

# **Coker Heater Design The Heart of the Coking Process**

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Fired Heater Division**



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# NEW UNITS OPTIONS





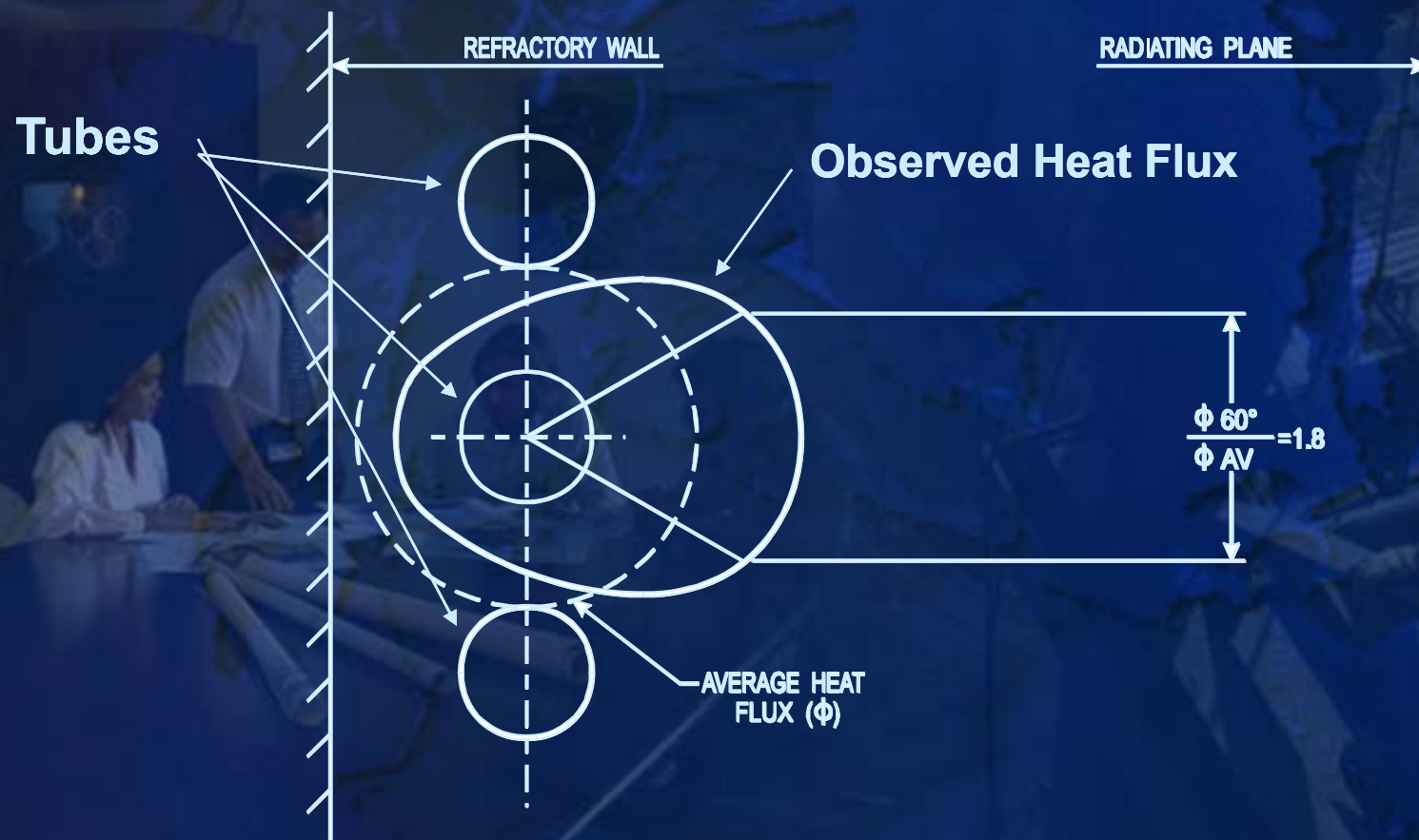
# ELLIOTT'S RULES FOR COKER HEATERS

- Individual Pass Control and Firing Ability
- High In-Tube Velocities (6 fps min.)
- Minimum Residence Times
- Optimum Flux and No Mal-distribution
- Constantly Rising Temperature Profile
- Symmetrical Pass Arrangements and Piping
- Steam/Condensate Injection
- Generous Firebox Dimensions

