

# SULZER

## Upgrading a FCC Main Fractionator to Improve Operational Reliability and Flexibility

Giuseppe Mosca | RefComm conference, Budapest 4,5 October 2017



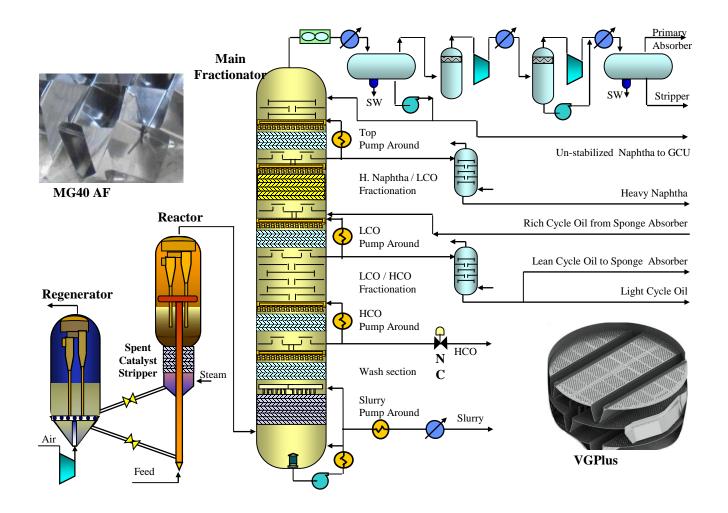


## Agenda

- FCCU flow diagram
- Major concerns of the existing Unit
- Plant Survey
- Modifications of the Main Fractionator
- Plant feed back data
- Conclusions



#### **FCC Unit Flow Diagram**





## **Unit Background**

- The Unit was licensed by UOP, and commissioned in 1984 with a capacity of 1 MM t/a
- A first revamp was implemented in 1994 to boost the capacity by 50%, i.e. 1.5 MM t/a
- A second revamp was implemented in 2005 to further increase the capacity up to 1.75 MM t/a
- The third revamp was implemented in 2012, same capacity, 1.75 MM t/a, but lighter feed and higher conversion than 2012 revamp.



## **Unit Major Concerns**

- In 2014, after 2 years operation from third revamp, the Unit started to face instable operation at Main Fractionator
- The pressure drop across the tower started to increase
- The Unit could not operate anymore at maximum capacity, it was reduced down to 85% of the target
- The reactor temperature was reduced with a consequent reduction of the conversion.

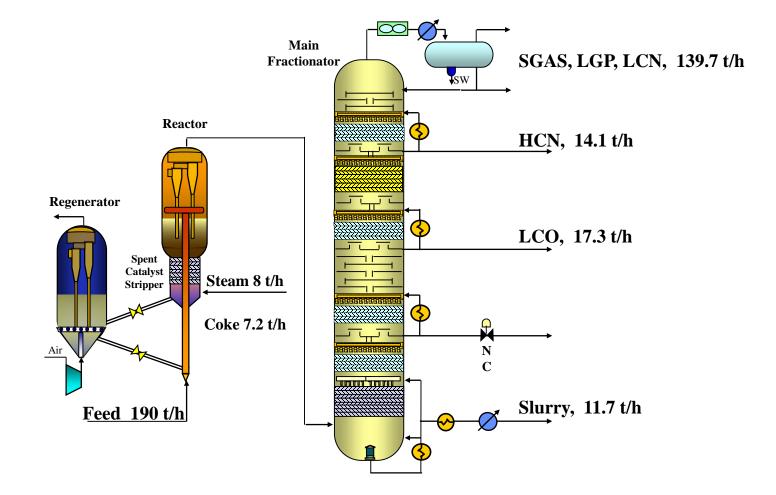


## **Plant Survey**

- In 2015 the team "Engineered Solutions Refinery" of Sulzer was appointed to troubleshoot the Main Fractionator
- A test run was performed with Sulzer people at site, the following main data was gathered:
  - Temperature and pressure profiles of the Main Fractionator and GasCon towers
  - Flow rates of the Pump Arounds, refluxes, and run down products
  - Distillation curve and density of the liquid products
  - Composition of the LPG and Gas

