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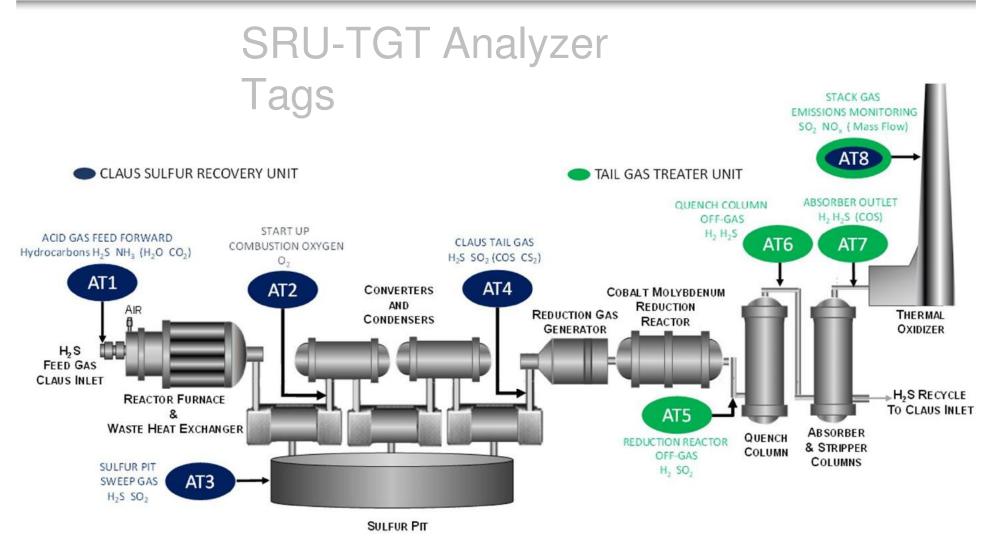
### **SRU-TGTU Analyzer Best Practices**

### RefComm Galveston 2016 Sulfur Recovery





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## AT-1 (Acid Gas)

 $H_2S$  + Total Hydrocarbon (CO<sub>2</sub>, H<sub>2</sub>O, NH<sub>3</sub>) (BTEX, MeOH)



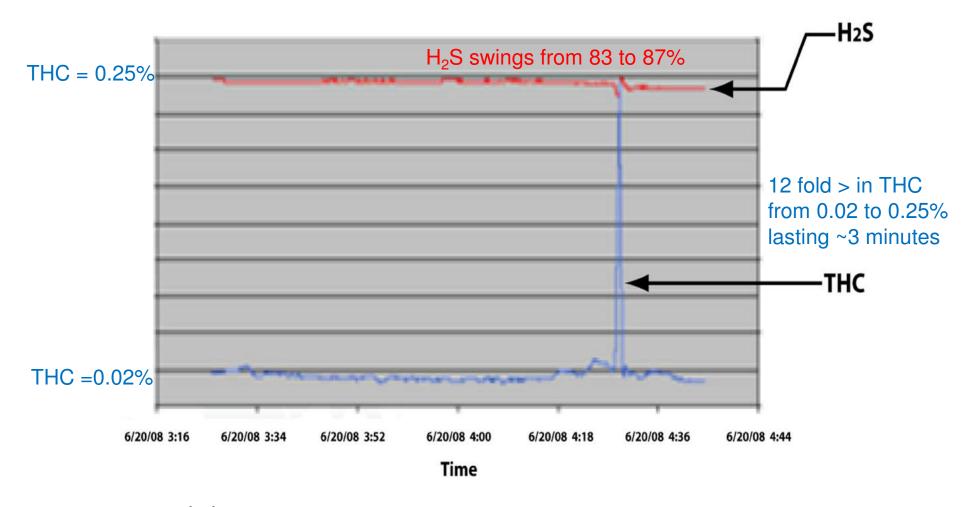
### O<sub>2</sub> Required to Burn Hydrocarbons Compared to an Equal Amount of H<sub>2</sub>S

