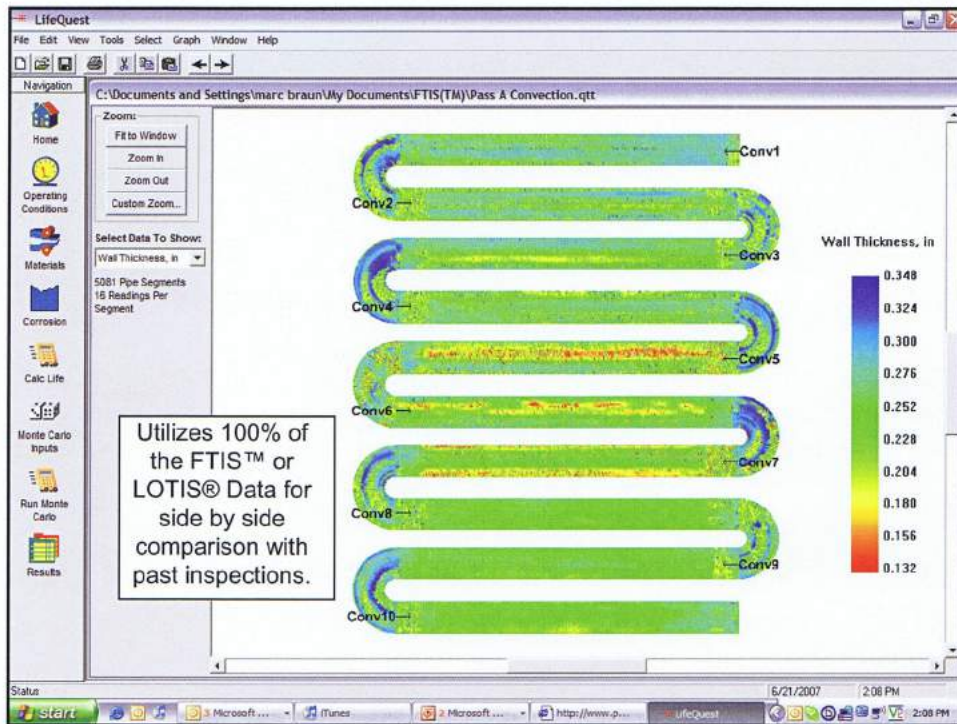
Creep Damage (Flame Impingement)

