

New Technology Controls High Temperature Coker Heater Fouling

Coking.com Safety Seminar
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Bruce Wright



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Discussion Topics

1. Impact of fouling on DCU and refinery operations
2. Coker heater fouling mechanisms
3. Stages of fouling
4. Design of custom MILESTONE™ additive programs
5. Coking Stability Index (CSI)
6. Case histories
7. Summary



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Economic Impacts of Coker Heater Fouling

Throughput Losses
2-5% - \$5 MM

De-coking Costs
\$25K - \$50K/coil

Reduced Flexibility
Can be > \$5 MM



Conversion Losses
1% ~ \$3 MM

Increased Fuel Usage
2% > \$200,000

E, H & S Concerns

(All Values Based on Typical 40,000 B/D Unit)

Coker Heater Design & Operation

- Operating Parameters Affecting Coking Rates
 - Fluid velocity
 - Continuous throughput

Continuous Flow and Adequate Velocities are Critical to Good Operations!



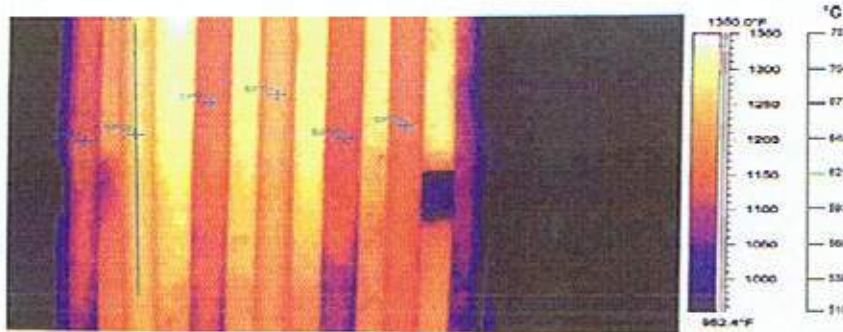
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Coker Heater Design & Operation

- Operating Parameters Affecting Coking Rate
 - Heater Outlet Temperatures
 - Uneven Heat Distribution - “Hot Spots”
 - Poor Flow Distribution



Feed Factors Impacting Fouling

- Asphaltene content and stability
 - Higher asphaltene content leads to more coke generation in the coils
 - Low stability feeds result in increased fouling
- Content of solids/inorganics
 - Corrosion by-products
 - Filterable solids and salts
 - Sodium concentration



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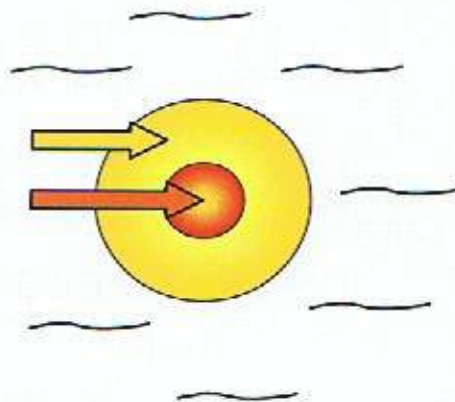
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Sources of Inorganic Materials

- **Iron sulfide, rust (corrosion by-products)**
 - Crude oil storage and transmission
 - Upstream process units
- **Salts: sodium, calcium, and magnesium chlorides**
 - From crude oil producing formation
 - Brine contamination from transportation
- **Caustic**
 - NaOH injections into desalted crude
- **Clay, dirt, catalyst fines**
 - From producing formation
 - From upstream process units

Asphaltene Micelle In Solution

Resins
Asphaltene Core



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Asphaltene Destabilization

- Readily destabilize when subjected to stress
 - Changes in pressure, temperature, pH and solution environment can cause destabilization
 - Can occur when oils are blended and processed
- Disruption of asphaltene – resin interaction
- Thermal cracking conditions (>400°C) cause progressive loss of asphaltene solubility in the bulk oil phase
- Asphaltenes lose paraffinic side-chains and naphthenic portions are de-hydrogenated to aromatic rings