Compound	Moles O <sub>2</sub> per Mole HC	Ratio of $O_2$ needed per mole HC compared to mole of $H_2S$
Methane	2	4
Ethane	3.5	7
Propane	5	10
Butane	6.5	13
Pentane	8	16
Hexane	9.5	19



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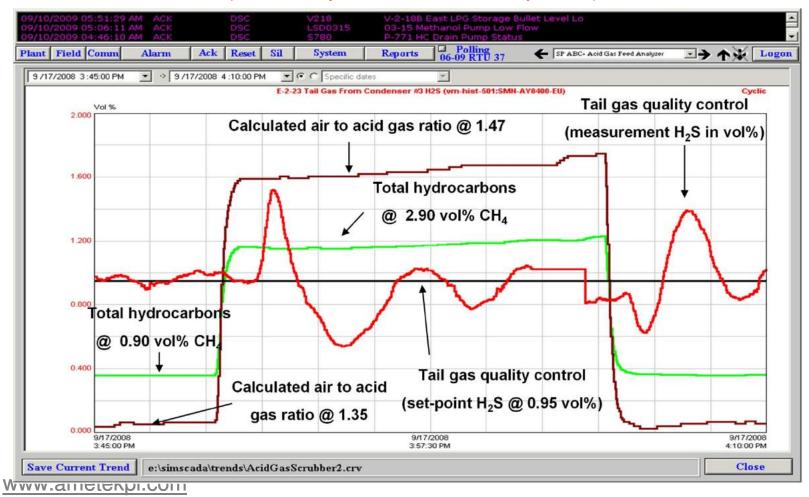
### Field Data / HC Process Upset





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### Feed Forward Analysis: Actual Control Response to Hydro-Carbons (Courtesy of Jacobs Comprimo)





### Acid Gas Analyzer / Summary

- Benefits
  - For SRUs with TGTU: Mitigation of SO<sub>2</sub> breakthrough to the amine absorber...Its not when the HC comes that makes the problem, its when the HC goes away
- To be "ready" install a heated acid gas probe at shutdown



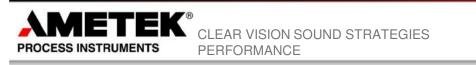


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## AT-4 (SRU Tail Gas)

 $H_2S/SO_2$  $(COS, CS_2)$ 

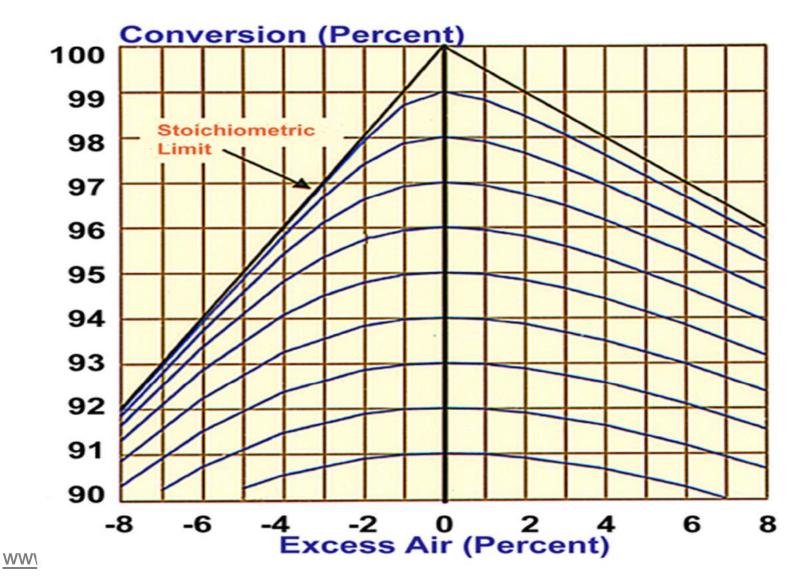


### Ratio vs Excess H<sub>2</sub>S vs Air Demand

- Ratio is the non linear expression of 2 H<sub>2</sub>S / SO<sub>2</sub>
- Excess  $H_2S$  is the linear expression of [ $H_2S$ ] - 2[ $SO_2$ ] = -1%...0...+1%  $H_2S$
- Air Demand uses a scaling factor *AD*{2[SO2] - [H<sub>2</sub>S] } = -5%...0...+5% AIR (*AD* factor is nominal 3.5)