# SINGLE VERSED DOUBLE FIRED

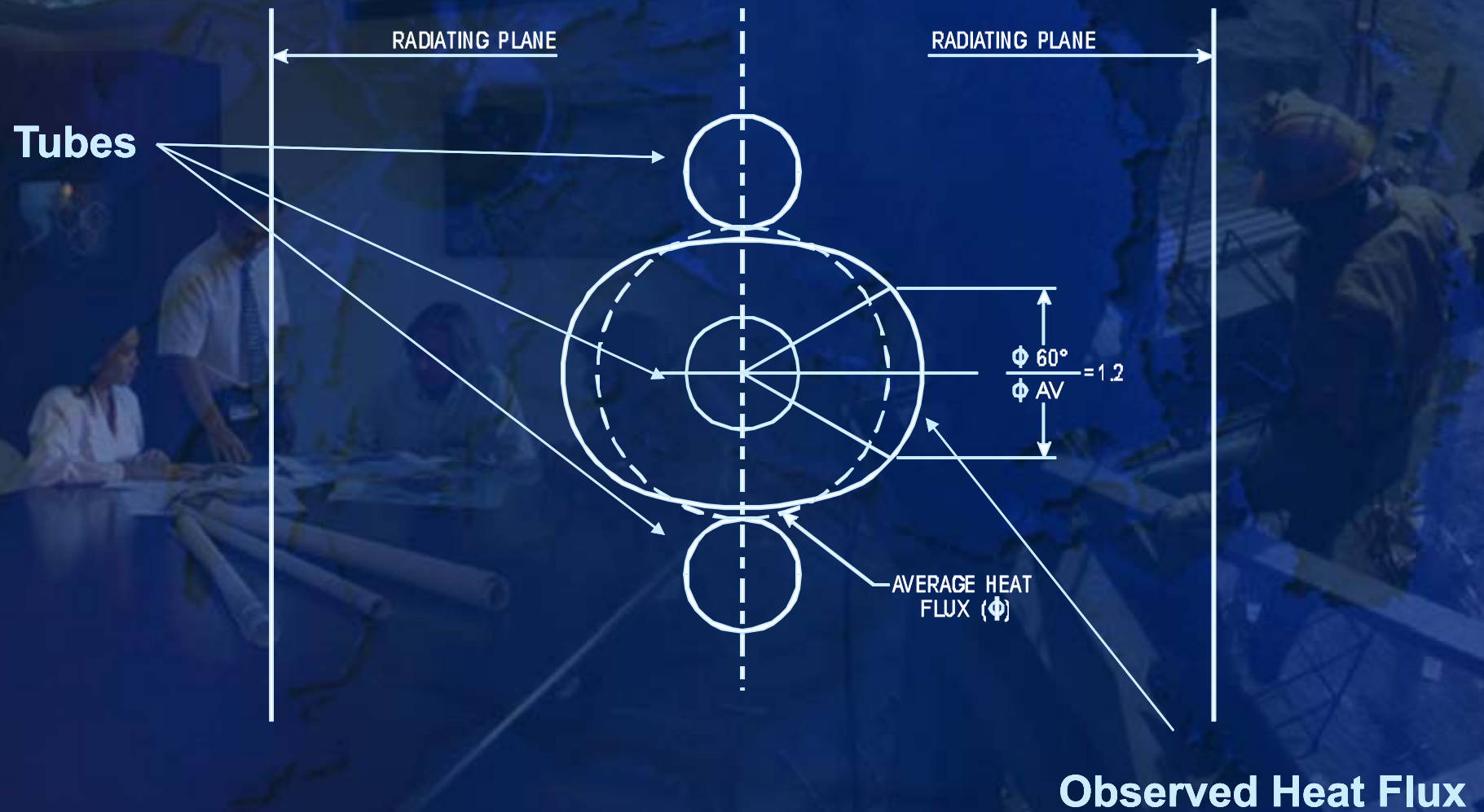
- Same Peak Heat Flux
- Same TMT Limit
- Double Fired – 2/3 the Radiant Surface
- Double Fired- More Volume in Radiant Section
- Double Fired- Higher Velocity For Same  $\Delta P$
- Double Fired- More Uniform Heat Flux
- Double Fired-Handles Difficult Feeds Better

# CIRCUMFERENTIAL HEAT FLUX DISTRIBUTION - SINGLE FIRED TUBES



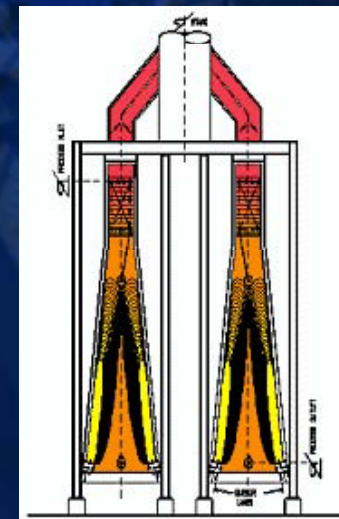
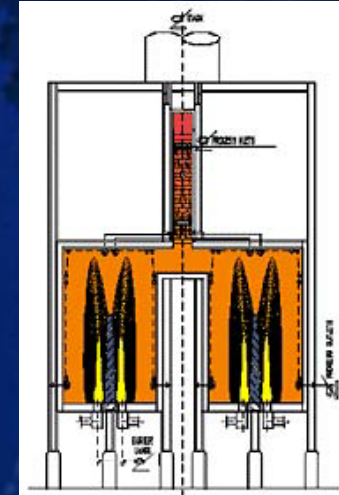


## CIRCUMFERENTIAL HEAT FLUX DISTRIBUTION - DOUBLE FIRED TUBES



# Heater Design Complete

**WHAT MORE IS THERE TO  
CONSIDER?**



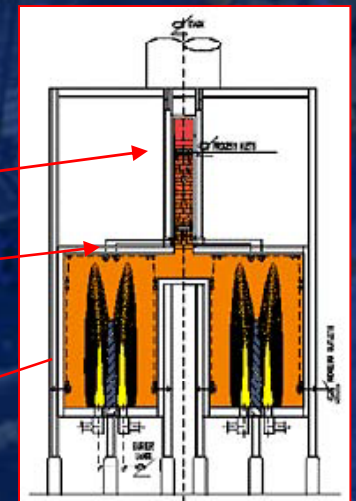
## **DETAIL CONSIDERATIONS**

- **Velocity Medium Injection/Locations**
- **Single vs. Multiple Design Temperatures**
- **Single vs. Multiple Design Pressures**
- **Tube Metallurgy/Diameter/Thickness**
- **Plug Headers/Wrought/Cast Fittings**
- **Radiant Header Boxes**
- **Pigging/Spalling/Steam Air Decoking**
- **Burner Selection/Layout**
- **Radiant Tube Supports**
- **Modularization**