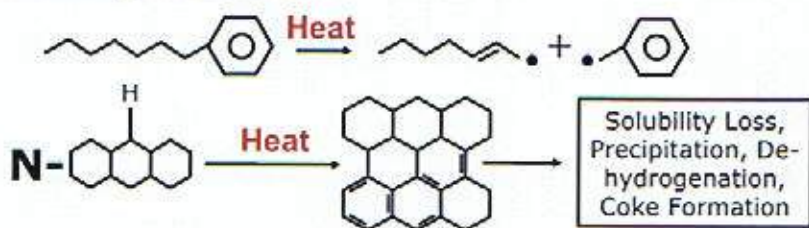


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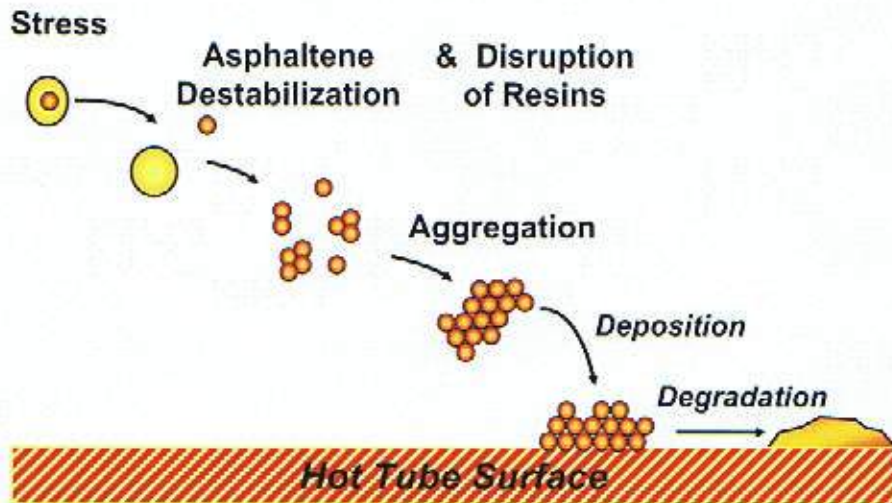
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Thermal Decomposition of Oil

- Concentration of paraffin compounds increases
- Resins are partly lost due to conversion to asphaltenes
- Naphthenes become aromatic
- Aromatics condense to form asphaltenes – lose solubility in bulk oil



Asphaltene Precipitation



Stages of Fouling

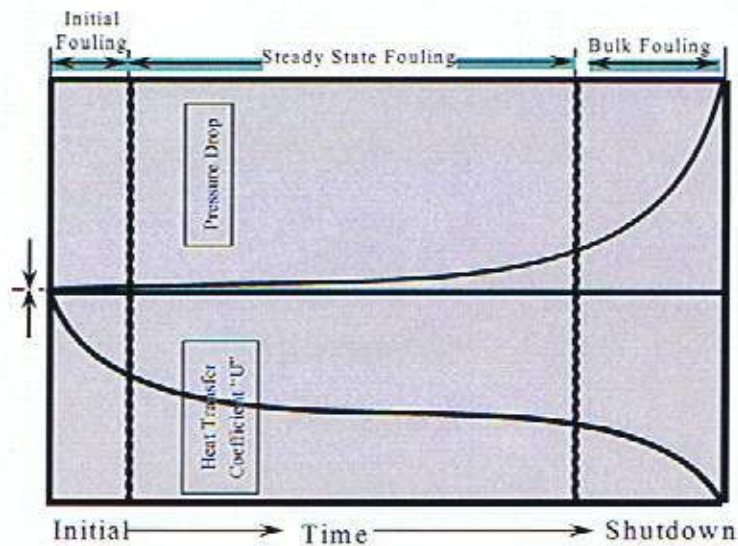
- **Initial layer formed on tube surface**
 - Metal catalyzed coking
 - Fast - at the startup of the unit when coils are clean and metal is exposed
- **Secondary layer of deposition**
 - Decreased asphaltene solubility in bulk oil
 - Thermal breakdown of asphaltenes
 - Precipitation of thermally converted asphaltenes or coke
 - Slower