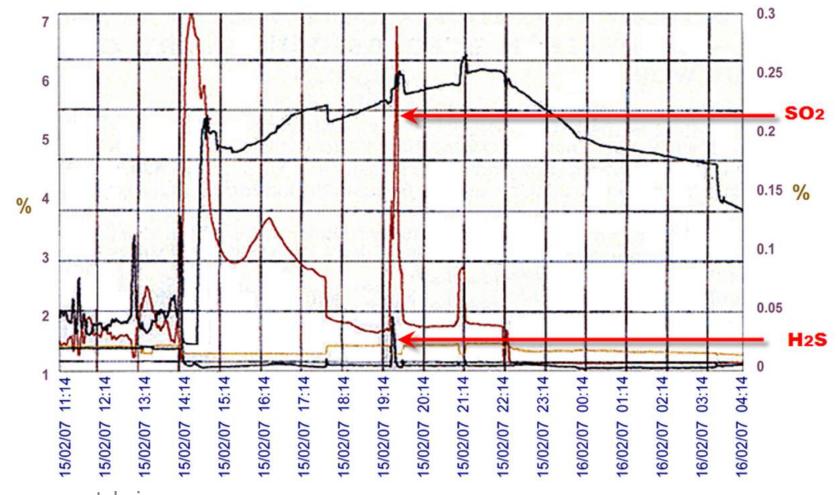
Tail Gas: Efficiency as a Function of Excess Air





### Tail Gas: Process Upset & Over-Range Event

SRU TAIL GAS ANALYSIS (Model 900 Air Demand Analyzer)