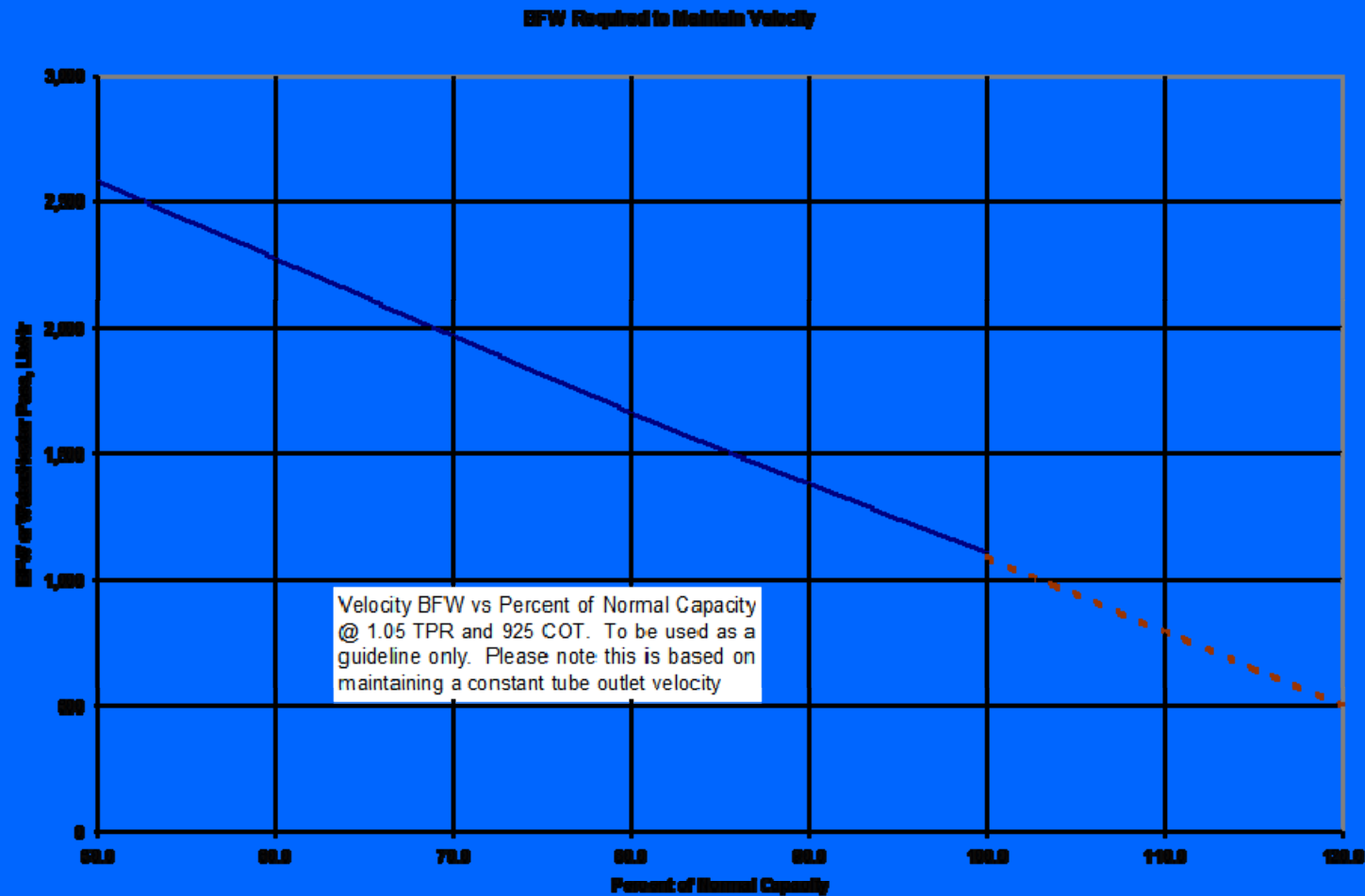
# STEAM/CONDENSATE INJECTION/LOCATIONS

- Amount
  - 1% wt Steam or Condensate
- Location
  - Prior to Convection Section
  - Crossover Piping
  - Just Prior to where Cracking Starts
- When to Relocate the Injection Point?
  - Pressure Drop issues Only
- Turndown



# TURNDOWN- VELOCITY INJECTION MEDIUM

FOSTER  WHEELER  
Fired Heaters



Each heater should have a velocity injection medium curve developed for the feedstock to be processed in the tube size installed

# VARYING DESIGN TEMPERATURES

## ➤ **PROS - Lower Convection Design Temperature**

- Thinner tubes
- Possible different metallurgies
- Possible different fin metallurgies
- Less costly

## ➤ **CONS -Lower Convection Design Temperature**

- Limits operating conditions at EOR
- Limits Spalling Flexibility (increase time)
- Fin losses and Thermal Efficiency losses
- Shorter run lengths
- Operational revenue lost



# VARYING DESIGN PRESSURES

- **PROS- Lower Radiant Design Pressure**
  - Thinner tubes
  - Less costly
- **CONS - Lower Radiant Design Pressure**
  - Limiting operating conditions at EOR
  - Can not handle Blocked-in Conditions
  - Shorter run lengths on opportunity crudes
  - Operational revenue lost

# TUBE DESIGN CONDITIONS

- **Metallurgy 9Cr-1Mo vs. 347SS**
  - **API Limits 1300°F for 9Cr-1Mo vs. 1500°F for SS**
  - **SS Tubes have better spalling ability on organic fouling due to thermal expansion properties**
  - **SS Tubes are more prone to erosion in return bends**
  - **9Cr has proven to be successful in operation on various feed stocks including high S, high minerals, and high TAN**
  - **SS Tubes must watch for chlorides in injection medium and sulfur in fuels and feeds for corrosion attack**

# TUBE DESIGN CONDITIONS

- **Diameter-Single Diameter in Radiant**
  - Elliott's Rule on High Velocity – Diameter Increase Reduces the Inside Heat Transfer Coefficient and Raises Film Temperature
  - More  $\Delta P$  is Seen with a Single Tube Diameter
- **Thickness-Single Thickness Throughout**
  - Allows Higher EOR conditions, Off-Design Operations like Spalling and Recovery from Emergencies like Blocked In Conditions
- **Ultimately Longer Run Lengths and Tube Life are possible**