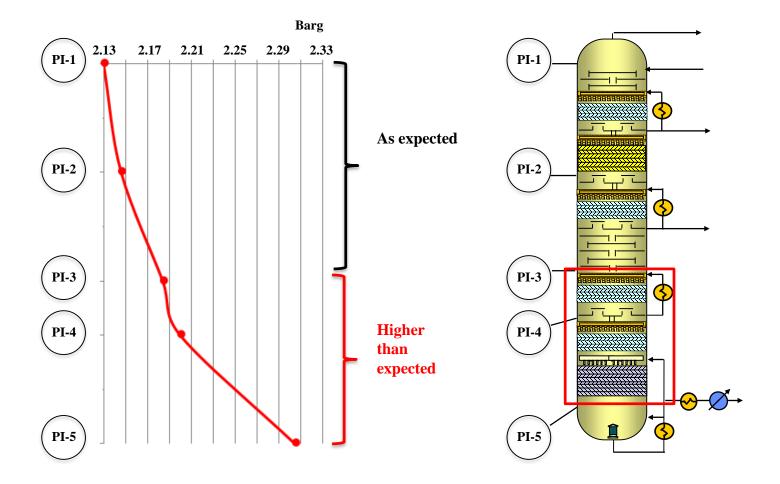


#### **Unit Material Balance**





#### **Pressure survey at Main Fractionator**





	VGO	LCN	HCN	LCO	НСО	CLO
Distillation Method		D86	D86	D86	D86	D1160
Sp. Gr.	0.8805	0.7218	0.8867	0.9440	0.9486	1.0387
IBP °C	290	31	168	126	164	282
5 % "	356	45	186	218		341
10 % "	377	49	190	241	310	356
20% "	398	55	195	260	324	373
30% "	412	60	201	272	340	386
40% "	424	66	210	281	340	397
50% "	436	75	217	289	348	408
60% "	449	90	224	298	353	418
70% "	465	111	233	306	358	430
80% "	485	136	243	317	362	446
90% "	511	158	256	333	372	471
95% "	530	173	266	347	383	491
FBP "	553	197	281	359	394	520

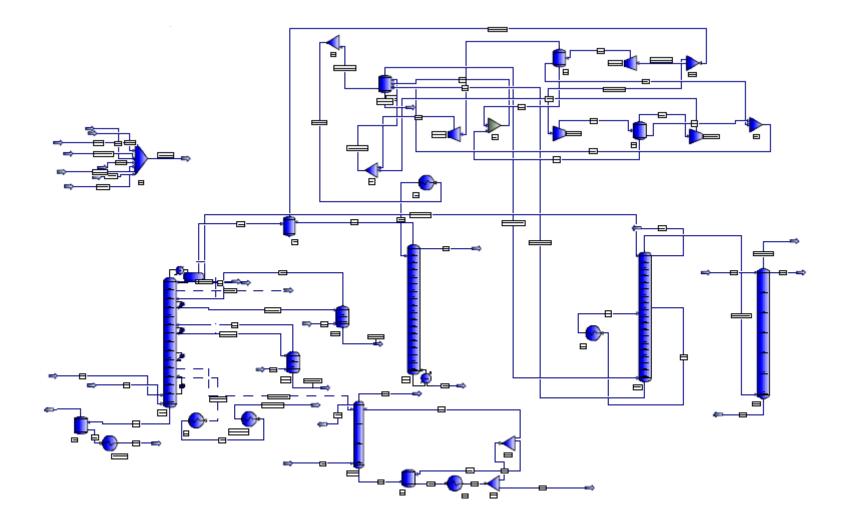


### LPG and Gas Composition

Gas Analysis						
Component Mole %	LPG	WGC	Sponge Gas			
<b>C</b> <sub>1</sub>		6.2	29.1			
C <sub>2</sub>	0.3	3.0	10.4			
C <sub>2</sub> -		5.2	21.3			
C <sub>3</sub>	11.6	6.4	0.9			
C <sub>3</sub> -	24.2	24.4	3.2			
IC <sub>4</sub>	27.1	13.5	0.6			
NC <sub>4</sub>	5.3	2.4	0.1			
1C <sub>4</sub> -	7.1	3.3				
IsoC <sub>4</sub> -	10.7					
$T_2C_4$	8.2	4.1	0.1			
C <sub>2</sub> C <sub>4</sub> -	5.4	2.5	0.1			
IC <sub>5</sub>		5.7	0.4			
NC <sub>5</sub>	0.1	0.4	0			
1,3,C <sub>2</sub> C <sub>4</sub> =			0.1			
H <sub>2</sub>		1.4	6.3			
0 <sub>2</sub>		2.2	1.5			
N <sub>2</sub>		13.9	21.4			
CO <sub>2</sub>		1.1	4.2			