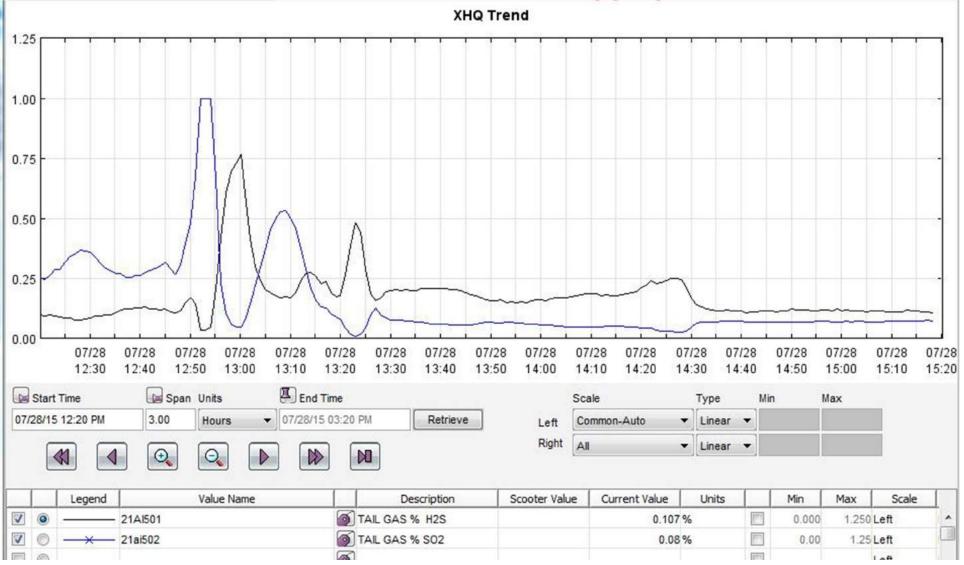




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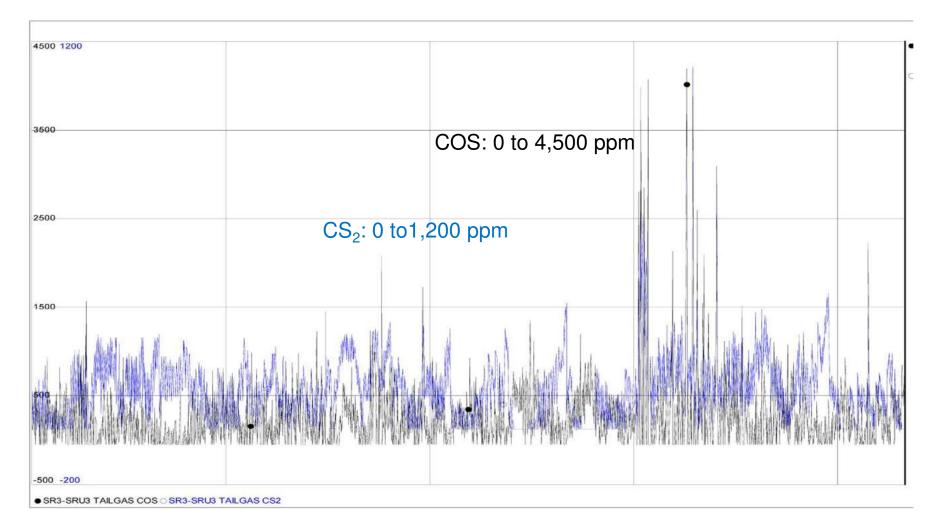
### SRU at Turndown

#### (slow response vs plugging)





### COS & CS<sub>2</sub> in SRU Tail Gas





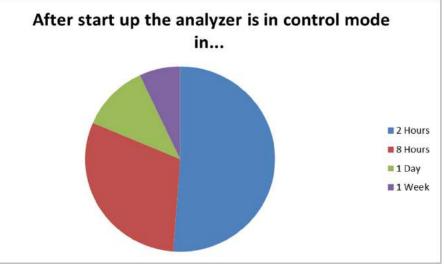
### Putting the Analyzer in Control After Start-up

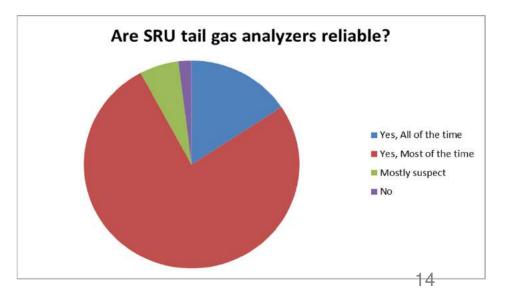
- "After start up when is the analyser put into control mode ?"
- Catalyst preference for H2S over SO2 can skew true air control.
- Sulphur Experts recommends control mode after 8 hours.

#### "Do you consider tail gas analysers to be reliable ?"

- Thankfully yes was common response
- Responses capture the evolution of the tail gas products.
- Time for a 3<sup>rd</sup> generation.









Tail Gas / Best Practices



**Top of the Pipe Analyzer** 

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Insulated steam jacketed nozzle



www.ametekpi.com



Sample Line Analyzer 900 ADA

> Weather cover for ASR probe and jacket





### Tail Gas Best Practices / Weather Protection



"Each 10C increase in operating temp above 25C reduces mean electronics component operating life by 50%"



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### Tail Gas "Sample Line" / Best Practices

Installed at 45° between Cd4 & RGG (bad piping design...good installation) Slope the sample line, no pockets







### Tail Gas Analyzer / Summary

- Heat integrity at the sample point is paramount
  - Regulated MP steam is best, trapped LP if a must
  - Solve heat integrity problems with Conto-Trace (do not wrap tubing around a nozzle (which does not work)
- Observe the H<sub>2</sub>S/SO<sub>2</sub> indicating outputs
  - They can give non predictive results
  - When the analyzer is moving...its working
- Connect the analyzer into the AIT data network