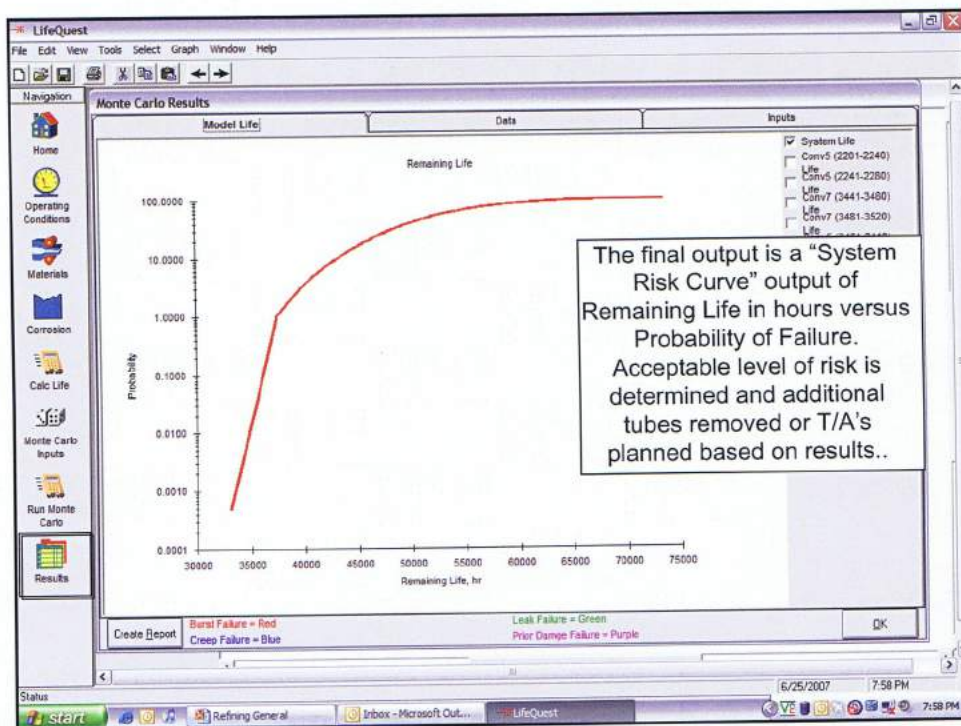
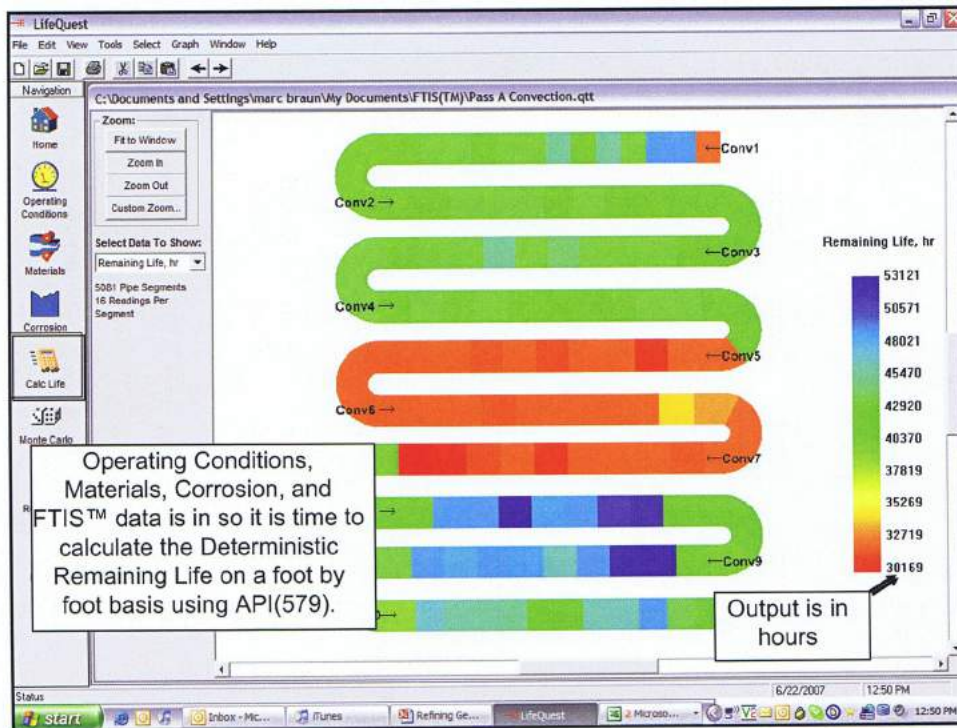


LifeQuest™ Heater Overview

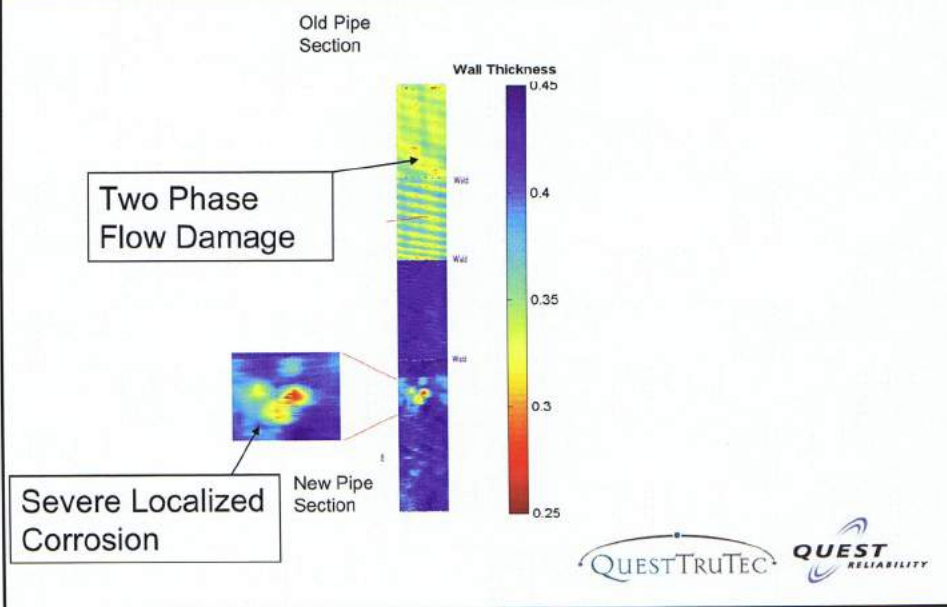
- ▶ Clients demanded the ability to use FTIS™ and LOTIS® data to make decisions concerning safe and reliable operations.
- ▶ What clients asked for:
 - Remaining Life Assessment within 24 hours
 - Utilization historical data
 - Compare data sets
 - Assess risk versus time to help with turn-around planning
 - In-house control over the process