#### **Process Simulation Model**



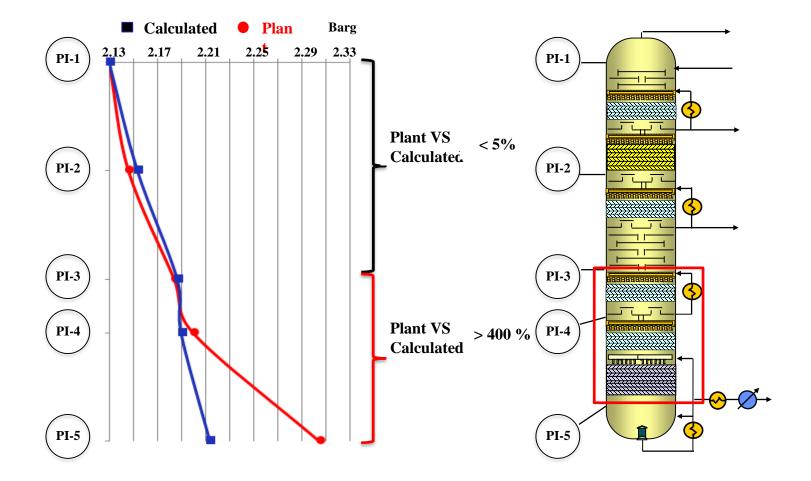


## Hydraulic Rating of Main Fractionator

Tower Section	МТС	Hydraulic Flood	
Top fractionation	Conventional Trays	Moderate	
HCN PA	Structured Packing	Moderate	
HCN / LCO fractionation	2 <sup>nd</sup> Generation Structured Packing	Moderate	
LCO PA	Structured Packing	Moderate	
LCO / HCO fractionation	High Performance Trays	Moderate	
HCO PA	Structured Packing	Moderately high	
Wash Bed	Structured Packing	High	
Slurry PA	Structured Grids	High	



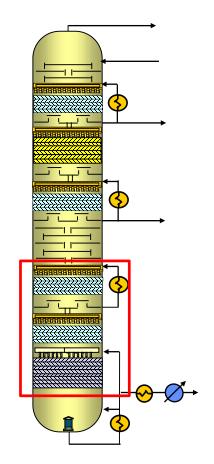
#### **Pressure Profile: Plant data VS Calculated one**





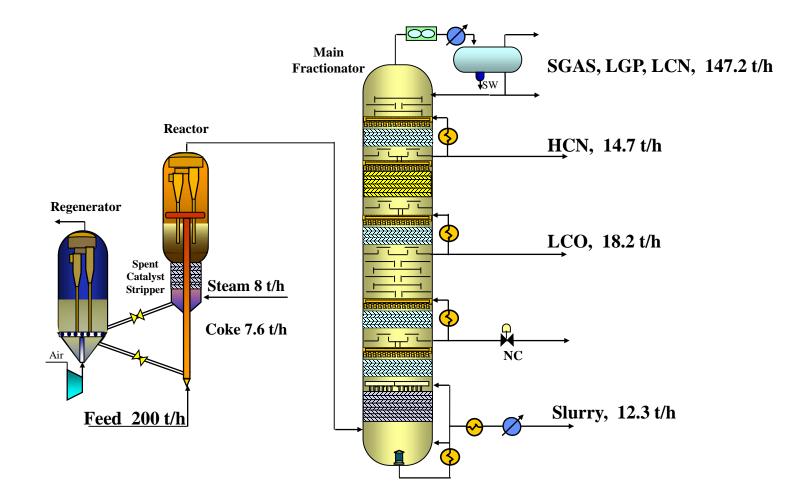
## **Plant survey: Findings**

- The top sections of the Main Fractionator are working fine, i.e. HCN PA, HCN / LCO fractionation, LCO PA, LCO / HCO fractionation
- The bottom 3 sections are the bottleneck, i.e. HCO PA, Wash section and Slurry PA
- The bottleneck is more related to fouling accumulation than hydraulic limitation of the existing Mass Transfer Components