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# AT-5/6/7 (TGTU)

 $H_2/H_2S$  $(COS / SO_2)$ 

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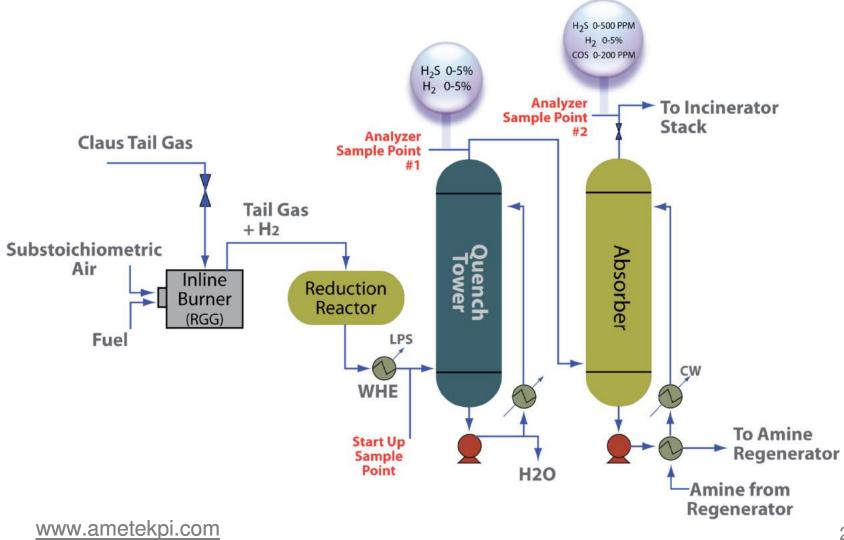
### Analytical Measurements on a TGTU

- The critical (gas) measurements are <u>H<sub>2</sub> and H<sub>2</sub>S</u>
- <u>COS</u> is a secondary measurement in combination with  $H_2 + H_2S$
- <u>CS<sub>2</sub></u> for certain applications but COS considered more important
- $\underline{SO}_2$  can be measured at the quench inlet or outlet (not common)
- <u>pH</u> is measured in the quench water (not addressed here)



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#### **Amine-Based Tail Gas Treating Unit**





### Ranges for H<sub>2</sub>S/COS/CS<sub>2</sub> Location for H<sub>2</sub> Measurement

- Optimal analytical ranges
  - [H<sub>2</sub>S] > [COS] > [CS<sub>2</sub>] generally exist in < concentrations</li>
  - Ranges subject to spectroscopy matrix, optimal ranges are;
    - H<sub>2</sub>S 0-100 ppm (up to 0-500 ppm FSR depending on permit levels)
    - COS 0-200 ppm
    - CS<sub>2</sub> 0-50 ppm
- H<sub>2</sub> sample point location when there are 2 analyzers
  - Locate the H2 measurement at the Absorber outlet (slightly cleaner)
  - If using Flexsorb locate the H2 measurement at the Quench outlet



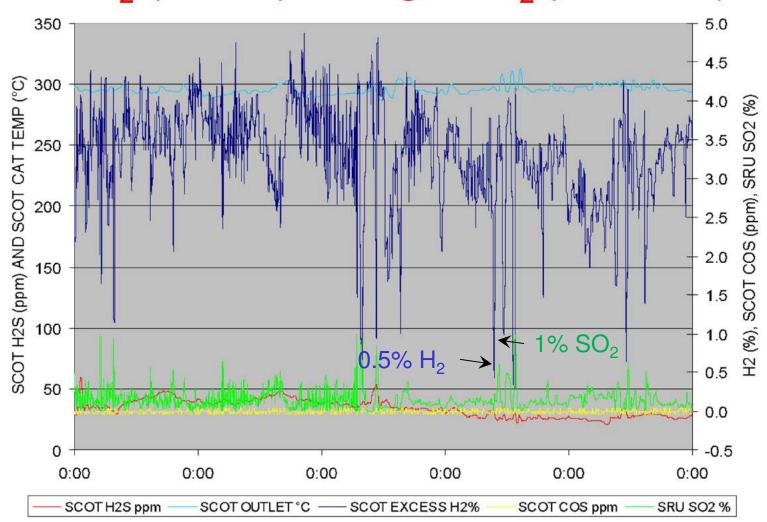
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### HAG Particulate Filter After SO<sub>2</sub> TGTU Upset