# PLUG HEADERS

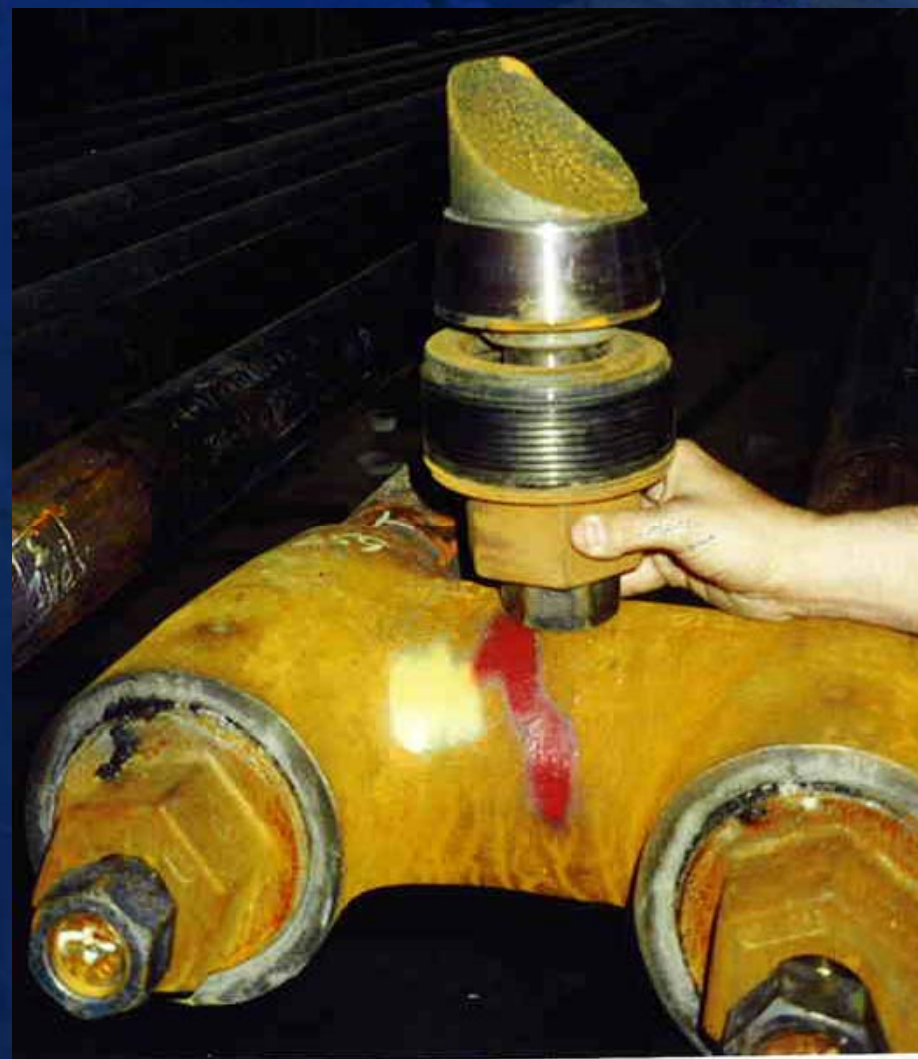
## ➤ Plug Headers Cons

- Leak
- Maintenance Problems
- Require Header Boxes

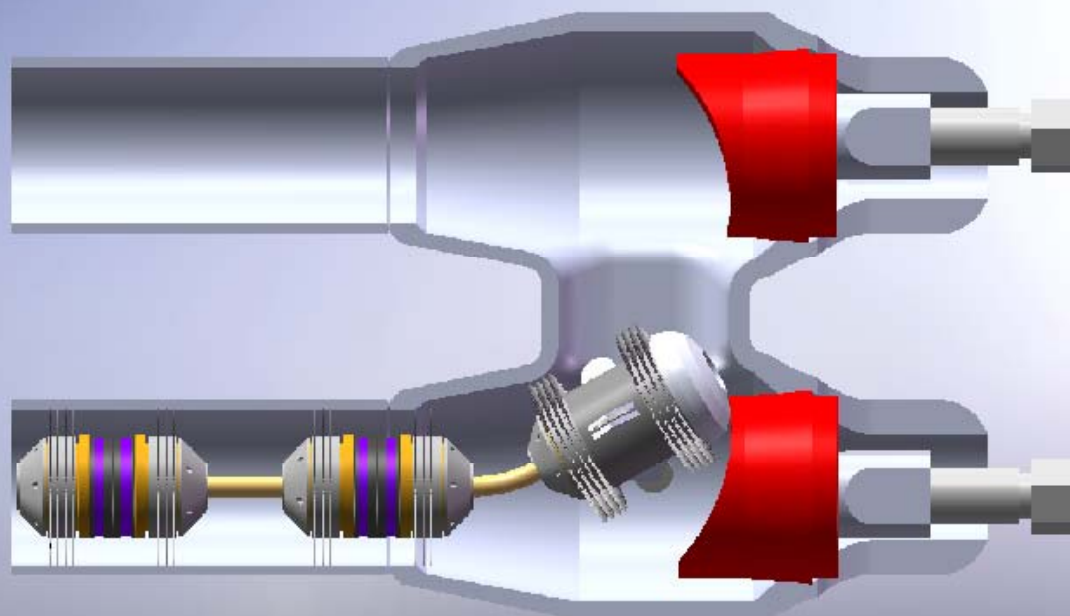
## ➤ Plug Header Pros

- Can Pay for Themselves with One Use
- Are Useful for New Coker Unit Owners
- New Contoured Plug Designs for Pigging
- Can Now be Smart Pigged

# CONTOURED PLUG HEADER



# SMART PIGS



Plug headers as pictured will allow for Quest Integrity Group's FTIS intelligent pig inspection process

**Courtesy of Quest Integrity Group**



# RETURN BEND DESIGN-RADIANT

## ➤ WROUGHT FITTINGS

- Typically Supplied in a Thicker Schedule than the Tube
- The Reduced ID Causes Additional Acceleration and Additional Erosion on the Return Bends

## ➤ CAST FITTINGS

- Supplied with the Extra Thickness on the OD for Enhanced Erosion Resistance
- Maintains the Same ID as the Tube to Limit Acceleration Related Erosion Effects

## ➤ INTERNAL SURFACING

- Primarily Used on the External 'Swing Elbow' for Erosion Prevention
- Patented for Use Inside the Heater- Believe it is of Limited Use

# CAST RETURN BENDS





# RADIANT HEADER BOXES

## ➤ PROS

- Allow Lower Design Temperatures on Fittings
- Easier to Remove and Replace than Large End Panels
- No Confined Space Entry to Exam or Repair Return Bends
- End Panel Option Allows Easy Access to Exam Return Bends on a 'Pit Stop' Turnaround
- Required for Plug Header Designs

## ➤ CONS

- Requires More Tube Length (not effective area)
- Requires More Plot Length
- Additional Cost