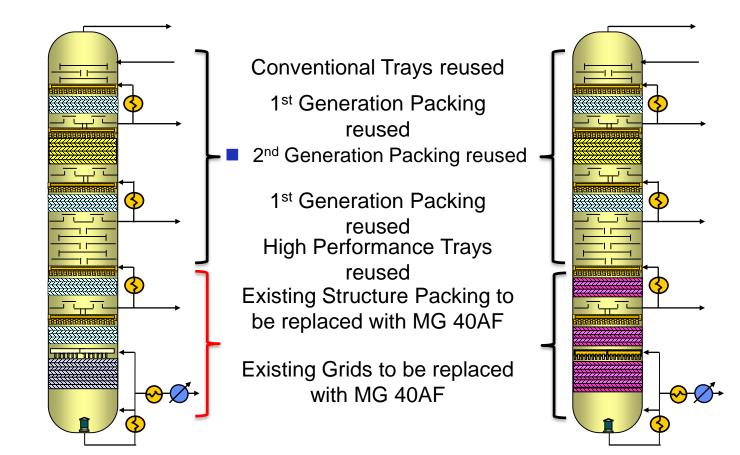


## **Required Material Balance for future operation**





## **Main Fractionator Modifications**

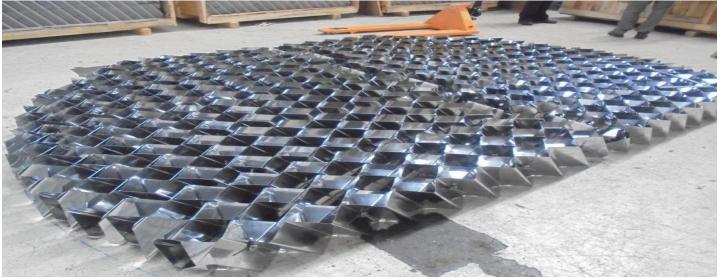




## **New Anti-Fouling Grid Packing MG40 AF**

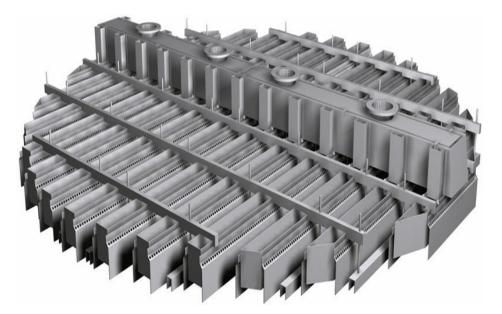
- Highest hydraulic capacity
- High heat transfer efficiency
- Superior fouling resistance
- Superior mechanical stability







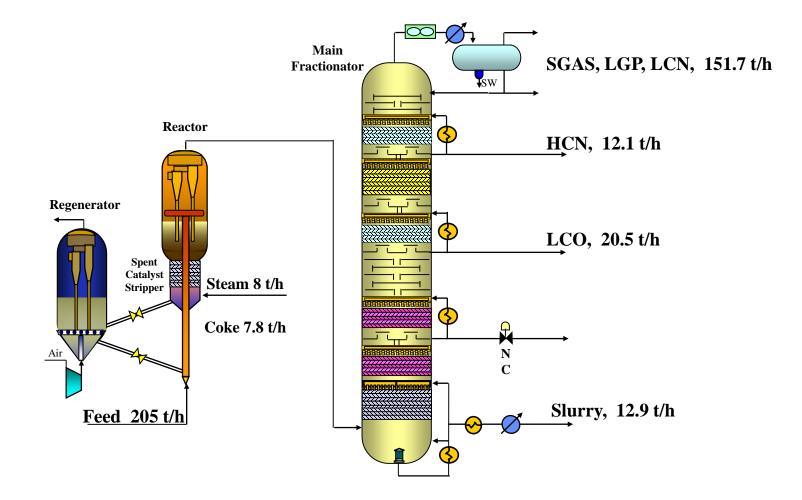
## **Anti-Fouling liquid distributor VES**



- Through type liquid distributor
- Suitable for high liquid loadings
- Suitable for handling solid debris
- Great resistance to fouling
- Good distribution efficiency
- High mechanical stability



#### Test Run data after revamp





## Conclusions

- The upgrading of the Main Fractionator was implemented in the planned turnaround, and the plant was successfully re-started last October 2015
- The Unit is operating at capacity even higher than revamp target, with smooth column operation and desired products qualities
- There is still a room to further boost the throughput, the ultimate capacity will be checked when the feed will be made available.