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Low H<sub>2</sub> (TGTU) vs High SO<sub>2</sub> (Tail Gas)



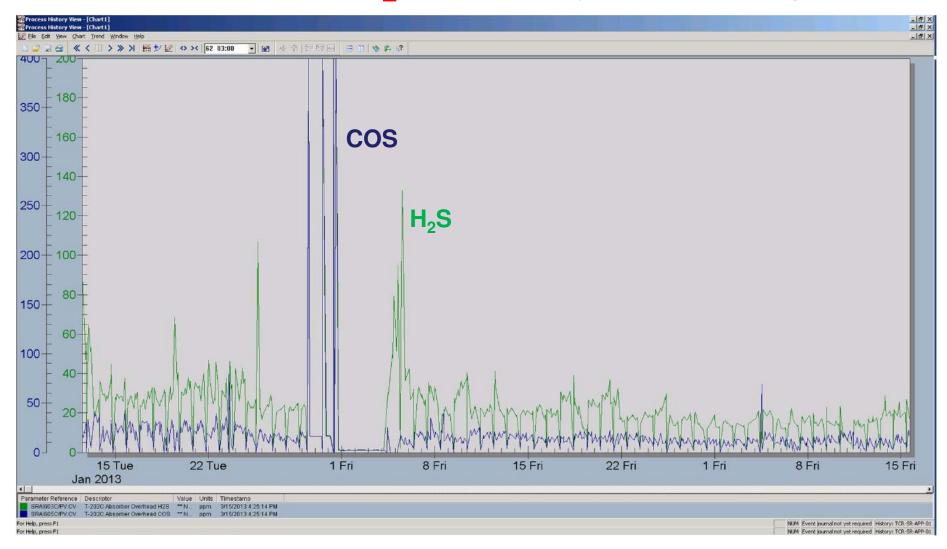
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### TGTU (COS & H<sub>2</sub>S) Steady State & Upset





### TGTU Analyzer Summary

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- $A H_2 / H_2 S$  analyzer is critical to the operation of a TGTU
- When replacing a legacy H<sub>2</sub>/H<sub>2</sub>S analyzer add the COS/CS<sub>2</sub> measurements
- If there is a diverter valve have a "start up" sample point
- If there is an analyzer at both the Quench and Absorber outlet put a H<sub>2</sub> sensor at both locations
- This survey is based on~190 analyzers
  - Of which ~150 are at Abs outlet, ~35 at Quench outlet. ~5 at Quench inlet



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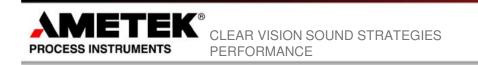
## AT-8 (Emissions)

### $SO_2$ $SO_2$ Mass Emission (H<sub>2</sub>S, O<sub>2</sub>, NOx)



### **Other Parameters**

- SO<sub>2</sub>
  - Dual range for TGTU bypass periods
- H<sub>2</sub>S
  - Measurement of residual value after incineration (~10 ppm)
  - The part of EPA sub-part J(a) that was not promulgated
  - Accounting for un-combusted reduced S compounds by oxidizing the residual H<sub>2</sub>S to SO<sub>2</sub>
- O<sub>2</sub>
  - Stand alone analyzer or on board with CEMS SO<sub>2</sub> analyzer
  - Combustion control can only be done with stand alone
- NOx
  - NOx values are low, not normally required