# RADIANT HEADER BOXES



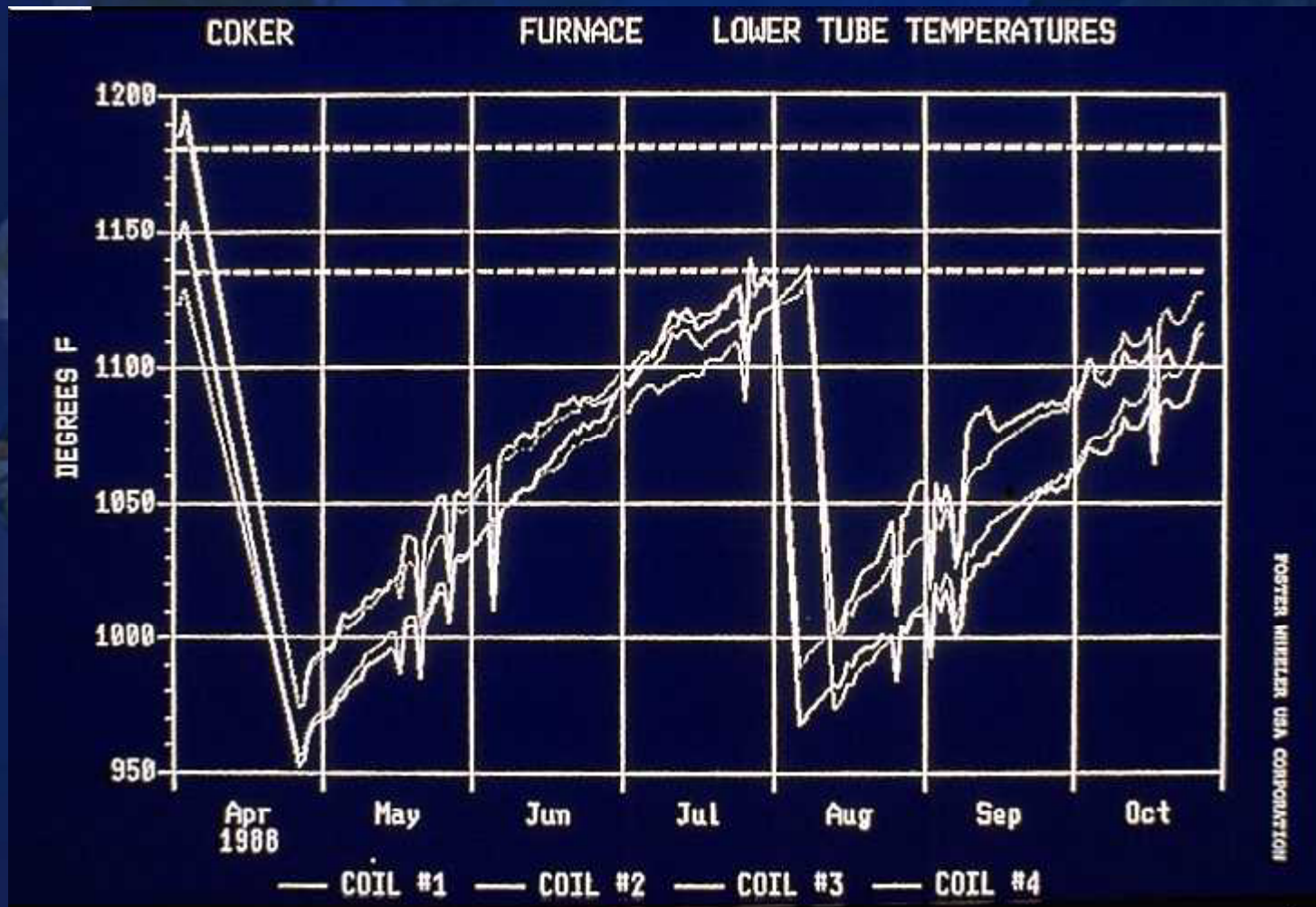
# PIGGING/SPALLING/DECOKING

**In General, the Refiner Should Determine Early in the Project with DCU Licensor the Desired Decoking Method(s) so Provisions Can be Made in the Heater Design and Heater Piping Layout**

- **On-Line Spalling and Pigging**
- **Off-line Spalling and Pigging**
- **Organic Fouling – Spalling and Pigging Compatible**
- **Inorganic Fouling- Pigging Only**



# SPALLING CHART



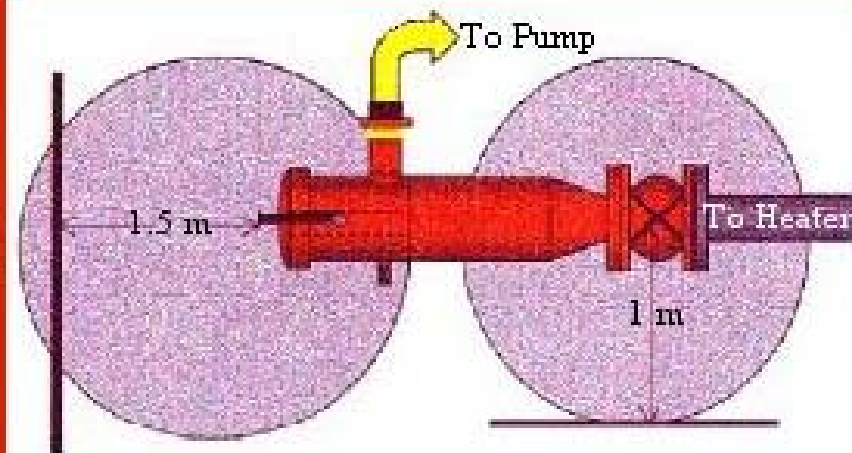
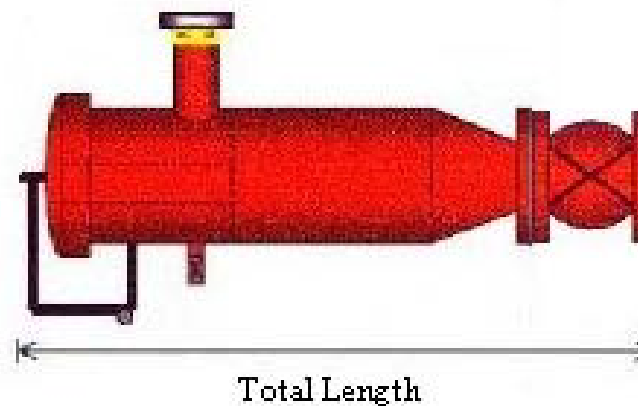