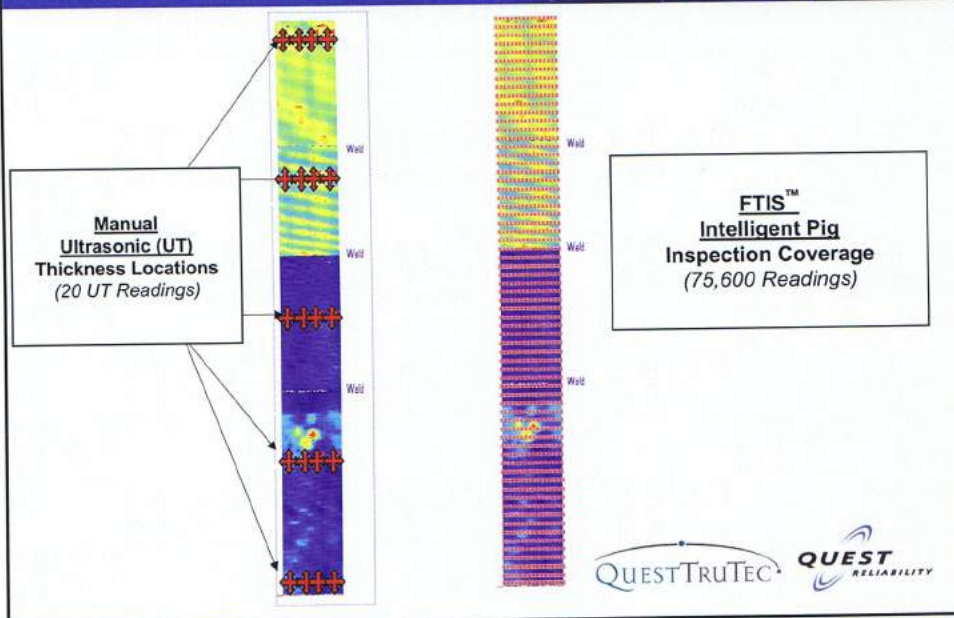




Case Study #1



Inspection Coverage Manual UT vs. FTIS™



Case Study #2

VACUUM HEATER

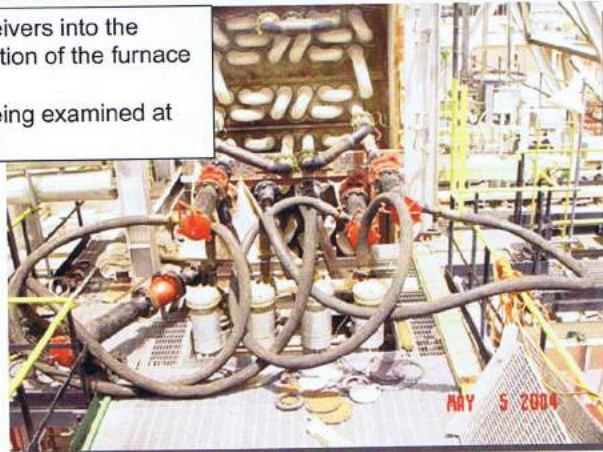
- ▶ Number of Coils / Passes = 8
- ▶ Pipe Material = 5Cr (5", 6" & 8" x Sch-80)
- ▶ Plant had modified heater convection section
- ▶ During mechanical pig cleaning process **water** was observed coming from Convection Section
- ▶ Plant elected to have FTIS™ Intelligent Pig inspection carried out rather than start cutting off return bends to find damage
- ▶ A FTIS™ Inspection was carried out on all 8 coils/passes (Inspection encompassed "both" Radiant and Convection sections)
- ▶ FTIS™ Intelligent Pig revealed only 8 pipe sections were damaged and localized to one end. All damage was "external"
- ▶ Plant stated that FTIS™ saved them over \$1M in coil replacement cost



Case Study #2: Pigging Set-Up

Launcher/Receivers into the convection section of the furnace

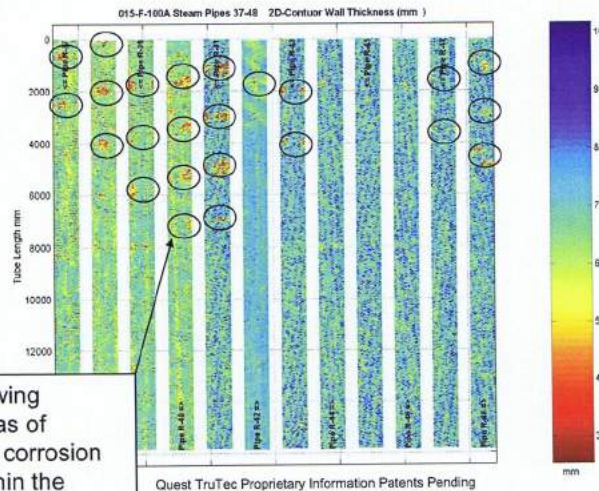