### **Emission Analyzers**

- "The Color of Plumes"
  - White: Steam plume caused by water condensation (cold, Canada)
  - Bluish white: SO<sub>3</sub> plume usually caused by high SO<sub>2</sub> emissions
  - (....Confirmed by "<u>Green Slime</u>" in the CEMS sample system)
  - Orange: NO<sub>x</sub> plume
  - Brown: Unburned hydrocarbon / soot plume
  - Green: Burning H<sub>2</sub>S plume



## AT-2 (O<sub>2</sub> / SRU Start up)

### O<sub>2</sub> (CO, Combustibles)



### Process Oxygen Measurement

- For start-ups and shut-downs of the SRU
  - Requires excess O<sub>2</sub> to near stochiometric conditions of 0.1% xs air
- Measurement typically done by operators using portable unit
  - Safety considerations: exposure of personnel during start up
  - SRU-TGTU tend to be all at one time and not in sequence
- A fixed (permanent) system can consist of;
  - Laser based "non contact" type analyzer (capable of sampling into "Claus" mode but shut-in after transition to "Claus" mode)
  - Isolated between start ups with "ASR" probes



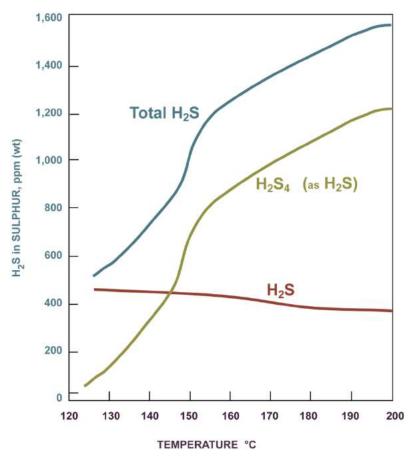
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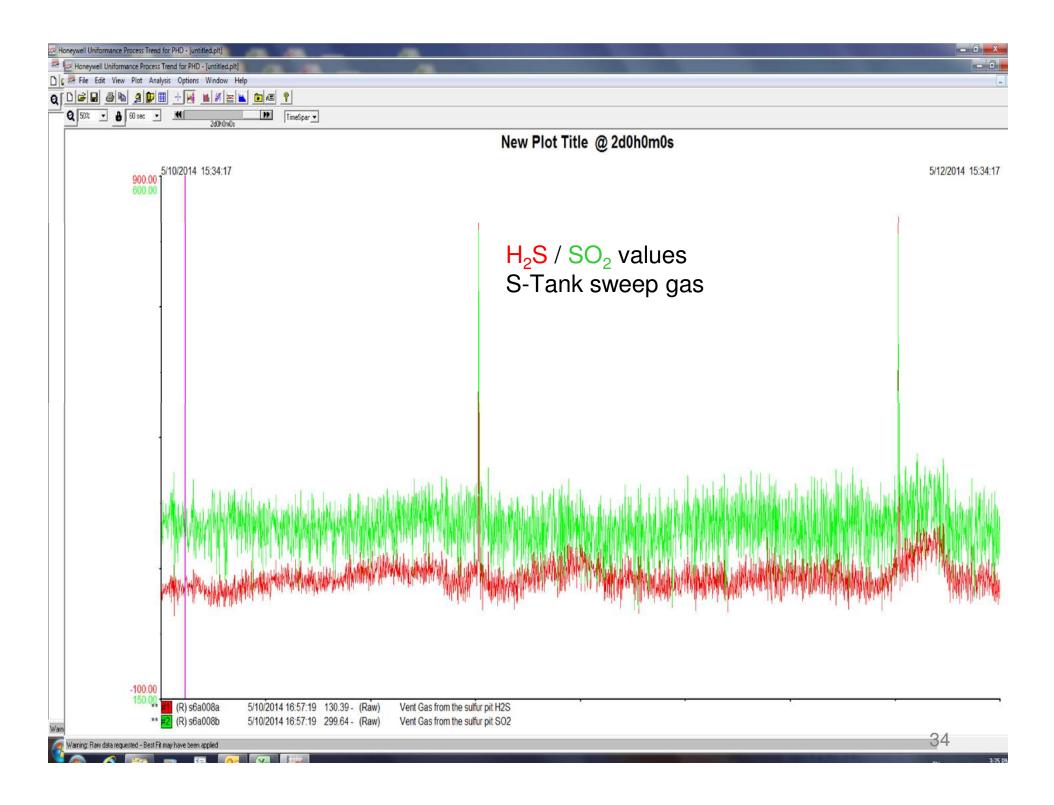
## AT-3 (Sulfur Pit)

