



MYTHBUSTERS!

Steam Heating System Design

Episode

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Background



- Sulfur needs to be maintained within narrow temperature range to preserve flow
- Most common approach is steam heating
- Steam transfers heat to sulfur via jacketing
- Someone must design how...
 - Steam is transported to the heating system
 - Steam is routed through the system
 - Condensate is removed from the system

→ *Steam system design is often left to industry myths instead of engineering design*

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Stakes



- Process performance
- CAPEX savings
- OPEX savings
- Less maintenance/repair events

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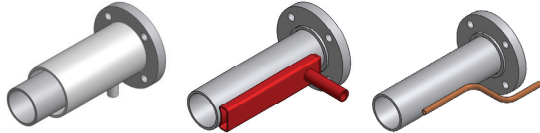
Agenda



- **Three common myths**

- Myth
- Basis for myth
- Real-life example that illustrates myth
- Evaluation
- Lessons learned

Steam jacketed systems for liquid sulfur lines



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Myth

1

If the sulfur lines are flowing, my heating system must be working.



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Basis for myth

1

- If it's flowing, it's not plugged
- Thermodynamics: hot piping will lose heat to cooler surroundings
- As process loses heat, its temperature can drop below sulfur freezing point, causing plugging
- Flowing process loses more heat than no-flow



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Real-life example #1

1

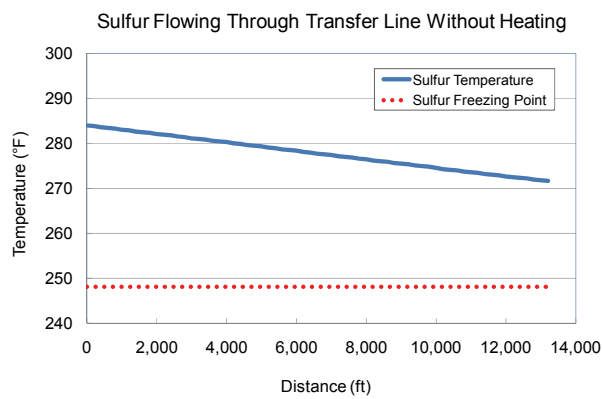
- 2.5 mile sulfur transfer line in Kazakhstan
- Design/install enough tracing to keep sulfur molten at end of line
- Minimize heat input to sulfur prior to forming unit
- Design details:
 - 8-in NPS
 - 2.5-in mineral wool
 - Ambient conditions: -40°F/ 25mph wind
 - 3 fps flow rate
 - Sulfur enters line at 284°F

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Evaluation: flowing

1

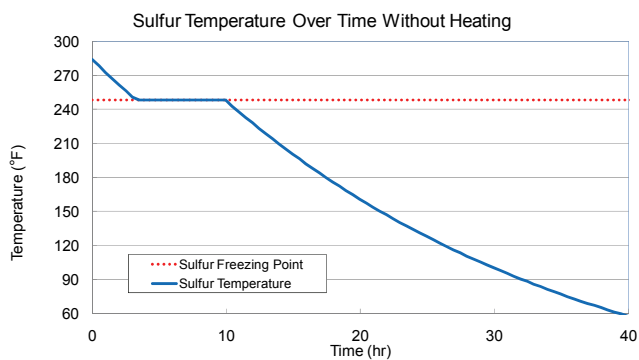


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Evaluation: no-flow

1



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Real-life example #2

1

- Consider this heating piping system...



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Myth

1

If the sulfur lines are flowing, my heating system must be working.

MYTH BUSTED!

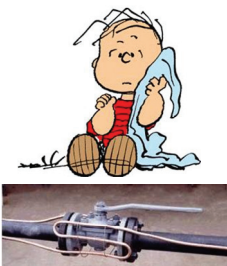
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Lessons learned

1

1. Flowing, insulated sulfur lines do not need heat
2. Real design requirement is no-flow and melt-out



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Myth

2

Condensate must be trapped after every JP spool.



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Basis for myth

2

- Water seeks its own level
- Gravity causes water to run downhill
- Concern that condensate which drains out of spool and into jumper will prevent free flow of steam into next JP spool

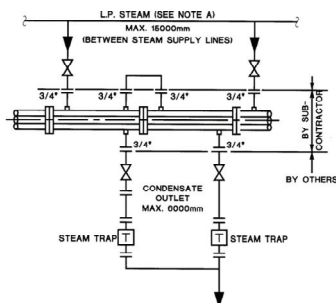
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Real-life example

2

APPENDIX 3
DETAILS OF STEAM AND CONDENSATE HOOK-UP ON JACKETED PIPING



- Taken from JP specification for 640-spool project
- Requires 1 trap per spool

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Evaluation: steam video

2



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Myth

2

Condensate must be trapped after every JP spool.

MYTH BUSTED!

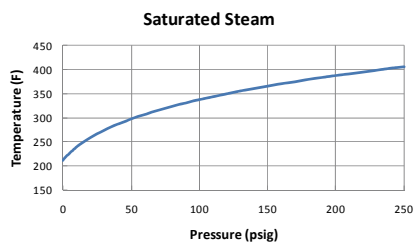
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Lessons learned

2

1. Condensate does not stop steam flow
2. Real limitation on trap frequency (circuit length) is steam pressure



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Lessons learned

2

3. Removing the “trap every spool” requirement can save lots of traps and \$ w/o impacting performance

	Trap Qty	CAPEX \$	OPEX \$/Yr
1 trap / spool	640	\$624,000	\$85,333
CSI design	148	\$144,300	\$19,733
Δ	492	\$479,700	\$65,600

Assumptions: \$975 CAPEX/trap; 3 year trap life; \$400 replacement cost including labor.



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Myth

3

A jacketed heating system will work with any type of standard steam trap.



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Basis for myth

3

- All traps share same basic objective:
 - Trap steam
 - Remove condensate
- Many types of traps
- Differences can be complicated
- Many have not taken the time to understand the differences or implications



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Real-life example



- New Alberta SRU
- Extensive freeze-ups during first winter
- Found 34 disc traps failed closed due to debris
- Found 19 disc traps failed open due to high back pressure
- Changed 550 traps to inverted bucket traps
- No issue during next winter

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Trap styles



Inverted Bucket



Thermodynamic (disc)



Float



Thermostatic



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Trap requirements



	Remove condensate
	Continuously purge entrained air
	Accommodate condensate return back pressure

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Trap recommendations



Type	Performance	Recommendation
IB		Recommended – No special considerations
Float		Acceptable <u>if</u> consider air purging
Disc		May be acceptable <u>if</u> consider condensate return pressure correctly
TS		Not acceptable – Condensate can back up in jacketing/tubing

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Myth



A jacketed heating system will work with any type of standard steam trap.

MYTH BUSTED!

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Summary



1. Design liquid sulfur lines for no-flow/melt-out
2. Design steam circuits using engineering rather than rules-of-thumb to save traps, \$, and issues
3. Choose inverted bucket or float/thermostatic steam trap for maximum robustness

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Thank you!



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