Two passes being examined at the same time



Typical Launcher / Receiver Set-up



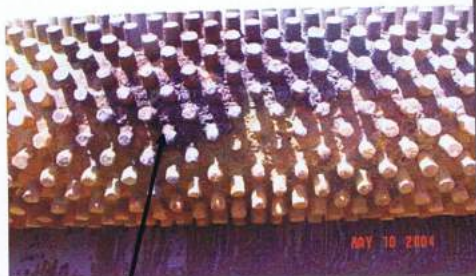
Case Study #2: FTIS™ External Damage



2D plot showing isolated areas of EXTERNAL corrosion damage within the studded region

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Case Study #2: "External" Corrosion



Soot blowers caused damage on OD of pipe
Note that the external studs are corroded away



Through wall hole in pipe where water was leaking from convection section

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Case Study #2: Removed Piping



Problem was isolated to 8 tubes and they were removed from heater for repairs

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Case Study #2: Tube Repairs (1/2 New - 1/2 Old Material)



New Pipe was welded to the Old Pipe to get heater back online

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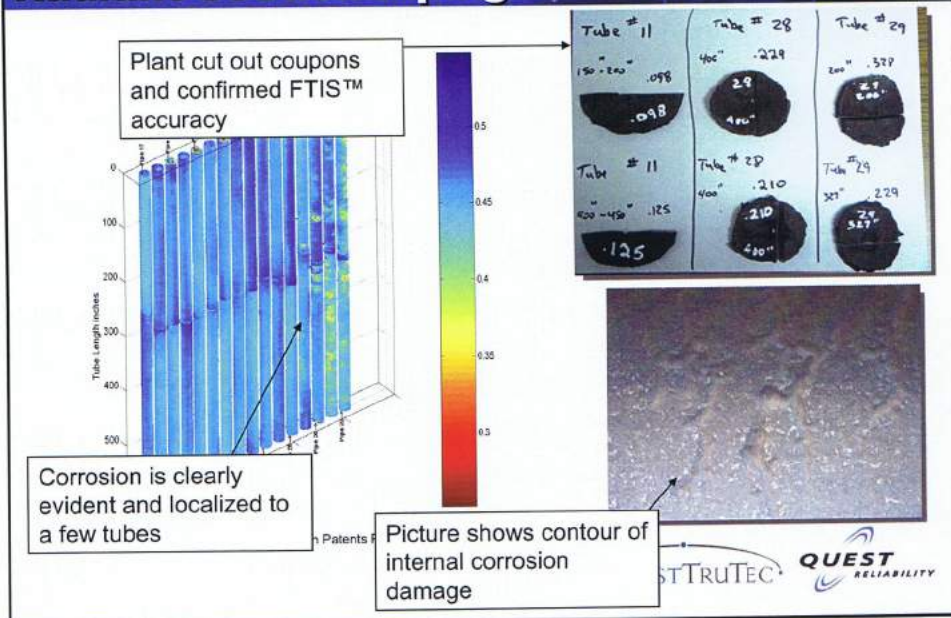
Case Study #3