# Pigging System (DDT Pigging)

**FOSTER WHEELER**  
Fired Heaters



Launcher & Ballvalve Assembly

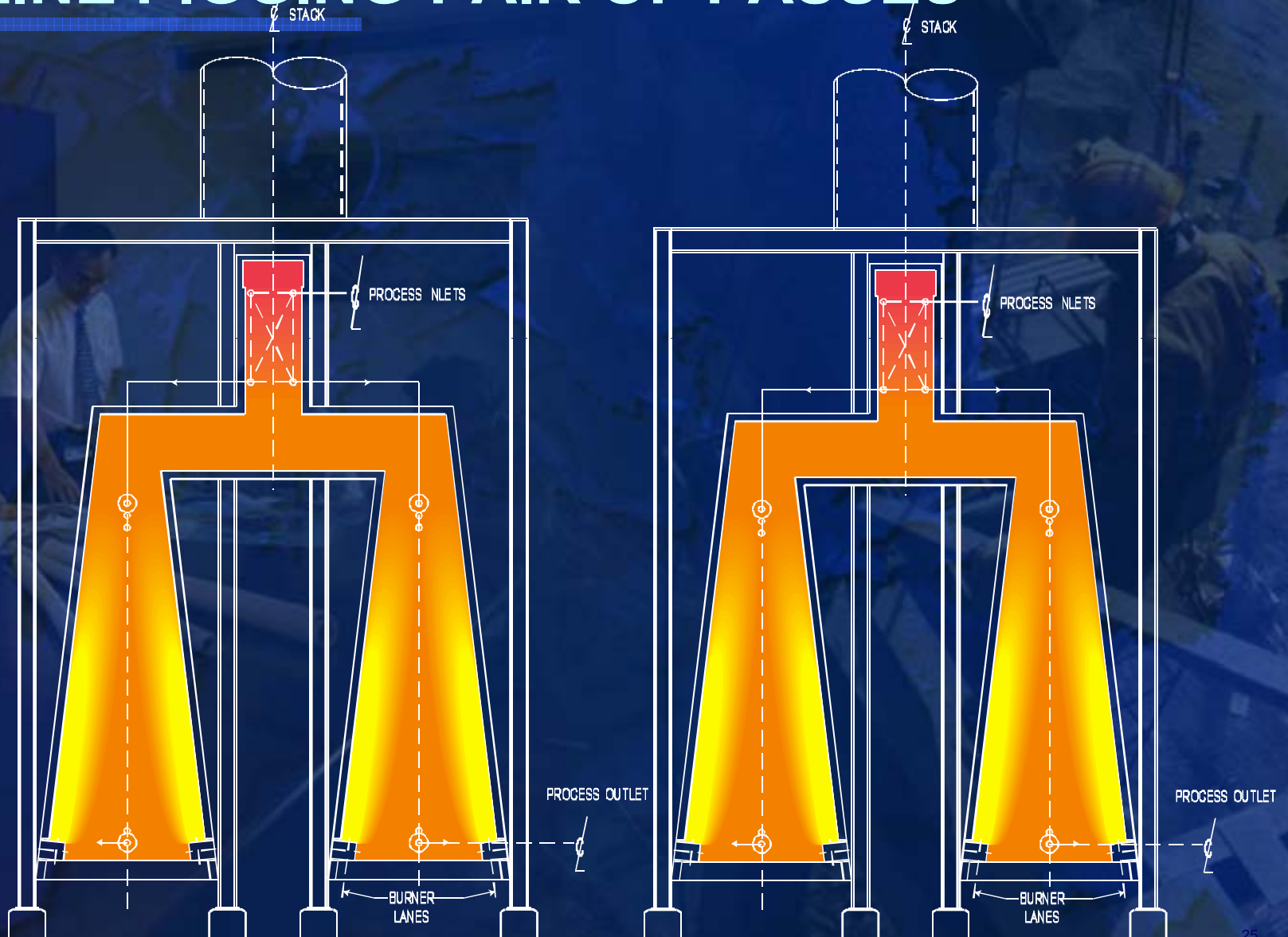


## Length

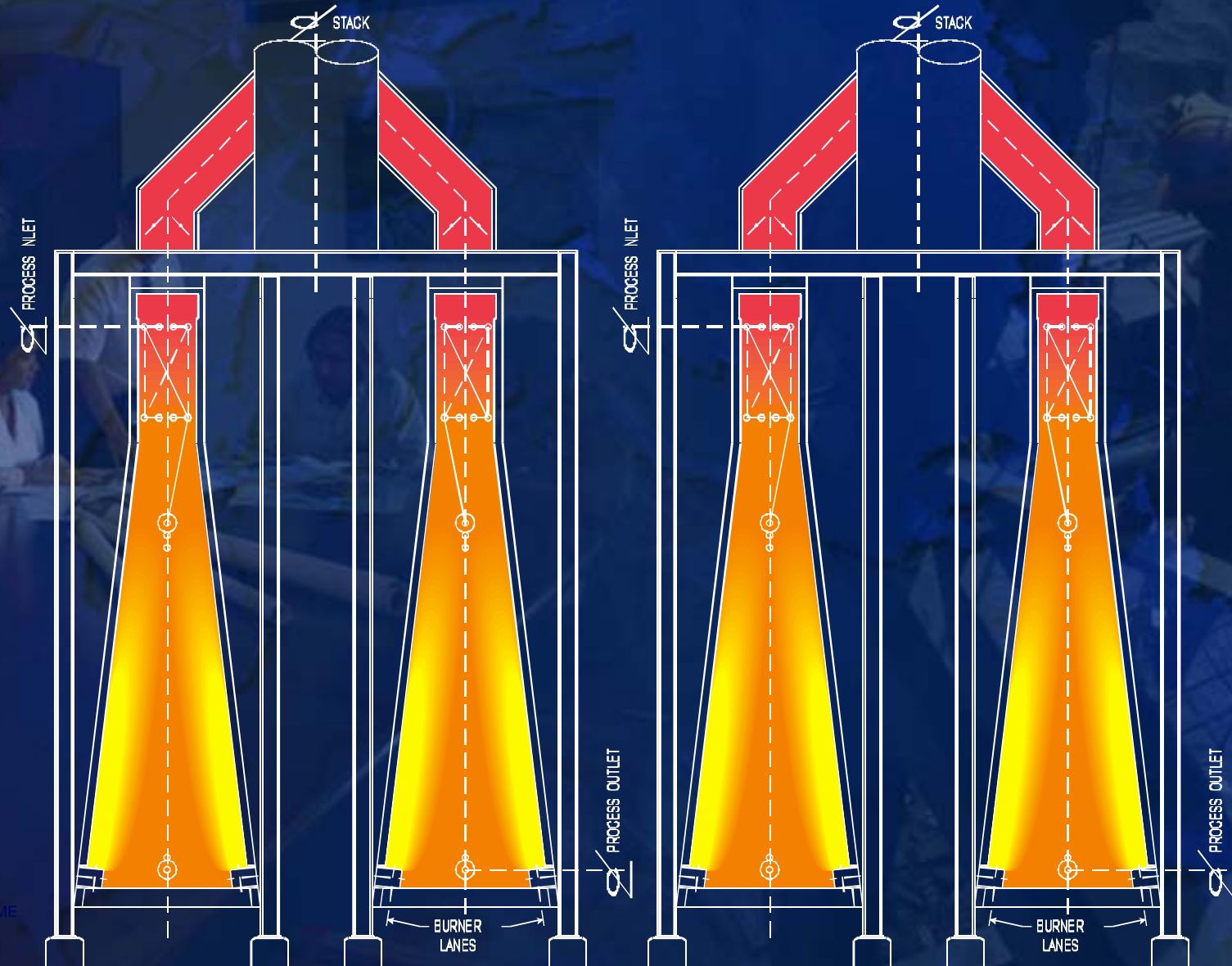
- 4" Assembly - 56"
- 6" Assembly - 66 3/4"
- 8" Assembly - 68 3/4"

**Courtesy of Decoking Descaling  
Technology Inc.**

# ON-LINE PIGGING-PAIR OF PASSES



# ON-LINE PIGGING INDIVIDUAL PASSES





# BURNER SELECTION

- Elliott's Rule on Individual Pass Control Impacts to Burner Selection and Firing
- Burner Flames Stabilized on a Bridgewall and only to Provide Heat for One Pass
- Planar Heat Flux Provides Uniform Heat Flux to Tube - Along the Tube Length as Well as Up the Radiant Coil
- Higher Burner Count Spreads the Flames and also Reduces Flame Length so Heat Flux is at the Process Outlet Where Desired
- Generous Firebox Dimensions Provide a Better Recirculation of the Flue Gases for More Uniform Bridgewall Temperature