 $H_2S \ (\text{LEL}) \\ SO_2 \ (\text{Pyrophoric sulfur fire})$ 

### Sulfur Pit Gas: Solubility of H<sub>2</sub>S in Sulfur

- Produced sulfur has ~600 ppm of dissolved H<sub>2</sub>S + hydrogenpolysulide
- Spontaneous degassing and concentration in the gas phase can increase to explosive levels (<u>3.25%</u>)
- Pit gas analyzer requires same sample integrity as tail gas analyzer
- H<sub>2</sub>S is measured to warn of LEL, SO<sub>2</sub> is measured to warn of S-fire
- Used to quantify addition to emissions (Pit can be1/3<sup>rd</sup> or more of emissions)



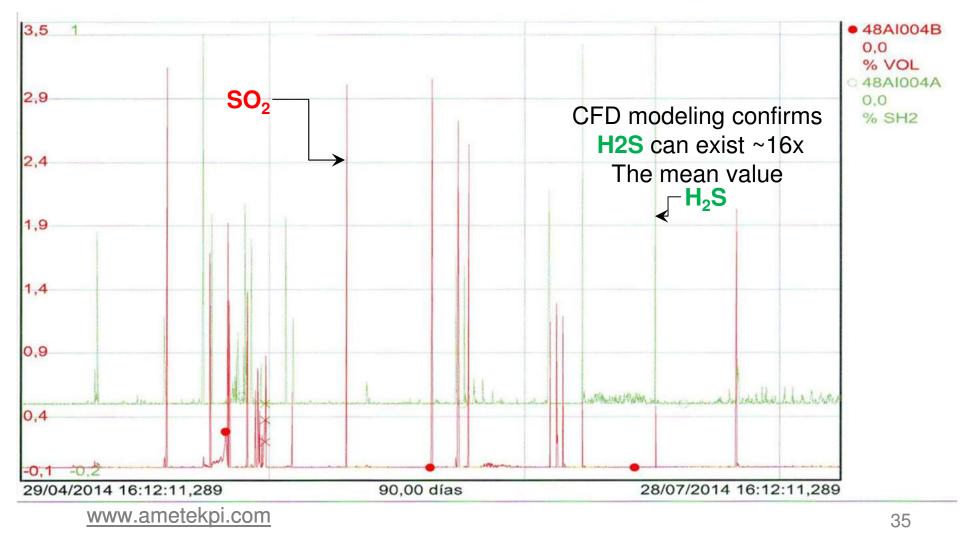


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### Sulphur Pit High H<sub>2</sub>S & SO<sub>2</sub> Values (Just prior to an incident)





### Maintenance: Analyzer Categories

	Complexity Factor Category	Type of Analyzer	Estimated PM (h/month)
	1. (Simple)	pH, Conductivity, Gas Detection, $O_2$	2
	2.(Physical Property)	Boiling Point, Flash Point, Freeze Point, RVP, Viscosity	3
Outside	3.(Environmental)	CEMs SO <sub>2</sub> , CO, Opacity, <mark>H<sub>2</sub>S</mark>	2.5
ō	4.(Complex)	Tail Gas, GC, Mass Spec, NIR, FTIR, <u>H<sub>2</sub>S</u>	4

Courtesy of Chevron ETC, Analyzer Engineering Group



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