ATMOSPHERIC HEATER

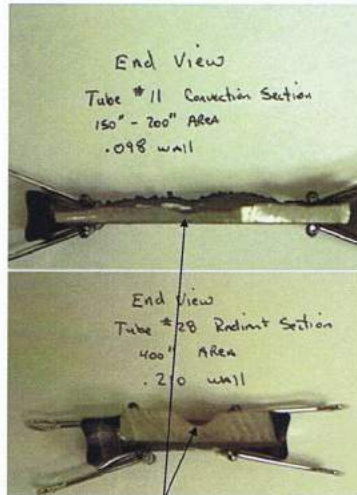
- ▶ Number of Coils / Passes = 4
- ▶ Pipe Material = 347Stainless (4", 5" & 6" x Sch-40/80)
- ▶ Plant expected some damage, however, not severe
- ▶ FTIS™ Inspection revealed substantial damage in both Radiant and Convection section of the coil
- ▶ Plant cut out sections to confirm data. When the results matched perfectly they then elected to expand scope of work and inspect a total of three (3) heaters
- ▶ FTIS™ Data clearly showed two types of damage patterns
- ▶ Plant cut out all damaged areas above threshold and confirmed accuracy of FTIS™. FTIS™ data matched destructive testing perfectly.
- ▶ Plant is now using FTIS™ data to better understand why damage is occurring



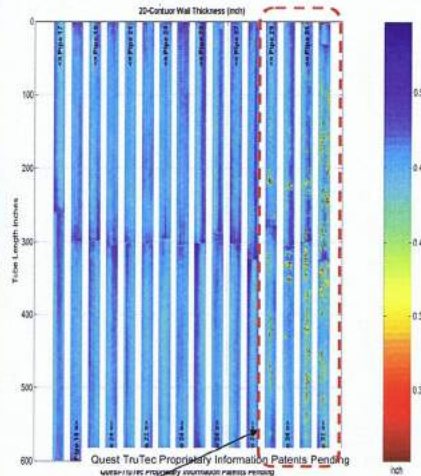
Case Study #3: (3D Plot) Corrosion in Radiant Section Piping



Case Study #3: (2D Plot) Corrosion in Radiant Section Piping



Photos show cross section views of coupons cut out by client



Notice that damage is isolated to all 4 tubes on the right.

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Case Study #3: Destructive Test Results

PIPING COIL INSPECTION RESULTS CONFIRMATION

1.) PIPE # 11 - 150"-200" AREA ----	FTIS™ REPORT ----	0.095- INCH
	MANUAL UT ----	0.095- INCH
	DRILLED HOLE w/CALIPER --	0.098- INCH
PIPE# 11- 400"- 450" AREA----	FTIS™ REPORT ----	0.095- INCH
	MANUAL UT ----	0.110- INCH
	DRILLED HOLE w/CALIPER --	0.098- INCH
2.) PIPE # 28- 400" AREA ----	FTIS™ REPORT ----	0.247- INCH
	DRILLED HOLE w/CALIPER --	0.248- INCH
3.) PIPE # 29 - 200" AREA ----	FTIS™ REPORT---	0.185- INCH
	DRILLED HOLE w/CALIPER -	0.188- INCH

- ▶ Thickness checks were initially performed by FTIS™
- ▶ Manual UT thickness were taken on exterior after removal
- ▶ Samples were cut out / hole drilled and measured with a micrometer - all readings were very close to the same.
- ▶ The areas showing localized thinning in the FTIS™ report have erosion areas throughout entire pipe length, with scattered deeper pitting.