## WITHOUT PASS CONTROL

**Flames are not  
Stabilized on a  
Wall and not  
Uniform in Flux**

**One Burner for 2  
Passes are not  
Individually  
Controllable.**

**Not able to  
individually  
spall**

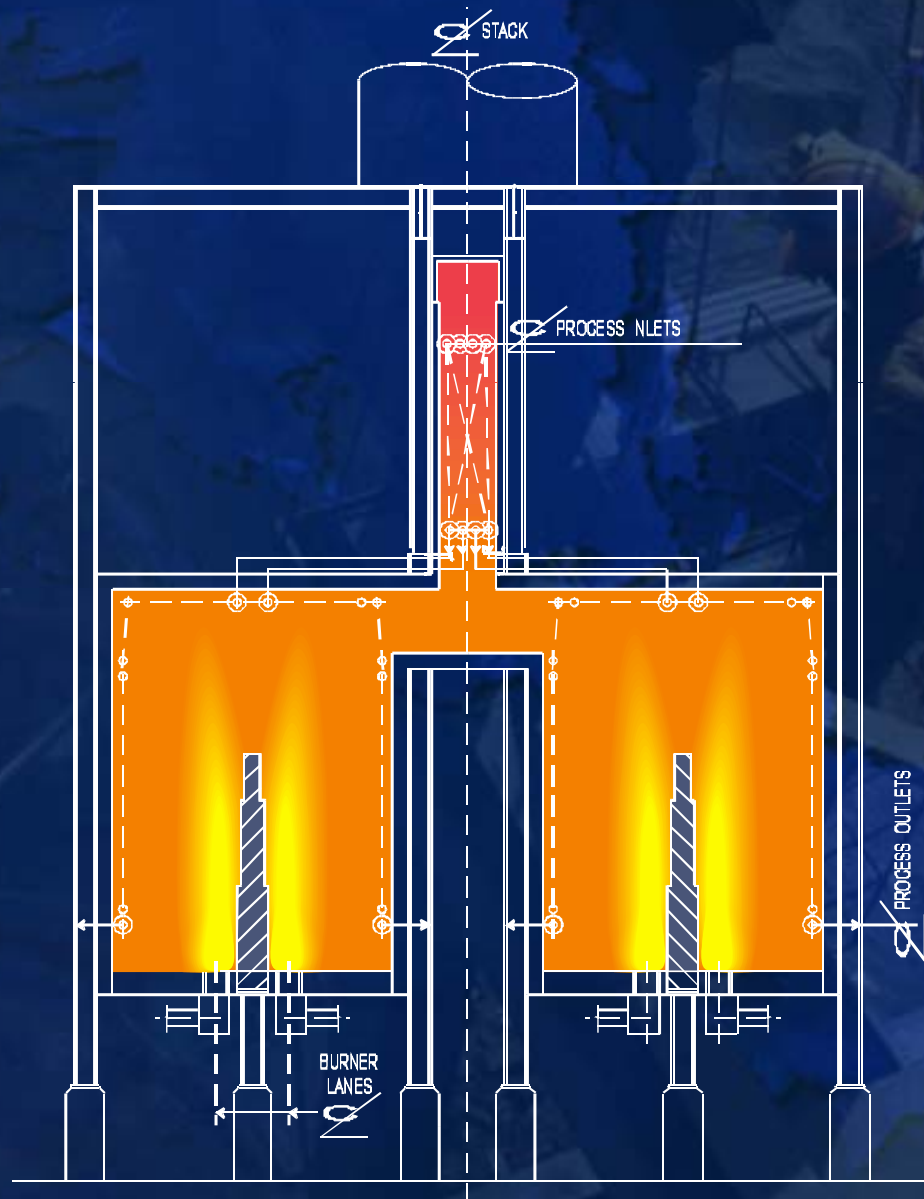


# DELAYED COKER CHARGE HEATER

**Flames  
stabilized on the  
Bridgewall for  
longitudinal and  
vertical uniform  
Flux**

**Individual pass  
and firing  
control.**

**On line spalling  
is possible.**





# UNIFORM HEAT FLUX FIREBOX

**More  
burners  
keep flames  
low in the  
firebox and  
spread the  
flames  
laterally**



# RADIANT TUBE SUPPORTS OPTIONS

- **Top supported**
  - Tubes will loose contact to support as the support grows downward
- **Bottom supported**
  - Tubes maintain contact to support as support expands upward
- **Replaceable with tube removal less costly upfront but requires cutting tubes**
- **Replaceable WITHOUT tube removal more costly upfront but prevents cutting tubes**





# MODULARIZATION

- **Extent of Shop Fabrication is One of the Most Important Price Differentiators**
- **Maximum Modularization has Numerous Connotations**
- **Full Understanding of the Degree of Pre-Fabrication is Crucial for a Proper Evaluation and Understanding of TIC**
- **Typically Field Work is a Multiple (X times) of the Equivalent Work Performed in a Shop**



# PANEL SUPPLY



**Least Costly Modularization  
Supplied With or Without Refractory**



# MODULARIZATION

## Over land shipment



**Refractory  
Usually Shop  
Installed**

# MODULARIZATION

## Ship/Barge Shipment



**Radiant Cell Fully Assembled**



# EXISTING UNIT OPTIONS

**More Capacity  
Higher Efficiency  
Longer Run Length  
New Process Conditions**

## GENERAL COMMENT

- Many old heaters (of any service) were designed for conditions far from what is encountered today
- Coker Heaters have the worst impact from this.
  - Crudes are heavier than original design
  - Burners were shorter and narrower
  - Throughput has been pushed
  - Design not set up for modern spalling and pigging operations
- Many new ideas may work uniquely and very well in certain applications but poorly in others applications.

# EXTERNAL PRE-HEAT

- **Heat Exchanger Pre-heat can Unload the Coker Heater Firing for Additional Capacity**
- **However, Increasing the Crossover Temperature is not Always a Good Idea**
  - **If the Process Flow Rate Increase does not Off-set the Longer Residence Time Above Cracking Temperature, More or Quicker Coking May Occur**
  - **If the Crossover Temperature is Increased too High, There is Risk of Convection (Shock) Row Cracking and Coking Occurring**
- **It is Suggested a Full Review of the Heater Design and Process Conditions be Performed for these Situations.**