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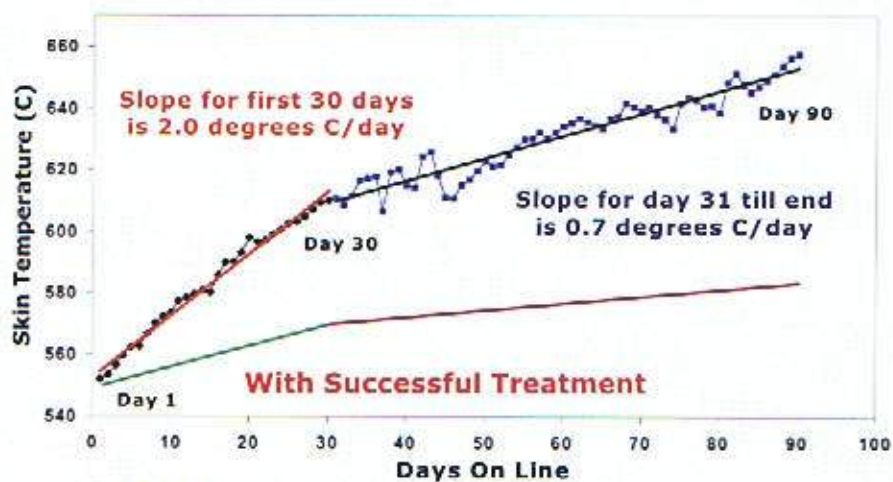
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Stages of Fouling



Target Treatment Results

Delayed Coker Heater Skin Temperatures



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Additive Program Design

- **Feedstock characterization test protocols**
- **Deposit characterizations**
- **Property ratios, correlations with fouling tendency**
- **Development of the Coking Stability Index**
- **Benchmark fluid characteristics with others in data base**

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CSI Coking Stability Index

- Predictive tool for determining fouling potential and rate of fouling
- Uses an NIR laser to detect the onset of asphaltene precipitation
- Titration technique with non-solvent
- Used in conjunction with oil characterizations to determine stability of coker feed
- Chemical additive screening

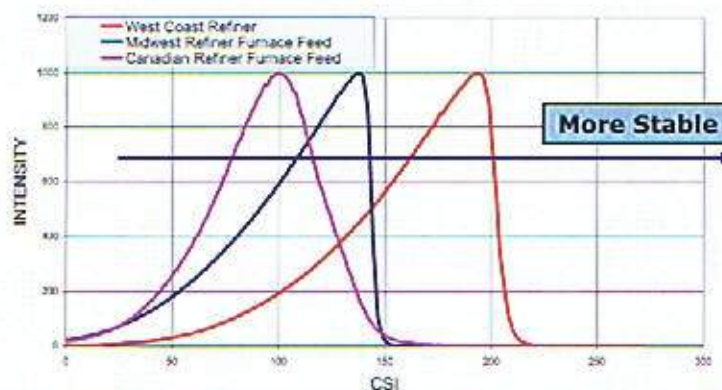


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| Coker Feed | Furnace Run Length | CSI | Asphaltene/Resin Ratio | Saturate/Aromatic Ratio |
|------------|--------------------|-------|------------------------|-------------------------|
| Canadian | 2.4 Months | 99.5 | 0.348 | 2.63 |
| Midwest | 5.0 months | 137.1 | 0.325 | 3.85 |
| West Coast | 9.0 Months | 192.0 | 0.458 | 2.94 |

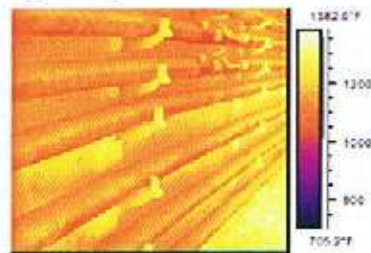
CSI Coker Stability Index
Furnace Feed Stability