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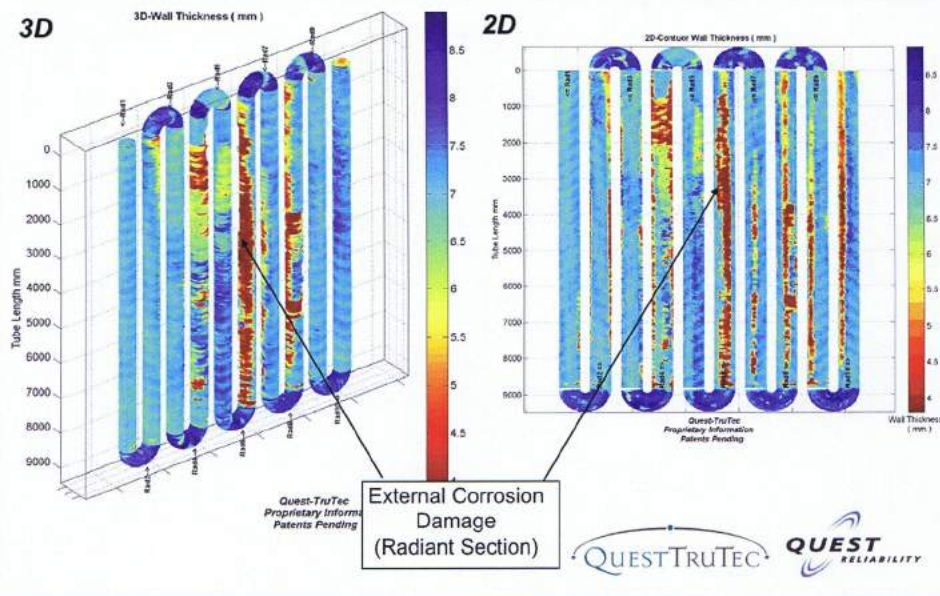
Case Study #4

VACUUM FURNACE

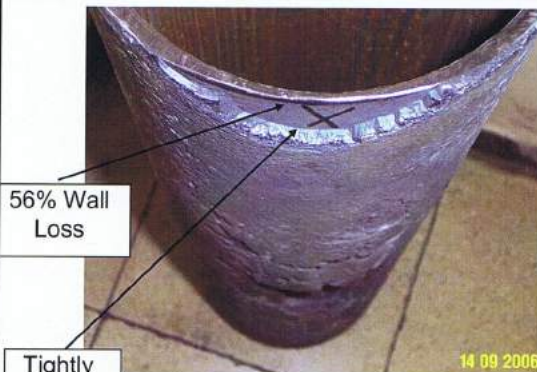
- ▶ Number of Coils / Passes = 2
- ▶ Pipe Material = ASTM A335 – P5 (6-inch x Sch.40)
- ▶ Heater Vintage = 1976
- ▶ FTIS™ was applied to inspect both process coils.
- ▶ FTIS™ inspection results detected extensive “external” corrosion damage in the radiant.
- ▶ Visual inspection found tightly adhered scale on piping exterior surface.
- ▶ FTIS™ results were not impacted by tightly adhered scale
- ▶ Large broad areas with 56% “external” wall loss was noted.
- ▶ Plant engineers utilized FTIS™ test results to make decision for replacement of several pipe sections



Case Study #4 Radiant Section Corrosion



Case Study #4



Tightly Adhered Scale



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Summary

- Aging infrastructures, PSM concerns, and capacity requirements are driving refiners globally to re-examine and redefine their entire inspection and reliability programs for Fired Heaters.

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Questions