# LoNOx BURNER ADDITIONS

- **Many Old Heaters were Designed for Different Conditions than they are Operated on today, Burners are No Exception.**
- **New LoNOx Burners Require Larger Spacing than Old Burners; A Burner for Burner Hole Change out is not Possible in Most all Cases.**
- **Old Short Fireboxes do not Accommodate New Longer Burner Flames without Impacting the Coker Heater Operation.**
- **A Combined Review of the Process and the Heater Design is Needed for Adding LoNOx Burners.**

## APH-AIR PREHEAT ADDITIONS

- **Similarly to External Pre-heat, APH modifies the Radiant Section Heat Recovery.**
  - **Reduced Flue Gas Flow Changes the Crossover Temperature**
  - **Radiant Flux is Increases Accordingly**
  - **Radiant Bridgwall Temperature is Increased**
  - **Burner Firing is Lower**
- **Again a Combined Process and Heater Review is Needed to Continue the Previously Achieved Coking Run Lengths.**

# CERAMIC COATINGS

- Can be Used on New Units too, but what is 'Design Basis'? The Coating working or it not working?
- Coatings are Used on Tubes and/or the Refractory to 'Re-shape' the Heat Flux Profile as Claimed
- Papers have been Presented Promoting the Successes, However the Results are not universal and the Coating has a Finite Life Before Recoating is Required.
- Some of the Success can be Attributed to the Cleanliness of the Tubes Needed for Applying the Coating.



## **INTERNAL COATINGS**

- **Alonizing was Promoted in the Past to Retard Internal Coke Build up. Fabrication Issues Prevented the Coating from Having Much Success in Industry.**
- **New Internal 'Nano' Coatings are Entering the Market with Recent Installation for Testing**
- **Chemicals for Injection are on the Market and Again Papers Presented on their Merits**
- **All these Uses Should be Properly Explored with Clear Expectations Identified from the Onset by Both Parties.**

# TUBE METALLURGY

- **Although Mentioned in New Units Section, this Option is more Applicable for Existing Units Use. Stainless Tubes are the Typical Alternate Tube Material Due to:**
  - **Thinner Tubes can Reduce  $\Delta P$  or Increase Flow rate**
  - **Spalling can be More Effective/Quicker**
  - **Tube Metal Temperatures can be increased (Longer Run Lengths Possible)**
- **Just Remember the Previously Mentioned Limitations of its use**

# OTHER IDEAS ON COKER HEATERS

- **Film Cracking**
- **Upflow in Radiant Section**
- **Split Flow**
- **Flue Gas Recirculation into radiant section  
(not to burners for NOx reduction)**
- **Double Row of Double Fired Tubes**



# JUST BECAUSE THE COIL IS SIZED, THE DESIGN OF THE COKER HEATER IS FAR FROM COMPLETE

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