Fouling Control Technology: MILESTONE Additives

MILESTONE Additive Technology:

- Interacts with metal surfaces to reduce catalytic effects on surface coking reactions
- Stabilizes compounds in the feedstock to inhibit their precipitation
- Disperses organic & inorganic particles



MILESTONE Technology: Pilot Scale Demonstrations

- JIP – Joint Industry Project, Using Department of Energy (DOE) Pilot Delayed Coking Unit (University of Tulsa)
 - Investment by major refiners to study coker operating variables, including coker heater fouling
 - Pilot unit studies confirmed suspected heater fouling mechanisms
 - Pilot unit tests also confirmed efficacy of Baker Petrolite fouling control technology



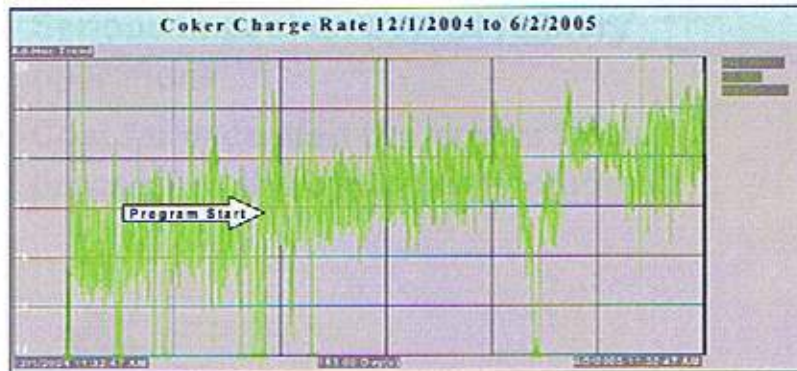
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Case Histories – Refinery A

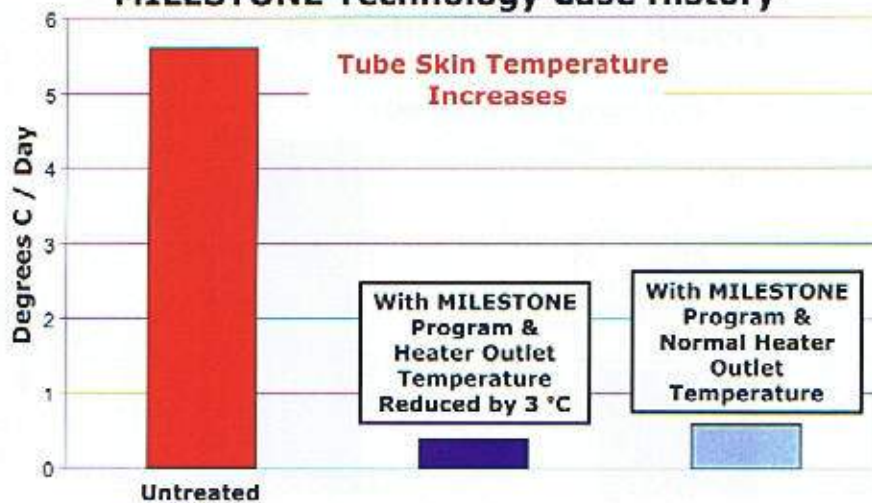
Improvements obtained with MILESTONE Program

- Throughput increase from 15,000 BPD to 19,000 BPD
- Tube skin temperature increase to 0.7°C/day, still less than target 0.8°C/day



Case Histories – Refinery A

MILESTONE Technology Case History



Summary

- Delayed coker furnace fouling is a complex phenomenon involving heavy hydrocarbon compounds and inorganic materials
- Two stages of fouling: initial catalytic stage and thermal or steady-state stage
- Costs of delayed coker furnace fouling can be significant especially when throughput is restricted either during operation or during de-coking cycles



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Summary

- The Baker Petrolite research group has developed a successful mitigation program for delayed coker furnace fouling
- A multi-component program is utilized to combat the various mechanisms of heater fouling
- Treatment programs have been used in several applications with outstanding results



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Thank You for Your Attention!

Any Questions?



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